

USARTL-TR-78-55C

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LEVEL II



COMBUSTOR DESIGN CRITERIA VALIDATION
Volume III - User's Manual

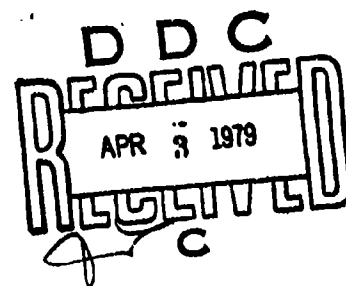
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February 1979



Final Report for Period 2 JULY 1975 - 31 October 1978

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APPLIED TECHNOLOGY LABORATORY POSITION STATEMENT

This report describes an effort undertaken to improve small gas turbine combustor design techniques. This analytical procedure is viewed as a significant step toward reducing the design and development time and the cost associated with future Army gas turbine combustors while simultaneously achieving a more durable and fuel-efficient design. The reader is referred to the report documentation page for a description of each of the three volumes of this report. It is considered worthy of widespread application with the turbine industry. Any critique or other response regarding its use should be addressed to this Laboratory.

Mr. Kent Smith of the Propulsion Technical Area, Aeronautical Technology Division, served as Project Engineer for this effort.

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SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

REPORT DOCUMENTATION PAGE		READ INSTRUCTIONS BEFORE COMPLETING FORM	
1. REPORT NUMBER	2. GOVT ACCESSION NO.	3. RECIPIENT'S CATALOG NUMBER	
18 USART TR-78-55C			
6 COMBUSTOR DESIGN CRITERIA VALIDATION, VOLUME III, USER'S MANUAL	9	4. TYPE OF REPORT & PERIOD COVERED	
		Final Technical Report	
		2 July 1975 - 31 October 1978	
	14	5. AUTHORING OR PERFORMING ORGANIZATION NAME(S)	
		75 211882(38) 3	
10		6. CONTRACT OR GRANT NUMBER(s)	
H. C. Mongia R. S. Reynolds	15	DAAJ02-75-C-0044	
7. PERFORMING ORGANIZATION NAME AND ADDRESS		10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS	
AI Research Manufacturing Co. of Arizona 111 South 34th Street Phoenix, Arizona 85034	404 1196	B2209AHF262200AH78 00 079 EK	17 00
11. CONTROLLING OFFICE NAME AND ADDRESS		12. REPORT DATE	
Applied Technology Laboratory, U.S. Army Research and Technology Laboratories (AVRADCOM) Fort Eustis, Virginia 23604	11	February 1979	
14. MONITORING AGENCY NAME & ADDRESS (if different from Controlling Office)		13. NUMBER OF PAGES	
12 444 p		409	
		15. SECURITY CLASS. (of this report)	
		Unclassified	
		15a. DECLASSIFICATION/DOWNGRADING SCHEDULE	
16. DISTRIBUTION STATEMENT (of this Report)			
Approved for public release; distribution unlimited.			
17. DISTRIBUTION STATEMENT (of the abstract entered in Block 20, if different from Report)			
18. SUPPLEMENTARY NOTES			
Volume III of a three volume report.			
19. KEY WORDS (Continue on reverse side if necessary and identify by block number)			
Spray trajectory, evaporation rate, nozzle design, fuel-mixing rate, mean droplet size, reverse-flow annular combustor, liner wall temperature			
20. ABSTRACT (Continue on reverse side if necessary and identify by block number)			
This document, the User's Manual, is Volume III of the Combustor Design Criteria Validation Program. It contains general information, descriptions of analytical models, descriptions of associated computer codes, and illustrations of the various combustor models. Volume I of this report contains the results of the combustor element tests and analytical model validation which took place in Task I of the program. Volume II contains the results of Tasks II and III on the design, fabrication, and rig tests of two different reverse flow annular combustors (3 pps) designed to specific goals utilizing the analytical procedures.			

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TABLE OF CONTENTS

	<u>Page</u>
LIST OF ILLUSTRATIONS	5
LIST OF TABLES.	6
I. INTRODUCTION	7
General Information	7
Objective	8
1. Engine/Component Configurations	9
2. Parameters and Goals	9
Summary	10
II. DESCRIPTION OF ANALYTICAL MODELS	12
Annulus-Flow Model	12
3-D Combustor Performance Model	18
1. Equations of Continuity, Momentum and Enthalpy	20
2. Turbulence Model	22
3. Chemical Species Equations	23
4. Radiation Model	27
5. Spray Combustion	30
6. Calculation of Gas Temperature	37
7. Finite-Difference Solution of the Equations	38
8. Boundary Conditions	43
Liner Cooling Model	44
Transition-Liner Mixing Model	50
Gaseous Emissions Model	51
Fuel-Insertion Model	54
III. DESCRIPTION OF COMPUTER CODES.	58
Annulus Flow Model	58
3-D Combustor Performance Model	59
Liner Cooling Model	63
Transition Liner Mixing Model	65
Emission Model	67
Fuel Insertion Model	69

TABLE OF CONTENTS (Contd)

	<u>Page</u>
IV. ILLUSTRATIONS	71
Annulus Flow Model	71
Combustor Performance Model	77
Liner-Cooling Model	99
Transition Mixing Model	108
Emissions Model	120
Fuel Insertion Model	128
REFERENCES	137
APPENDIXES	
A - Input Sheets	139
B - Listing of Annulus Loss Model	178
C - Listing of 3-D Combustor Performance	207
D - Listing of Liner Cooling Model	273
E - Listing of Transition Mixing Model	316
F - Listing of Emissions Model	347
G - Listing of Fuel Insertion Model	383

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LIST OF ILLUSTRATIONS

<u>Figure</u>	<u>Title</u>	<u>Page</u>
1	Control Volumes for Annulus-Flow Model . . .	13
2	Liner Port Model Schematic	16
3	A Typical Comparison Between Prediction and Measured C_p	19
4	Schematic of Spray in Combustor Flow Field	33
5	Typical Grid Spacing and Control Volume Around a Point P	41
6	A Schematic of Reverse-Flow Annular Combustor and Application of Analytical Model	45
7	Typical Isothermal Plots of an Annular Combustor Along X-Y Plane in Line With Primary Jet	49
8	Annulus Loss Model Example Geometry	72
9	Annulus Loss Model Input Sheet	73
10	Sample Work Sheet for Program 117	75
11	Program 117 Input Data Sheet Input Format for Element Cards-Sheet 2	76
12	Annulus Loss Model Output	78
13	Annulus Loss Model Output	79
14	Annulus Loss Model Output	80
15	Combustor Geometry for 3-D Combustor- Performance Model	81
16	3-D Combustor Performance Model	82
17	Information Necessary to Describe an Inclined Wall	89
18	3-D Performance Model Output	92
19	Liner Cooling Model Input Sheet	100
20	Liner Cooling Model Output	105
21	Transition Mixing Example Geometry	109
22	Transition Mixing Model Input Sheet	110
23	Transition Mixing Model Output	116

LIST OF ILLUSTRATIONS (Contd)

<u>Figure</u>	<u>Title</u>	<u>Page</u>
24	Calculation Domain for Predicting Emission Output of Example Combustor	121
25	Emissions Model Input Sheet	123
26	Emission Model Output	129
27	Emission Model Output	130
28	Fuel Insertion Model Input	131
29	Fuel Insertion Model Output	135
30	Fuel Insertion Model Output	136

LIST OF TABLES

<u>Table</u>	<u>Title</u>	<u>Page</u>
1	Initial Profiles for Liner Cooling Example	104
2	Transition Mixing Model Geometry Input . . .	114
3	Initial Profiles for Transition Mixing Example	115
4	Additional Profiles for Emission Model. . . .	127

I. INTRODUCTION

GENERAL INFORMATION

The present program represents an extension and refinement of the previous effort with specific application to the design requirements of advanced, small, high-temperature-rise combustors for aircraft engines in the 2- to 5-pound-per-second (0.91- to 2.27-kilogram-per-second) flow range. This program was performed for the Applied Technology Laboratory, U.S. Army Research and Technology Laboratories (AVRADCOM), Ft. Eustis, Virginia by the AiResearch Manufacturing Company of Arizona during the period July, 1975, to October, 1978. The program is documented in this three-volume final report.

OBJECTIVE

The primary objective of this program was to further develop and validate existing analytical combustor design procedures that can be used to significantly shorten the design and development cycle of small advanced gas turbine engine combustors. Descriptions of the combustor analytical models, element tests and model validations are presented in Volume I.

The basic approach of the program consisted of a concentrated analytical treatment of key combustion phenomena affecting combustor performance complemented by rig tests. The rig test culminated in a complete series of performance mapping to validate the empirical/analytical combustor design procedure in an environment matching an actual operating engine.

The program was initially comprised of four technical tasks:

Task I - Analytical-Model Refinement

Task II - Full-Scale Combustor Design, Fabrication, and Preliminary Tests

Task III - Combustor-Performance Mapping

Task IV - Limited Modification and Retest

The Task I technical effort is described in Volume I. A complete description of the Task II and Task III activities is presented in Volume II. The computer codes for combustor design that evolved from that effort are fully documented in Volume III of this report. The combustor performance goals were achieved in Tasks II and III; thus Task IV was cancelled.

The computer models are based upon the numerical solution of the governing aero/thermo equations applicable to turbo-propulsion combustor environment, and are, therefore, applicable for analyzing internal flow field of can, can-annular and annulus combustor geometries. Both the inline and reverse-flow combustor configurations can be analyzed.

The cost-effectiveness of the empirical/analytical design procedure was to be demonstrated by undertaking the design and development testing of two full-scale annular combustors based on the following engine/combustor configurations, parameters and goals:

1. Engine/Component Configurations.

- Annular-combustor configurations
- Centrifugal compressor (last stage)
- First-stage axial turbine
- Nonregenerative cycle

2. Parameters and Goals.

- Engine airflow, $W_{a3} = 2.87$ pounds per second (1.30 kg/s)
- Combustor inlet pressure (P_3) = 10 atmospheres
- Compressor efficiency = 78.4 percent (total-to-static)
- Combustor inlet temperature = 660°F (622°K)
- Combustion efficiency = 99.5 percent (100 percent power) = 98.0 percent (5 percent power)
- Combustor pressure loss $\frac{P_{T3} - P_{T4}}{P_{T3}} = 3$ percent
- Combustor discharge temperature (T_{4avg}) = 2300°F (1533°K)
- Maximum pattern factor (PF) ≤ 0.23

$$\text{where } PF = \frac{T_{4 \text{ max}} - T_{4avg}}{T_{4avg} - T_3}$$

- Average radial temperature profile compatible with typical turbine blade requirements
- Maximum radial pattern factor (RPF) ≤ 0.075

$$\text{where } PF = \frac{T_{4 \text{ avg rad max}} - T_{4 \text{ avg}}}{T_{4 \text{ avg}} - T_3}$$

$T_{4 \text{ avg rad max}}$ = peak value of the circumferentially averaged radial temperature profile

- Good light-off/relight capability to 20,000 feet (6091 meters) altitude and ambient-temperature conditions per MIL-E-5007D Paragraph 3.2.5.1 (dated 15 October 1973)
- No visible carbon formation with hot fuel or at high-altitude conditions
- Multifuel capability, including JP-4 and JP-5
- Fuel contamination tolerance per MIL-E-8593A, Table X with filtration to 10 microns
- The combined CO and HC exhaust emissions will be sufficiently low to meet the previously noted combustion efficiency goals at 100- and 5-percent rated power. The NO_x LTO emissions level will be at or below the 1979 EPA NO_x standards. The maximum smoke number will be below the threshold of the exhaust plume visibility
- Acceptable component temperature levels and gradients to ensure long combustion system life and reliability
- Reasonable cost and weight

SUMMARY

A complete description of the following six combustor analytical models, associated computer codes, and users manuals are given in this report.

- Annulus-flow model
- Combustor-performance model

- Liner-cooling model
- Transition-liner mixing model
- Emissions model
- Fuel-insertion model

The annulus-flow model is used to compute airflow distribution around the combustor liner and pressure drop. The information provided by this model on jet velocities and efflux angles is used for specifying the boundary conditions of the internal-flow computer models.

A 3-D reacting recirculating-flow model is used for computing internal profiles of velocity components, chemical species, and temperature of a given combustor design. Effects of detail-design changes can be analytically predicted in regard to combustion efficiency, exhaust temperature quality, and lean blowout.

Two-dimensional parabolic programs are used for predicting liner-wall-temperature levels, mixing rate in the combustor transition liner of reverse-flow annular combustors, and gaseous emissions. A fuel-insertion model is used to compute mean drop-let size and size distribution of pressure atomizers, including simplex, duplex, and air-assist pressure atomizers, and airblast nozzles. The model is also used to compute spray trajectory and evaporation rate of a given nozzle design in a specified flow field.

The use of these models is illustrated in Section IV by a worked-out illustration of a simple combustor.

II. DESCRIPTION OF ANALYTICAL MODELS

The six combustor analytical models are described in this section. The relevant computer codes are described in Section III. The use of these models is illustrated by an example in Section IV.

ANNULUS-FLOW MODEL

An annulus-flow model is used to compute pressure losses, annulus Mach number and associated air velocity, and airflow distribution around the combustor liner.

A one-dimensional analysis of the plenum annulus is conducted based upon the generalized one-dimensional continuous flow-analysis approach of Shapiro¹. The analysis considers the effect of area change, wall friction, drag introduced by inserted obstacles such as fuel nozzles and service struts, heat transfer from the liner wall, and injection or extraction of air from the annulus. The analysis is valid for constant specific heat and molecular weight.

Following the approach of Shapiro for a small control volume around a point P located at a distance "X" from the compressor discharge, as shown in Figure 1, the following three working relations are obtained for Mach number M, stagnation pressure P_0 , and static temperature T.

¹Shapiro, Ascher H., "The Dynamics and Thermodynamics of Compressible Fluid Flow, Vol. I", Chapter 8, The Ronald Press Company, New York (1953).

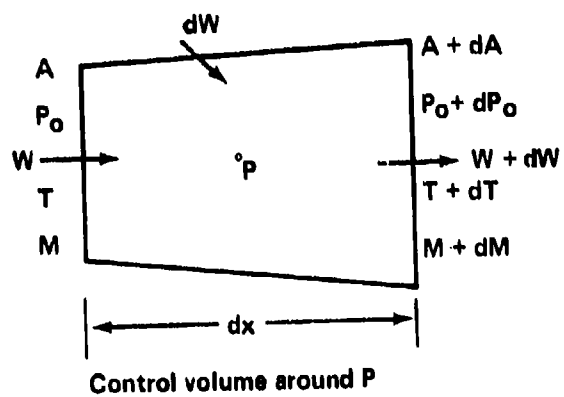
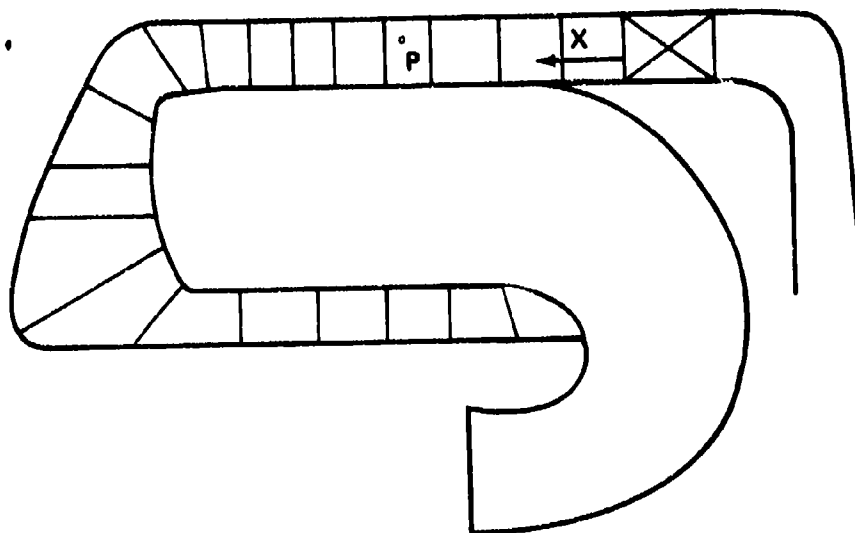


Figure 1. Control Volumes for Annulus-Flow Model.

$$\frac{dM^2}{M^2} = -2 \left(\frac{1+\gamma-1}{2} M^2 \right) \left[\frac{dA}{A} + \left(\frac{1+\gamma M^2}{2} \right) \frac{dT_O}{T_O} + \frac{\gamma M^2}{2} \left(4f \frac{dx}{D_H} + \frac{dF}{\frac{1}{2}\gamma p A M^2} - 2\gamma \frac{dW}{W} \right) + (1+\gamma M^2) \frac{dW}{W} \right] \quad (1)$$

$$\frac{dp_O}{p_O} = -\frac{\gamma M^2}{2} \left[\frac{dT_O}{T_O} + 4f \frac{dx}{D_H} + \frac{dF}{\frac{1}{2}\gamma p A M^2} + 2(1-\gamma) \frac{dW}{W} \right] \quad (2)$$

$$\begin{aligned} \frac{dT}{T} = & \frac{M^2}{1-M^2} \left[(\gamma-1) \frac{dA}{A} + \left(\frac{1-\gamma M^2}{M^2} \right) \left(\frac{1+\gamma-1}{2} M^2 \right) \frac{dT_O}{T_O} \right. \\ & - \frac{\gamma}{2} (\gamma-1) M^2 \left(4f \frac{dx}{D_H} + \frac{dF}{\frac{1}{2}\gamma p A M^2} - 2\gamma \frac{dW}{W} \right) \\ & \left. - (\gamma-1) (1+\gamma M^2) \frac{dW}{W} \right] \quad (3) \end{aligned}$$

Where:

A = Flow area

D_H = Mean hydraulic diameter

f = Coefficient of skin friction

F = Drag force by inserted obstacles

T = Static gas temperature

W = Mass flow rate

y = Injected mass axial velocity/mainstream velocity

γ = Ratio of specific heats

The above set of equations is written for each of the control volumes, shown schematically in Figure 1, applicable to a reverse-flow combustor geometry. Appropriate expressions are used for skin friction coefficient and drag introduced by fuel nozzles and other obstacles in the flow path. The remaining unknown variable dW , which will be negative for the flow through various orifices, is calculated by using the following approach.

The orifice configurations used in a combustor liner can be broadly divided into two basic categories.

- Configurations such as swirlers, primary pipes, and venturi sections which are either difficult to handle analytically or their flow rates are less affected by approach conditions.
- Liner orifices, including flush port, plunged holes, and scooped ports are affected by approach conditions and are amenable to analytical approach for predicting flow rates, jet velocities, and efflux angles.

The first type of ports are handled by specifying discharge coefficients, whereas the liner orifices are handled by using a modified analytical approach described by Gurevich². The Gurevich approach is based upon a 2-D potential flow solution of a problem shown schematically in Figure 2.

For an infinitely long slot of width b , the following three relations are obtained for the three unknowns, namely n , β and C_D .

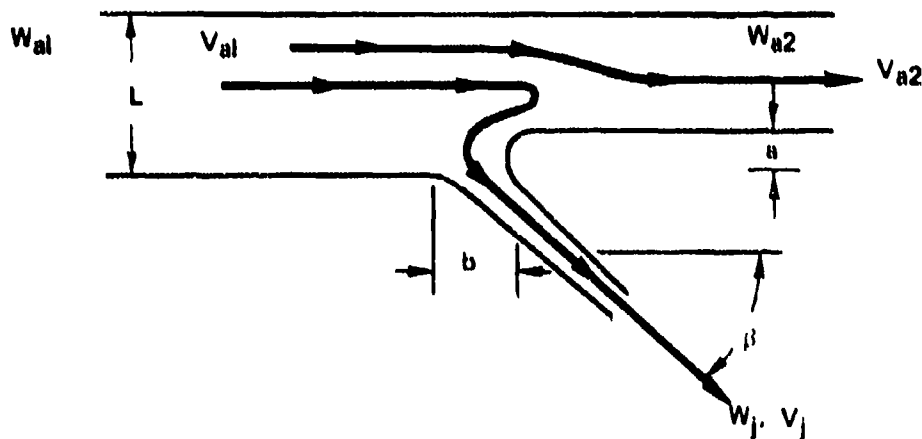
²Gurevich, M.I., "Theory of Jets in an Ideal Fluid", Pergamon Press, pp 52-59.

$$c = \cos\beta / (1 - \frac{1}{2n}) \quad (4)$$

$$\frac{b}{L} = \frac{1}{\pi} \left[\frac{\pi \sin\beta}{n} - \frac{\cos\beta}{n} \ln \left(\frac{1 + \cos\beta}{1 - \cos\beta} \right) + \frac{\left(1 - \frac{1}{2n}\right)^2 + \cos^2\beta}{\left(1 - \frac{1}{2n}\right) \cos\beta} \ln \left\{ \frac{\left(1 - \frac{1}{2n}\right) + \cos\beta}{\left(1 - \frac{1}{2n}\right) - \cos\beta} \right\} \right] \quad (5)$$

$$\frac{\left(1 - \frac{1}{2n}\right)^2 + \left(1 - \frac{1}{n}\right)^2 \cos^2\beta}{\left(1 - \frac{1}{2n}\right) \cos\beta} \ln \left\{ \frac{\left(1 - \frac{1}{2n}\right) + \left(1 - \frac{1}{n}\right) \cos\beta}{\left(1 - \frac{1}{2n}\right) - \left(1 - \frac{1}{n}\right) \cos\beta} \right\} \left[\frac{\cos\beta}{\left(1 - \frac{1}{2n}\right)} \right]$$

$$C_D = \frac{L}{b} \left(\frac{2 \cos\beta}{2n - 1} \right) \quad (6)$$



Where:

a/L = annulus width change/upstream width

b/L = slot width/upstream annulus width

n = annulus upstream flow rate/slot flow rate, W_{a1}/W_j

c = upstream annulus velocity/slot velocity, V_{a1}/V_j

β = jet efflux angle

C_D = discharge coefficient

Figure 2. Liner Port Model Schematic.

These equations are applied to combustor liner orifices by maintaining area similarity through the following relationships:

$$b/L = A_H/A_{ea}$$

where A_H = orifice area ($= \frac{\pi}{4} D^2$ for circular hole)

A_{ea} = effective annulus area with boundary-layer
blockage effects

For a given application, the annulus upstream conditions and the static pressure inside the combustor must be specified. With the above equations, an orifice can be sized to pass a specified flow rate, or the flow through a specified orifice can be calculated. The procedure for each is outlined as follows.

For given values of annulus and orifice flow rates and velocities, c can be calculated and then the efflux angle can be found from Equation 4. For the special case where all annulus flow passes through the orifice, $n = 1$ and

$$\cos \beta = c/2$$

If the orifice flow is a negligible portion of the annulus flow, n approaches infinity,

$$\cos \beta = c$$

After the value of β is obtained, Equation 5 can be used to calculate b/L and A_H/A_{ea} from Equation 7; then from Equation 6, C_D can be calculated.

For the alternate problem, with the orifice specified, the above procedure is used in an iterative solution starting with an estimated flow rate (value of n). The iteration is continued until n converges to a small difference between iterations.

Such an approach has given good correlation with measure C_D^3 data of the circular orifices, as shown typically in Figure 3. For plunged orifices and the metering orifices of film-cooling geometries, the approach gave only qualitative agreement. However, by multiplying the computed C_D values by 1.48 and 1.4, and by assuming β equal to 80- and 0-degrees, respectively, for the plunged orifices and the cooling slot, the approach gave good agreement with the data, as shown in Figure 3.

With the above procedure for computing dW appearing in Equations 1, 2, and 3, it is now possible to write a set of equations for each of the control volumes around the combustor liner, as shown schematically in Figure 1. These equations are solved iteratively to compute isothermal combustor-pressure drop. To this can be added pressure drop due to heat addition which gives combustor total pressure drop.

3-D COMBUSTOR PERFORMANCE MODEL

A 3-D elliptic, reacting-flow model is used for calculating internal flow field of gas turbine combustors. The model solves governing equations for the following variables, as described in Paragraph 6 below:

- Axial, radial, and swirl velocity components
- Specific enthalpy and temperature
- Turbulence kinetic energy and dissipation rate

³Hunter, S. C., K. M. Johansen, H. C. Mongia, and M. P. Wood, "Advanced, Small, High-Temperature-Rise Combustor Program, Volume II: Analytical Mode Derivation and Combustor-Element Rig Tests (Phases I and II)", AD778766 (1974).

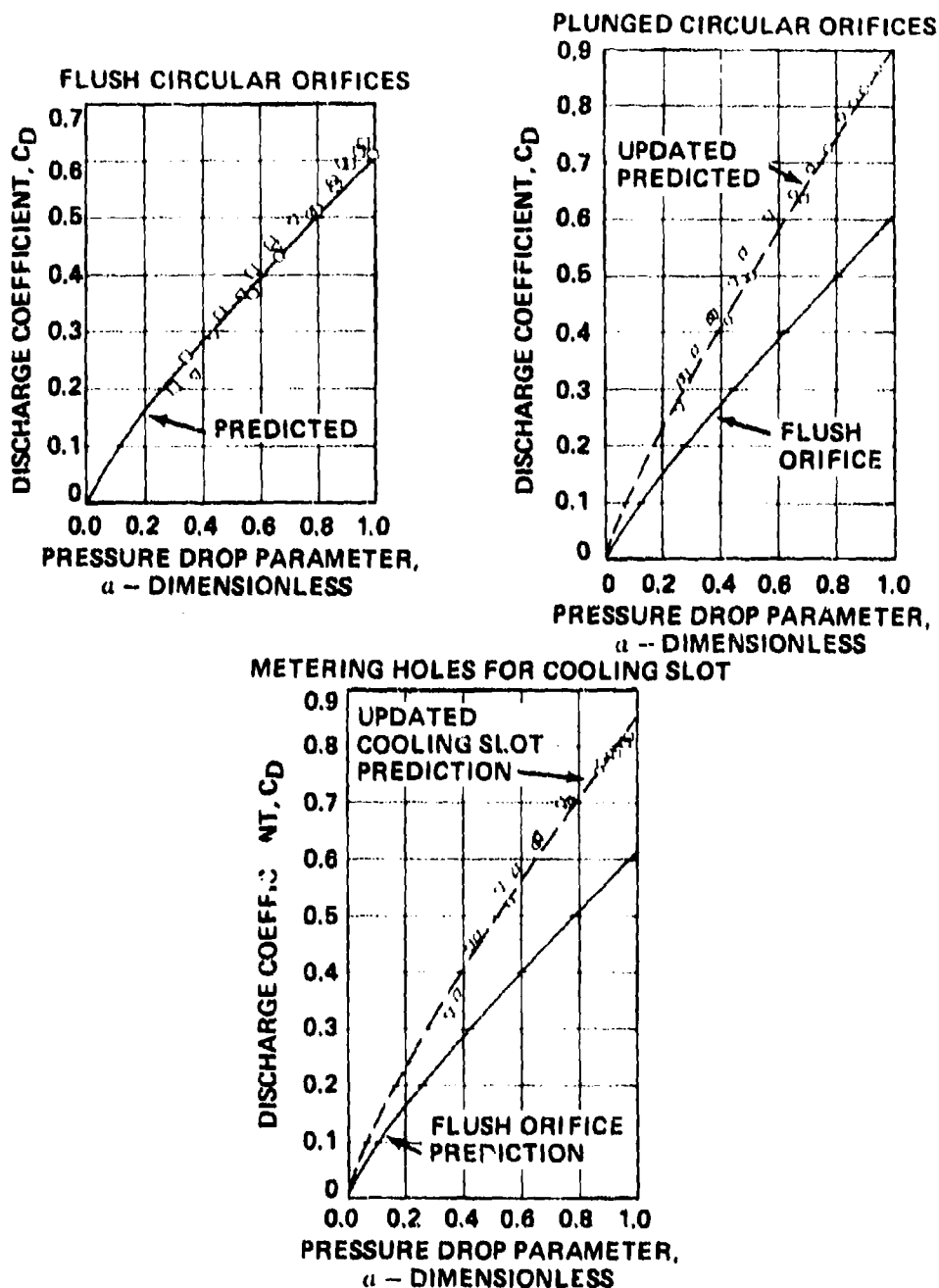


Figure 3. A Typical Comparison Between Prediction and Measured C_D .

- Unburned fuel, CO, and composite fuel fraction
- Radiation-flux vectors
- Spray combustion

Paragraphs 7 and 8 below give a brief description of the boundary conditions and the numerical scheme used for solving the set of nonlinear coupled partial differential equations.

1. Equations of Continuity, Momentum, and Enthalpy.

a. Continuity.

$$\text{div} (\rho \vec{V}) = \dot{m}_{\text{spray}} \quad (8)$$

b. x-Momentum.

$$\begin{aligned} \text{div} (\rho \vec{V} u - \mu_{\text{eff}} \text{grad } u) = & - \frac{\partial p}{\partial x} - \frac{2}{3} \frac{\partial}{\partial x} (\mu_{\text{eff}} \text{div } \vec{V}) \\ & + \frac{\partial}{\partial x} (\mu_{\text{eff}} \frac{\partial u}{\partial x}) + \frac{1}{r} \frac{\partial}{\partial r} (\mu_{\text{eff}} r \frac{\partial v}{\partial x}) + \frac{1}{r} \frac{\partial}{\partial \theta} (\mu_{\text{eff}} \frac{\partial w}{\partial x}) \\ & + S_{\text{spray}}^u \end{aligned} \quad (9)$$

c. y-Momentum.

$$\begin{aligned} \text{div} (\rho \vec{V} v - \mu_{\text{eff}} \text{grad } v) = & - \frac{\partial p}{\partial r} - \frac{2}{3} \frac{\partial}{\partial r} (\mu_{\text{eff}} \text{div } \vec{V}) \\ & + \frac{\partial}{\partial x} (\mu_{\text{eff}} \frac{\partial u}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial r} (\mu_{\text{eff}} r \frac{\partial v}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial \theta} [\mu_{\text{eff}} (\frac{\partial w}{\partial r} - \frac{w}{r})] \\ & - 2 \frac{\mu_{\text{eff}}}{r} (\frac{1}{r} \frac{\partial w}{\partial \theta} + \frac{v}{r}) + \frac{\rho w^2}{r} + S_{\text{spray}}^v \end{aligned} \quad (10)$$

d. θ -Momentum.

$$\begin{aligned} \text{div } (\rho \vec{V} w - \mu_{\text{eff}} \text{grad } w) = & - \frac{1}{r} \frac{\partial p}{\partial \theta} - \frac{2}{3} r \frac{\partial}{\partial \theta} (\mu_{\text{eff}} \text{div } \vec{V}) \\ & + \frac{\partial}{\partial x} \left(\frac{\mu_{\text{eff}}}{r} \frac{\partial u}{\partial \theta} \right) + \frac{1}{r} \frac{\partial}{\partial r} [\mu_{\text{eff}} r \left(\frac{1}{r} \frac{\partial v}{\partial \theta} - \frac{w}{r} \right)] \\ & + \frac{1}{r} \frac{\partial}{\partial \theta} \left[\frac{\mu_{\text{eff}}}{r} \left(\frac{\partial w}{\partial \theta} + 2v \right) \right] - \frac{\rho v w}{r} + \frac{\mu_{\text{eff}}}{r} \left(\frac{\partial w}{\partial r} + \frac{\partial v}{r \partial \theta} - \frac{w}{r} \right) \quad (11) \\ & + S_{\text{spray}}^w \end{aligned}$$

e. Specific enthalpy.

$$\text{div } (\rho \vec{V} h - \frac{\mu_{\text{eff}}}{P r_{\text{eff}}} \text{grad } h) = S_h \quad (12)$$

where

S_h represents the sum of all the enthalpy source terms for radiation and spray evaporation

Definition of variables are:

\vec{V} = Net gas velocity vector

u, v, w = Velocity components along x , radial and circumferential directions

x, y, θ = Axial, radial and circumferential coordinates

p = Static pressure

h = Static specific enthalpy

$S_{\text{spray}}^u, S_{\text{spray}}^v, S_{\text{spray}}^w$ = Momentum transfer from spray to the gas phase u , v and w - momentum equations

$\dot{m}'_{\text{spray}} = \text{spray evaporation/combustion rate per unit volume}$

$$\text{div} (\rho \vec{v} \phi) = \frac{1}{r} \left[\frac{\partial}{\partial x} (r \rho u \phi) + \frac{\partial}{\partial r} (r \rho v \phi) + \frac{\partial}{\partial \theta} (r \rho w \phi) \right]$$

$$\text{div} (\mu \text{grad } \phi) = \frac{1}{r} \left[\frac{\partial}{\partial x} (r \mu \frac{\partial \phi}{\partial x}) + \frac{\partial}{\partial r} (r \mu \frac{\partial \phi}{\partial r}) + \frac{\partial}{\partial \theta} (\frac{\mu}{r} \frac{\partial \phi}{\partial \theta}) \right]$$

The effective viscosity μ_{eff} is given by $\mu_{\text{eff}} = \mu_l + \mu_t$

where μ_l and μ_t are the molecular and turbulent viscosities of the fluid, respectively.

2. Turbulence Model.

The turbulent viscosity μ_t is calculated by using a two-equation turbulence model that solves governing equations for the turbulence kinetic energy (k) and the dissipation rate (ϵ). The governing equations for k and ϵ are:

$$\text{div} (\rho \vec{v} k - \Gamma_{k,\text{eff}} \text{grad } k) = G_k - \rho \epsilon \quad (13)$$

$$\text{div} (\rho \vec{v} \epsilon - \Gamma_{\epsilon,\text{eff}} \text{grad } \epsilon) = (C_1 G_k - C_2 \rho \epsilon) \frac{\epsilon}{k} \quad (14)$$

where

$$G_k = \mu_t \left[2 \left\{ \left(\frac{\partial u}{\partial x} \right)^2 + \left(\frac{\partial v}{\partial r} \right)^2 + \left(\frac{\partial w}{r \partial \theta} + \frac{v}{r} \right)^2 \right\} + \left(\frac{\partial w}{\partial x} + \frac{\partial u}{r \partial \theta} \right)^2 + \left(\frac{\partial u}{\partial r} + \frac{\partial v}{\partial x} \right)^2 + \left(\frac{\partial w}{\partial r} + \frac{\partial v}{r \partial \theta} - \frac{w}{r} \right)^2 \right] \quad (15)$$

$$\Gamma_{k,\text{eff}} = \mu_{\text{eff}} / \sigma_{k,\text{eff}} \quad (16)$$

$$\Gamma_{\epsilon,\text{eff}} = \mu_{\text{eff}} / \sigma_{\epsilon,\text{eff}}$$

$$\mu_t = C_D \rho k^2 / \epsilon$$

C_D , C_1 , and C_2 are constants. $\Gamma_{k,eff}$, $\Gamma_{\epsilon,eff}$, $\sigma_{k,eff}$ and $\sigma_{\epsilon,eff}$ are the effective exchange coefficients and Schmidt numbers for k and ϵ , respectively.

The k - ϵ turbulence model is moderate in complexity and is considered to be superior to other models having a similar degree of complexity. This model has been extensively used by many investigators and has proved to be adequate in a wide range of flow conditions. More advanced turbulence models, such as those based upon the Reynolds-stress modeling approach, are not yet fully developed to warrant their use in recirculating flow-field problems as encountered in gas-turbine combustors. In addition, such an approach will appreciably increase the computation effort.

Recommended values for the constants appearing in the above equations are

$$C_D = 0.09$$

$$C_1 = 1.44$$

$$C_2 = 1.92$$

$$\sigma_{k,eff} = 0.9$$

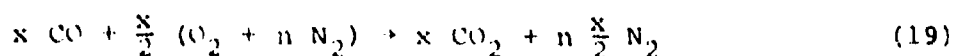
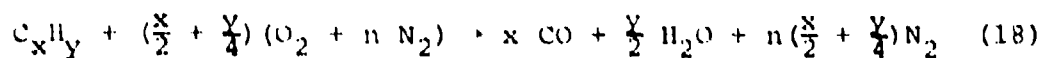
$\sigma_{\epsilon,eff}$ is calculated from

$$\sigma_{\epsilon,eff} = \frac{k^2}{(C_2 - C_1) C_D^{1/2}}$$

where k is the vonKarman constant taken to be equal to 0.42.

3. Chemical Species Equations.

A two-step kinetic scheme is used as represented by Equations 18 and 19.

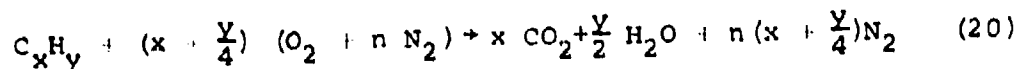


Stoichiometric oxygen-to-fuel and oxygen-to-CO ratios for the first and the second reactions are given by

$$i_1 = \frac{32 \left(\frac{x}{2} + \frac{y}{4} \right)}{(12x + y)}$$

$$i_2 = 0.571$$

Combining Equations 18 and 19, one obtains overall stoichiometry equation as



The corresponding stoichiometric oxygen-to-fuel ratio is

$$i = \frac{32 \left(x + \frac{y}{4}\right)}{(12x + y)}$$

Governing equations for fuel and CO mass fractions are:

$$\text{div} (\rho \vec{v} m_{fu} - \Gamma_{fu, \text{eff}} \text{grad } m_{fu}) = \dot{m}'_{\text{evap}} - R_{fu} \quad (21)$$

$$\text{div} (\rho \vec{v} m_{CO} - \Gamma_{CO, \text{eff}} \text{grad } m_{CO}) = -R_{CO} \quad (22)$$

where R_{fu} and R_{CO} are rate of oxidation of fuel and CO in accordance with the combustion model explained in paragraph a. \dot{m}'_{evap} is the rate of spray evaporation per unit volume computed in accordance with the spray combustion model description in Paragraph 5.

Equations similar to the above are required for O_2 , CO_2 , and H_2O . However, by using Shvab-Zeldovich approximation⁴, one needs to solve only one more equation for composite fuel fraction,

$$\phi_{fuox}$$

⁴Williams, F. A., "Combustion Theory", Addison-Wesley Publishing Company, Inc. (1965).

$$\text{div } (\rho \vec{v} \phi_{\text{fuox}} - l'_{\text{fuox}} \phi_{\text{fuox}}) = \dot{m}'_{\text{evap}} \quad (23)$$

$$\text{where } \phi_{\text{fuox}} = \frac{\phi - \phi_A}{\phi_F - \phi_A}$$

$$\text{where } \phi = m_{\text{fu}} - \frac{m_{\text{ox}}}{i}$$

ϕ_A and ϕ_F are the values of ϕ for air and fuel streams, respectively.

Knowing the amount of fuel burned ($\text{FB} = \phi_{\text{fuox}} - m_{\text{fu}}$), the concentrations of CO_2 , O_2 , and H_2O are given by

$$m_{\text{CO}_2} = 44 \frac{x \text{ FB}}{(12 + y)} - \frac{44}{28} m_{\text{CO}}$$

$$m_{\text{ox}} = i m_{\text{fu}} + i_2 m_{\text{CO}} + 0.232 - (0.232 + i) \phi_{\text{fuox}}$$

$$m_{\text{H}_2\text{O}} = \frac{18 y \text{ FB}}{2 (12 + y)}$$

Mass fraction of N_2 is given by

$$m_{\text{N}_2} = 1 - (m_{\text{ox}} + m_{\text{fu}} + m_{\text{CO}} + m_{\text{CO}_2} + m_{\text{H}_2\text{O}})$$

a. Calculation of Reaction Rates.

Equations are needed for oxidation rates of fuel and CO , i.e., R_{fu} and R_{CO} . The turbulent reactive flow is an area of intensive research, and a number of models have been proposed to predict burning rate of fuel in turbulent environments. A simple model is used in the present study as explained in the following paragraphs.

The rate of oxidation of fuel is determined by the minimum of the following three equations:

$$R_{fu, ch} = k_1 \rho^{1.5} m_{ox} m_{fu}^{\frac{1}{2}} e^{-\left(\frac{E_1}{R_T}\right)} \quad (24a)$$

$$R_{fu, turb} = C_{R_1} \rho m_{fu} \epsilon/k \quad (24b)$$

$$R_{fuox, turb} = C_{R_1} \rho \frac{m_{ox}}{i_1} \epsilon/k \quad (24c)$$

Here, Equation 24a is the rate of fuel oxidation as controlled by chemical kinetics. Generally, a bimolecular Arrhenous expression is assumed for this reaction. However, the Task I reacting-flow mapping data was best correlated by using Equation 24a in conjunction with Equations 24b and 24c.

Equation 24b is based upon the eddy-breakup model of Spalding⁵ and expresses the rate of fuel oxidation as influenced by turbulence intensity and scale, and concentration of unburned fuel. This model is applicable to premixed flames. Since combustion in gas-turbine combustors is neither fully premixed nor entirely diffusion controlled, Equation 24c is postulated, similar to Equation 24, which determines the rate of fuel oxidation as controlled by the availability of the oxygen. The constant i_1 appears from stoichiometry of the chemical Equation 18. One could use i instead of i_1 without any loss of generality, because the empirical constant C_{R_1} will simply be different.

The rate of oxidation of CO is similarly the minimum of the following three equations:

$$R_{CO, ch} = k_2 \rho^2 m_{CO} m_{ox} e^{-\left(\frac{E_2}{R_T}\right)} \quad (25a)$$

$$R_{CO, turb} = C_{R_2} \rho m_{CO} \epsilon/k \quad (25b)$$

$$R_{COox, turb} = C_{R_2} \rho \frac{m_{ox}}{i_2} \epsilon/k \quad (25c)$$

⁵Spalding, D. B., "Mixing and Chemical Reaction in Steady Confined Turbulent Flames", Thirteenth Symposium (International) on Combustion, The Combustion Institute, 1971.

4. Radiation Model.

A six-flux radiation model based upon the Schuster-Hamaker approximation^{6,7} is used in the present program. It should be noted that, as pointed out by Siddall,⁸ other flux model approximations such as Milne-Eddington and Schuster-Schwarzschild can be represented by the same form of flux equations with constants being different. Therefore, the user can modify the flux equations with relative ease.

The differential equations describing the variations of the fluxes along the six directions are:

$$\frac{d}{dx} (I_{x+}) = - (a + s) I_{x+} + aE + \frac{s}{6} I \quad (26)$$

$$\frac{d}{dx} (I_{x-}) = - (a + s) I_{x-} - aE - \frac{s}{6} I \quad (27)$$

$$\frac{1}{r} \frac{d}{dr} (r I_{r+}) = - (a + s) I_{r+} + \frac{I_{r-}}{r} + aE + \frac{s}{6} I \quad (28)$$

$$\frac{1}{r} \frac{d}{dr} (r I_{r-}) = - (a + s) I_{r-} + \frac{I_{r+}}{r} - aE - \frac{s}{6} I \quad (29)$$

$$\frac{1}{r} \frac{d}{d\theta} (I_{\theta+}) = - (a + s) I_{\theta+} + aE + \frac{s}{6} I \quad (30)$$

$$\frac{1}{r} \frac{d}{d\theta} (I_{\theta-}) = - (a + s) I_{\theta-} - aE - \frac{s}{6} I \quad (31)$$

⁶Hamaker, H. C., "Radiation and Heat Conduction in Light-Scattering Material", Philips Research Report, Vol. 2, pp 55-67, 1947.

⁷Patankar, S. V., and D. B. Spalding, "A Computer Model for Three-Dimensional Flow in Furnaces", Fourteenth Symposium (International) on Combustion, The Combustion Institute, 1973.

⁸Siddall, R. G., "Flux Methods for the Analysis of Radiant Heat Transfer", Paper presented at the Fourth Symposium on Flames and Industry, 1972.

where I_{x+} , I_{r+} , and $I_{\theta+}$ are the fluxes along the positive directions of axial, radial and circumferential directions, respectively; I_{x-} , I_{r-} , and $I_{\theta-}$ are the corresponding fluxes along the negative directions.

a = absorption coefficient defined as radiation absorbed per unit length

s = scattering coefficient defined as radiation scattered per unit length

E = black body emissive power = σT^4

where σ is the Stefan-Boltzman constant

$$I = I_{x+} + I_{x-} + I_{r+} + I_{r-} + I_{\theta+} + I_{\theta-}$$

With the composite-fluxes R^x , R^r and R^z defined as:

$$R^x = \frac{1}{2} (I_{x+} + I_{x-})$$

$$R^r = \frac{1}{2} (I_{r+} + I_{r-})$$

$$R^z = \frac{1}{2} (I_{\theta+} + I_{\theta-})$$

one can reduce the six first-order flux equations into the following three second-order equations:

$$\frac{d}{dx} \left(\frac{1}{a+s} \frac{dR^x}{dx} \right) = a (R^x - E) + \frac{s}{3} (2R^x - R^r - R^z) \quad (32)$$

$$\frac{1}{r} \frac{d}{dr} \left(\frac{r}{a+s+\frac{1}{r}} \frac{dR^r}{dr} \right) = a (R^r - E) + \frac{s}{3} (2R^r - R^x - R^z) \quad (33)$$

$$\frac{1}{r} \frac{d}{d\theta} \left(\frac{1}{a+s} \frac{dR^z}{d\theta} \right) = a (R^z - E) + \frac{s}{3} (2R^z - R^x - R^r) \quad (34)$$

Once R^x , R^r , and R^z are known, the net radiation fluxes in the axial, radial, and circumferential directions, Q^x , Q^r , and Q^z respectively, are given by:

$$\begin{aligned} Q^x &= I_{x+} - I_{x-} \\ &= - \frac{2}{a+s} \frac{dR^x}{dx} \end{aligned} \quad (35)$$

$$\begin{aligned} Q^r &= I_{r+} - I_{r-} \\ &= - \frac{2}{a + s + \frac{1}{r}} \frac{dR^r}{dr} \end{aligned} \quad (36)$$

$$\begin{aligned} Q^z &= I_{\theta+} - I_{\theta-} \\ &= \frac{2}{a+s} \frac{1}{r} \frac{dR^z}{d\theta} \end{aligned} \quad (37)$$

The contribution of R^x , R^r , and R^z to the source terms of specific enthalpy, Equation 12, is given by:

$$\begin{aligned} (S_h)_{\text{radiation}} &= 2a [(R^x - E) + \\ &\quad (R^r - E) + \\ &\quad (R^z - E)] \end{aligned} \quad (38)$$

Since information on the variations of a and s (with other quantities such as concentrations of CO , H_2O , CO and soot particles) is often scarce and unprecise, they have been assumed to be uniform. However, variable values of a and s can be incorporated in the program with minor modifications.

5. Spray Combustion.

It is very important to predict aerodynamic interaction between evaporating/burning sprays and flow field insofar as combustion efficiency, pattern factor, stability, liner-wall temperature levels and gradients, smoke and gaseous emissions formation are concerned. For example, the presence of smaller droplets influence flame stabilization as they provide the main source of heat in the recirculation zone. Larger droplets, however, escape the recirculation zone and are mainly responsible for the smoke formation. Measured data by McCreath and Chigier⁹ showed that droplets with initial sizes less than 50 microns were evaporated in the recirculation zone. The smaller droplets were influenced greatly by the recirculation zone velocity field, whereas up to 70 percent of the bigger droplets in the 100-200 microns range escaped the recirculation zone. Their trajectory was not influenced by the flow-field velocity distribution. The flow-field influence on evaporation and trajectory of medium-size droplets, between 50 and 100 microns, was moderate.

Combustion characteristics of liquid droplets burning individually are significantly different from those burning collectively in a spray. For example, Beer and his associates¹⁰ showed that the burning-rate constant of monosized droplet arrays was about half that of single droplets. There was also significant reduction^{10,11} in drag coefficient, C_D , as compared to that of a

⁹McCreath, C. G. and N. A. Chigier, "Liquid Spray Burning in the Wake of a Stabilizer Disc", Fourteenth Symposium (International) on Combustion, The Combustion Institute (1973).

¹⁰Nuruzzaman, A. S. M., A. B. Hedley, and J. M. Beer, "Combustion of Monosized Droplet Streams in Self-Supporting Flames", Thirteenth Symposium (International) on Combustion, The Combustion Institute (1971).

¹¹Chigier, N. A., et. al, "Dynamics of Droplets in Burning and Isothermal Sprays", Combustion and Flame, V23 (1974).

nonreactive sphere. On the other hand, Natarajan¹² showed that C_D of a burning droplet should be calculated for a nonreacting sphere at the mean properties and initial diameter.

The quasi-steady droplet combustion theory with spherical symmetry predicts the burning rate constant K to be independent of the surrounding gas pressure, where $K = -\frac{d}{dt} d_L^2$, and d_L is the liquid-droplet diameter. However, it has been found experimentally¹³ that K increases with an increase in pressure. Raghunandan and Mukunda¹⁴ critically evaluated the quasi-steady approximation, variable gas phase properties and incomplete combustion as related to predictions of burning-rate constant, the flame-to-diameter ratio and the flame temperature. The liquid-phase unsteadiness lasts for about 20-25 percent of the total burning time. It was shown by the authors that a good correlation with the burning rate data could be obtained by taking thermal conductivity and C_D as a function of concentration and temperature.

A majority of the reported work has been concerned with combustion of single component hydrocarbon fuels. Limited work has been reported, such as Reference 15, for combustion of multi-component fuel droplets; but, these approaches became quite complicated for predicting spray combustion of complex fuels like jet aviation fuels.

¹²Natarajan, R., "Experimental Drag Coefficients for Evaporating and Burning Drops at Elevated Pressures", Combustion and Flame, V20 (1973).

¹³Rush, J. H., and H. Krier, "Burning of Fuel Droplets at Pressures Greater than Atmospheric", Combustion and Flame V22 (1974).

¹⁴Raghunandan, B. N., and H. S. Mukunda, "The Problem of Liquid Droplet Combustion - Reexamination", Combustion and Flame V30 (1977).

¹⁵Shyu, R. R., C. S. Chen, G. O. Gondie and M. M. Elwakil, "Multi-Component Heavy Fuel Drop Histories in a High Temperature Flow Field", Fuel, V51 (1972).

Figure 4 pictorially presents the approach that has been used for spray combustion in the present program. The spray cone is divided into a number of sections or rays. Each ray has a particular x, y, and z direction associated with it, depending on the orientation of the fuel nozzle in the combustor and the spray cone angle.

The initial conditions for each droplet are that they have a velocity as specified by the program user and a direction corresponding to the particular ray in question. The total fuel-flow rate is currently divided equally among the rays, although it would be easily possible to do otherwise. For each ray and for each droplet size group, of which five are assumed, the droplet trajectories are calculated from a force balance assuming the drag on the droplet is for that of a sphere. Heat transfer to the droplet is calculated using the coefficient given in Equation 39.

$$h = 2 \frac{k}{D} (1 + 0.3 Pr^{\frac{1}{3}} Re^{\frac{1}{2}}) \left(\frac{J}{m^2 - K} \right) \quad (39)$$

where k is the thermal conductivity of fuel vapor, Re is Reynolds number based on relative velocity, and D is the droplet diameter. Until the droplet reaches the boiling temperature, no evaporation is assumed to occur; however, once reached, the evaporation rate is obtained from the burning rate constant k . Where:

$$k_o = \frac{d}{dt} (D^2)$$

$$k_o = \frac{8}{\rho_f} \frac{1}{C_{P1}} \ln(1+B)$$

$$B = \text{mass transfer No.} = \frac{1}{L_{\text{vap}}} \left[m_{O_2} \frac{H_c}{i} + C_{P1} (T_{\infty} - T_{\mu}) \right]$$

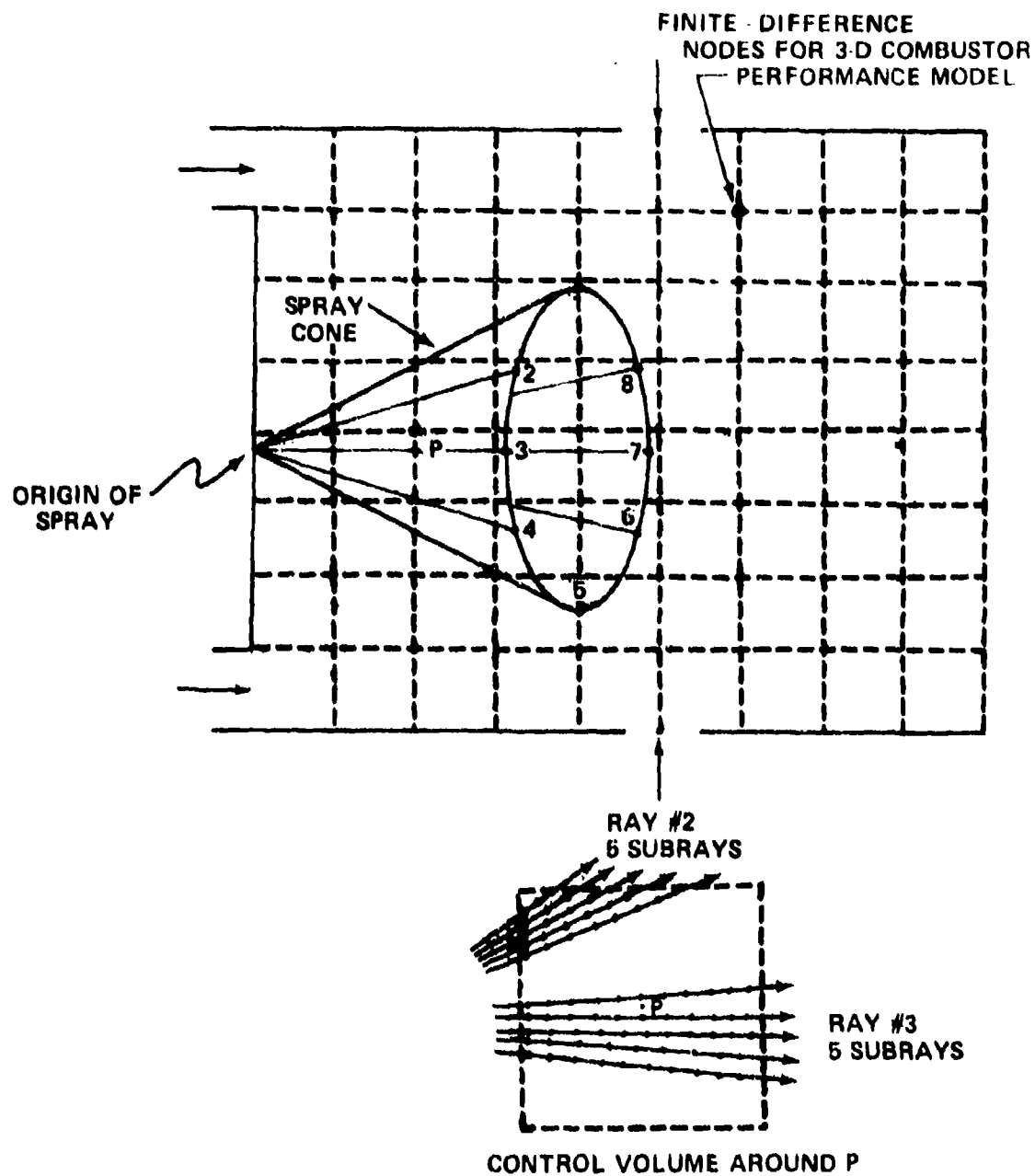


Figure 4. Schematic of Spray in Combustor Flow Field.

H_c = Heat of combustion

i = Stoichiometric O_2 -fuel mass ratio

L_{vap} = Latent heat of vaporization

ρ_f = Liquid fuel density

λ_1 and (CP_1) the thermal conductivity and specific heat inside the flame zone, are assumed to be

$$\lambda_1 = 0.4\lambda_f + 0.6 \lambda_{AIR}$$

$$CP_1 = CP_f$$

and are evaluated at the average of the boiling and flame temperatures. These calculations are performed explicitly, with care taken that the time step is sufficiently small, until at least 99 percent of the fuel has evaporated.

The above procedure requires knowledge of the fuel and air properties. The particular values used in the current program are listed below.

a. Droplet-Size Distribution.

<u>Group</u>	<u>Vol. % of Spray</u>	<u>Size Ratio (D/SMD)</u>
1	0-20	0.6
2	20-40	0.9
3	40-60	1.2
4	60-80	1.5
5	80-100	2.1

b. Liquid-Fuel Density (ρ_f).

$$\rho_f = 1000 [PR_{60} + 0.208 - 0.00072 T_f] \frac{KG}{m^3}$$

$$PR_{60} = \frac{1.076}{1 + \frac{1.076}{0.775} - 1 (1 - 0.67F)} \text{ for JP4}$$

PR_{60} = Specific gravity of residue at 60°F

F = Fraction evaporated

T_f = Fuel temperature

c. Specific Heat of Liquid Fuel (CP_f).

$$CP_f = 840.5 + 4.1372 T_f \text{ (J/KG } \cdot \text{ } ^\circ K)$$

d. Molecular Weight of Fuel Vapor.

Interpolated from table below,

<u>F</u>	<u>MW(JP4)</u>
0	93.26
0.1	114.60
0.3	126.61
0.5	138.16
0.7	150.59
0.9	173.21
1.0	204.76

e. Thermal Conductivity of Fuel Vapor (λ_f).

$$\lambda_f = 1.729 (A + BT_f) \text{ (j/M-}^\circ K\text{-Sec)}$$

where A and B are from the following list:

<u>MW_{fuel}</u>	<u>A</u>	<u>B</u>
50	-6.362E-3	53.5E-6
100	-6.358E-3	49.1E-6
150	-6.284E-3	46.6E-6
300	-6.010E-3	42.3E-6

f. Specific Heat of Fuel Vapor (CP_{f_v}).

$$CP_{f_v} = 4183.3 (0.153 + 0.00081T_f) \left(\frac{J}{KG-^{\circ}K} \right)$$

g. Latent Heat of Vaporization (L_{vap}).

$$L_{vap} = 30676.6 (1092.88 - 1.8T_f)^{.39} \quad (J/KG)$$

h. Boiling Temperature of Fuel (T_B).

$$T_B = A \ln P_v + B \quad (^{\circ}K)$$

where P_v is vapor pressure in pascals, A and B are from the following list:

<u>% Evaporated</u>	<u>A</u>	<u>B</u>
0	41.026	-114.000
10	30.857	41.574
30	27.348	96.534
50	23.997	146.567

The spray calculation procedure is briefly described in the following paragraph. Referring to Figure 4, the analysis is done for each of the rays selected and their subrays. Details are given for the control volume around a point P, where it is shown for two typical rays identified as Ray No. 2 and Ray No. 3. With each of these rays there might be five subrays, or less, depending upon the location of point P, initial droplet sizes, and the properties of the field through which the individual drops have traveled. Depending upon the direction of the ray and the

finite-difference nodal volume, calculations for evaporation/burning are done for a number of subgrid points. The droplets are allowed to exchange mass, momentum, and energy with the surrounding gas phase. The net amount of mass, energy, and momentum received by the node P is the sum total of all droplets passing through the control volume of P.

6. Calculation of Gas Temperature.

With the specific enthalpy and chemical species known, the gas temperature is calculated as follows: The specific enthalpy h is the summation of the enthalpies of individual species, i.e.,

$$\begin{aligned} h &= \sum_i m_i h_i \\ &= \sum_i m_i \left[h_{i,0} + \int_{T_0}^T c_{pi}(T) dT \right] \\ &= \sum_i m_i \left[h_{i,0} + \int_{T_0}^{T^*} c_{pi}(T) dT + \int_{T^*}^T c_{pi}(T) dT \right] \end{aligned}$$

Thus, giving

$$h = \sum_i m_i [h_i(T^*) + c_{pi}(T^*)(T - T^*)] \quad (47)$$

where m_i , h_i , $h_{i,0}$, c_{pi} , T^* , and T are species mass fraction, specific enthalpy, heat of formation at a reference temperature T_0 , isobaric specific heat, gas temperature of the previous iteration, and the unknown gas temperature, respectively.

Therefore, from Equation 47 one obtains the following expression for the gas temperature T :

$$T = T^* + \left[\frac{h - \sum_i m_i h_i(T^*)}{\sum_i m_i c_{pi}(T^*)} \right] \quad (48)$$

The variation of C_p as a function of temperature is taken as a fourth-order polynomial of temperature as given in Reference 16.

7. Finite-Difference Solution of the Equations.

The numerical solution of the nonlinear, coupled, partial differential equations can be obtained by using finite-difference methods. A numerical solution of the hydrodynamic equations can be obtained by two methods. The earlier approach employed for 2-D flows was the so-called streamline-vorticity method³. Here pressure is replaced from the momentum equations by differentiation. Stream function (ψ) and vorticity (ω) replace the velocity components and the pressure, thus requiring solution of only two instead of three variables: namely, u , v , and p . The equations were solved by a point-by-point successive-substitution procedure. Since ψ and ω are linked at the boundaries by way of the no-slip condition, the ω boundary specification could be done a number of ways leading to considerably different false diffusion levels as recently evaluated by de Vahl, Davis, and Mallinson¹⁷. In addition, problems were encountered in obtaining fully converging solutions with nonuniform grid spacing. Since 1973, AiResearch has used a pressure-velocity (primitive variable) solution approach, which has the following three advantages over the $\psi - \omega$ method:

- It permits computation of variable density flows where ρ depends upon pressure and temperature.

¹⁶Gordon, S., and B. J. McBride, "Computer Program for Calculation of Complex Chemical Equilibrium Compositions, Rocket Performance, Incident and Reflected Shocks and Chapman-Jouguet Detonations", NASA SP-273 (1971).

¹⁷de Vahl, Davis, and G. D. Mallinson, "An Evaluation of Upwind and Central Difference Approximations by a Study of Recirculating Flow", Computers and Fluids (1976).

- It allows unsteady flows to be calculated as easily as steady ones.
- It works for 3-D flows as well as 2-D flows, whereas the $\psi - \omega$ method cannot be easily extended.

Many primitive variable solution methods have been put forward by different researchers¹⁸. They vary enormously in complexity, ease of use, efficiency, and applicability. The 3-D combustor performance code is based on the well-tried SIMPLE (Semi-Implicit Method for Pressure-Linked Equations) algorithm of Patankar and Spalding as described in Reference 19. The features of the computer model include:

- Solution of sufficiently general single form differential equations
- Provision for use with different physical models
- Use of pressure and velocities as the main hydrodynamic variables
- Use of the pressure correction technique
- Provision of two coordinate (plane and axisymmetric) systems
- Use of nonuniformly spaced grids

¹⁸Anon., "Proceedings of the Third AIAA Computational Fluid Dynamics Conference", Albuquerque, New Mexico, June 27-28, 1977.

¹⁹Patankar, S. V., "Numerical Prediction of Three-Dimensional Flows", in Studies in Convection: Theory, Measurement and Application, Volume 1, Edited by B. E. Launder, Academic Press, 1975.

- Use of staggered grid with attendant minimum truncation errors
- Derivation of finite-difference equations by integrating the differential equations over finite control volumes and thus ensuring mathematical compatibility between the finite difference and the original differential-equation formulations
- Efficient line-by-line tri-diagonal matrix solution of the difference equations
- Unconditional convergence for all Reynolds numbers
- Provision for under-relaxation

A typical grid node spacing is shown in Figure 5. Finite-difference equations for a node are obtained by integrating the differential equations over a control volume enclosing a grid node. For evaluating the convection and diffusion fluxes through a control volume face, a linear variation (in the direction normal to the face) of the flow properties is assumed. For other purposes, a step-wise variation with discontinuities at control-volume boundaries is assumed. Net rate of flow of ϕ into the control volume around a node P (Figure 5) by convection and diffusion in the x-direction is

$$[T_{X-} + (1 - f_{X-}) L_{X-}] \phi_{X-} + [T_{X+} - f_{X+} L_{X+}] \phi_{X+} \\ - [T_{X-} - f_{X-} L_{X-} + T_{X+} + (1 - f_{X+}) L_{X+}] \phi_P$$

where

$$\begin{aligned} T_X &= \Gamma_{eff, \phi} A_X / \delta_X \\ L_X &= \dot{m}_X'' / A_X \\ A_X &= 0.5 (r_+ + r_-) \Delta Y \end{aligned} \tag{49}$$

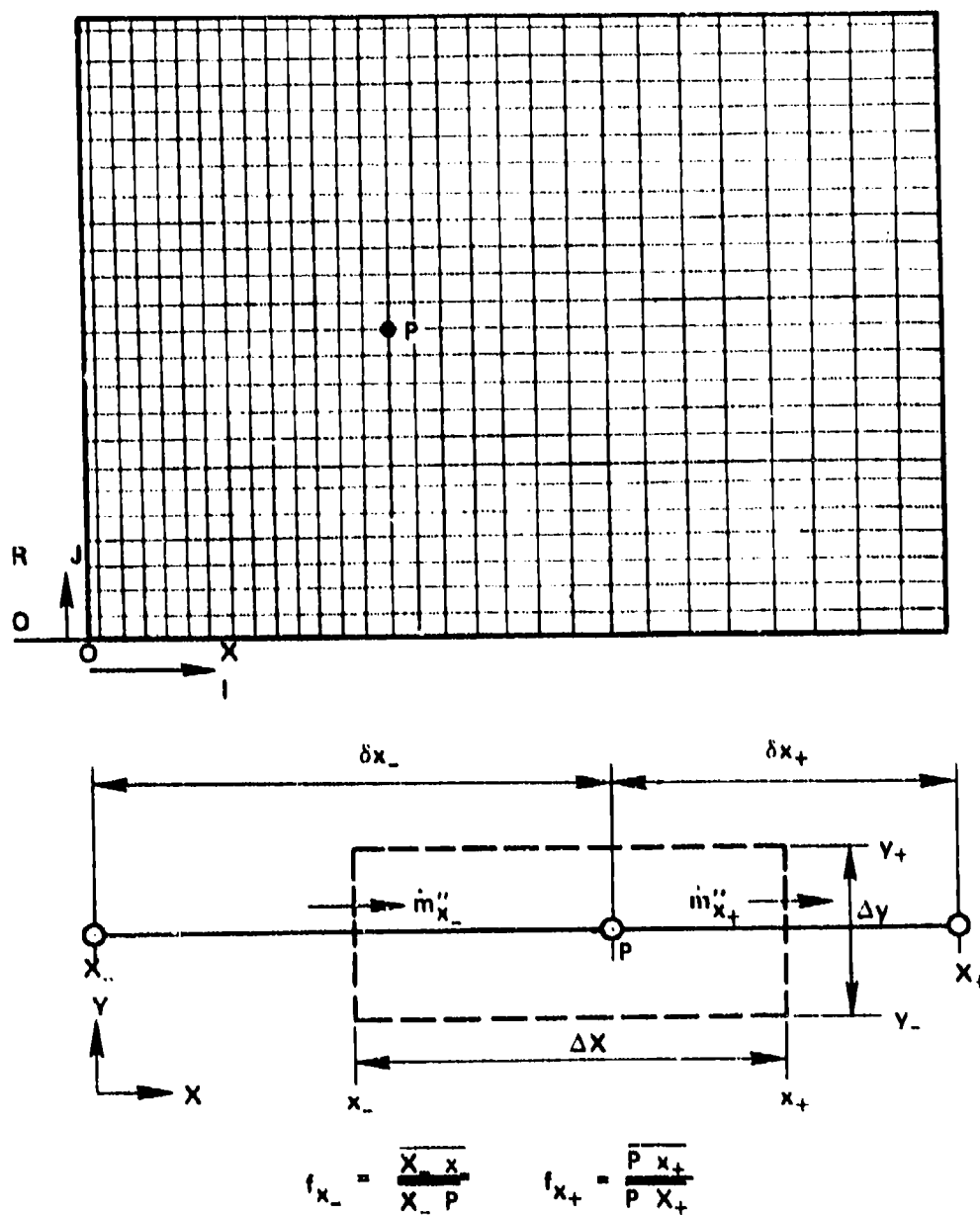


Figure 5. Typical Grid Spacing and Control Value Around a Point P.

Defining $\int \int \int S_v = S_u + S_p \phi_p$, the one-dimensional transport equation for the variable ϕ becomes

$$\begin{aligned} & [T_{X-} + (1 - f_{X-}) L_{X-} + T_{X+} - f_{X+} L_{X+} - S_p] \phi_p \\ & = [T_{X-} + (1 - f_{X-}) L_{X-}] \phi_{X-} + [T_{X+} - f_{X+} L_{X+}] \phi_{X+} + S_u \end{aligned}$$

The above equation was derived based on reasonable assumptions. However, the linear-profile assumption becomes unacceptable when $f_{X+} L_{X+}$ is large compared with T_{X+} because the weighting factor $(T_{X+} - f_{X+} L_{X+})$ then becomes negative, implying an unrealistic physical process through which raising the value of ϕ_{X+} could lower the value of ϕ_p . Therefore, it is assumed that if the convective flow rates (L) are large compared to the diffusion coefficients (T), the diffusion across the control-volume face is zero and the value of ϕ convection is equal to the value at the node on the upwind side of the face. With this assumption, the coefficient $T_{X+} - f_{X+} L_{X+}$ is replaced by $T_{X+}^* - f_{X+} L_{X+}$ where

$$T_{X+}^* = [T_{X+}, - (1 - f_{X+}) L_{X+}, f_{X+} L_{X+}] \quad (50)$$

Here $[a_1, a_2, a_3]$ stands for the largest of the three quantities a_1 , a_2 , and a_3 .

The final finite-difference equation is reduced to

$$A_p \phi_p = A_{X+} \phi_{X+} + A_{X-} \phi_{X-} + A_{Y+} \phi_{Y+} + A_{Y-} \phi_{Y-} + A_{Z+} \phi_{Z+} + A_{Z-} \phi_{Z-} + S_u \quad (51)$$

The solution of the above equation is obtained by line-by-line relaxation using an efficient tri-diagonal matrix algorithm. By this method, for an x-y plane, a traverse along one direction, say the x-direction, is made with old values for the y-direction nodes. Using this solution as the best estimate, the y-direction is then traversed. The same procedure is repeated for other x-y planes.

8. Boundary Conditions.

The specification of the boundary conditions is done in a number of ways depending upon the problem. For the left inlet boundaries, velocity, density, and turbulence profiles are either experimentally known or estimated. The program can handle any specified profiles. For boundaries of the second kind, where gradients and not the values of the variables are specified, the program uses one of the following two approaches. In the first approach, the boundary value is guessed and continually updated so as to satisfy the given gradient condition. The second approach breaks the link through the boundary to all adjoining external control volumes by first arranging for the finite-difference coefficient connecting the boundary node to an internal node to be zero, and then inserting the correct flux at the boundary as a false source of diffusion and/or convection for that internal node.

At the symmetry plane, the convection and diffusion fluxes are zero. Therefore, the convection coefficient C_{y-} and the exchange coefficient (Γ_{eff}) are made zero at the axis of symmetry. For the exit plane, information about some of the variables is not available. However, since it is the process occurring in the calculation domain that decides values of the variables which the outgoing fluid will carry, there is no need for information at such boundaries. These boundaries are simply treated by making the boundary Γ_{eff} equal to zero. The cyclic boundary conditions are used for the circumferential direction.

The near-wall region is given a special treatment in the program. Since the expression for Γ_{eff} is accurate for turbulent flows only, a means is provided for the inclusion of the correct shear stresses and other fluxes at the wall. Therefore, the nodes next to the wall are assigned the following values as per an empirical wall law:

$$\begin{aligned}
y^+ \leq 11.5 \quad \Gamma_{\phi, \text{wall}} &= \frac{\mu}{\sigma_{\phi}} \\
y^+ > 11.5 \quad \Gamma_{\phi, \text{wall}} &= \frac{\mu}{\sigma_{\phi}} \frac{y^+}{\frac{1}{\kappa} \ln(9y^+) + P_{\phi}} \quad (52) \\
y^+ &= \rho k^{\frac{1}{2}} C_D^{\frac{1}{4}} \frac{\delta}{\mu} \\
P_{\phi} &= 9.0 \left(\frac{\sigma}{\sigma_{\text{eff}}} - 1 \right) \left(\frac{\sigma}{\sigma_{\text{eff}}} \right)^{-\frac{1}{4}}
\end{aligned}$$

Where δ is the normal distance of the wall from the first interior adjacent node. The kinetic energy of turbulence has small diffusion near the wall; hence, Γ_{wall} for k is set equal to zero. Instead of computing Γ_{wall} for ϵ , it is calculated for the near-wall node by assuming a linear variation of the length scale giving the following expression:

$$c = C_D^{\frac{3}{4}} k^{\frac{3}{2}} / (\kappa \delta)$$

LINER COOLING MODEL

In order to design a durable combustor with conventional materials, the liner-wall temperature levels and gradients must be controlled. Consequently, it is imperative to have a calculation procedure that can be universally used for predicting liner wall temperatures. The wall temperature at a point P in a combustor liner (shown schematically in Figure 6) is determined by energy balance on a control volume around P, i.e.,

$$C_H + R_H = C_C + R_C$$

where C and R denote the heat transfer rate by convection and radiation, respectively. The subscripts H and C correspond to the hot side and cold side of the liner, respectively.

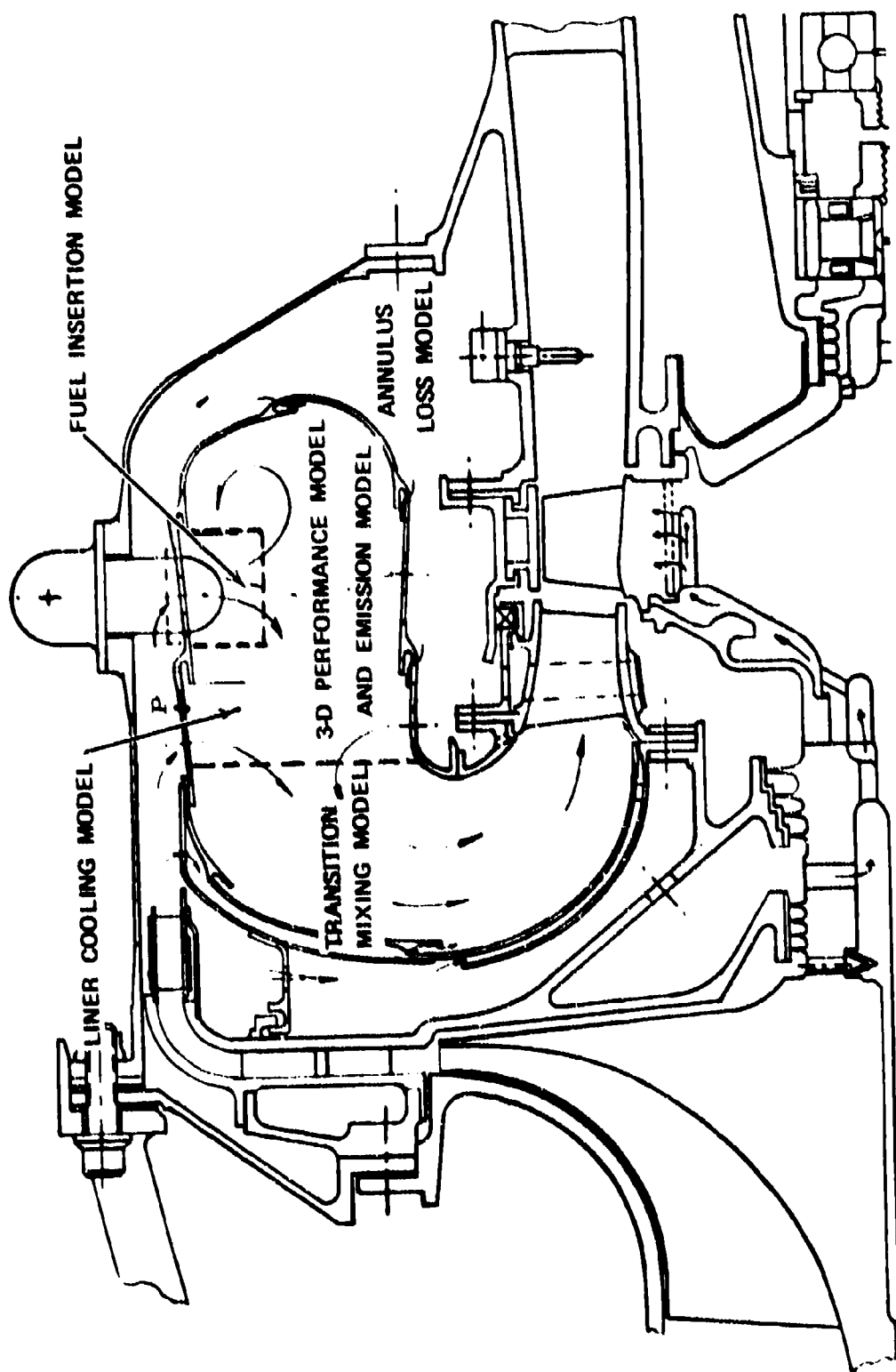


Figure 6. A Schematic of Reverse-Flow Annular Combustor and Application of Analytical Models.

A 2-D parabolic program is used to compute the hot-side convection and radiation heat transfer, the marching direction being x . The following expressions are used for calculating the cold-side heat-transfer rate.

$$C_C = 0.0268 (C_p G)_{an} R_{ex}^{-0.2} (T_w - T_{an}) \quad (54)$$

$$R_C = \sigma \left[\frac{1}{\frac{1}{\epsilon_w} + \frac{D_L}{D_P} \left(\frac{1}{\epsilon_P} - 1 \right)} \right] (T_w^4 - T_{an}^4) \quad (55)$$

where C_{pan} , G_{an} , and T_{an} are annulus air specific heat, mass velocity, and temperature, respectively. The length Reynolds number is based upon x downstream from the cooling-slot metering orifices. ϵ_w and ϵ_p are the liner-wall and the plenum-wall emissivities; D_L and D_P are the diameters of the liner and plenum, respectively. σ and T_w are the Stefan-Boltzman constant and the liner-wall temperature, respectively.

One major advantage of using algebraic expressions for the cold-side heat-transfer rates is that the appropriate expressions can be used for advanced cooling schemes that increase the heat-transfer rate from the cold side. Consequently, the cooling schemes, such as multiple impingement, extended-surface geometries, and chemically-etched surfaces, can be predicted by using the liner cooling model developed in this program.

Since a 2-D calculation procedure is used for calculating the hot-side heat-transfer rates, the model is strictly applicable to either uncooled liners or the liner walls protected by cooling films. The user will need to make approximations in predicting wall temperatures downstream from discrete radial jets such as the primary and secondary jets.

The 2-D parabolic program solves the governing equations for the following variables:

- Streamwise velocity and swirl velocity
- Turbulence kinetic energy and dissipation model of Jones and Launder²⁰.
- Specific enthalpy
- Unburned fuel, CO, and total fuel appropriate to the two-step kinetic scheme.
- Composite-radiation flux for the two-flux radiation model.
- Five-droplet trajectories

The governing equations, as reduced from the set of equations presented in paragraph B for parabolic flows, are transformed to the following generalized form of transport equations for the von Mises coordinate system²¹.

$$\frac{\partial \phi_j}{\partial x} + (a + b\omega) \frac{d\phi_j}{d\omega} = \frac{\partial}{\partial \omega} \left(c \frac{\partial \phi_j}{\partial \omega} \right) + d_j \quad (56)$$

where

$$a = r_I \dot{m}_I'' / (\Psi_E - \Psi_I) \quad (57)$$

$$b = (r_E \dot{m}_E'' - r_I \dot{m}_I'') / (\Psi_E - \Psi_I) \quad (58)$$

$$c = \frac{r^2 u_{eff}}{(\Psi_E - \Psi_I)^2 \sigma_{j,eff}} \quad (59)$$

$$\omega = (\Psi - \Psi_I) / (\Psi_E - \Psi_I) \quad (60)$$

²⁰Jones, W. P., and B. E. Launder, "The Calculation of Low-Reynolds Number Phenomena with a Two-Equation Model of Turbulence". ASME Paper 72-HT-20, 1971.

²¹Patankar, S. V., and D. B. Spalding, "Heat and Mass Transfer in Boundary Layers", Intertext Books, London; 1970.

Here ϕ_j is a generalized variable, and d_j contains the source/sinks and the other terms in the governing equation that do not fit in the convection and diffusion terms presented in Equation 56. ψ , r , and \dot{m}'' denote streamline, radius, and entrainment rate across the boundaries $\psi = \psi_I$ and $\psi = \psi_E$. The subscripts I and E refer to the inner and outer (external) boundaries of the domain of interest.

The numerical scheme used is a variant of the efficient numerics of Patankar and Spalding as described in Reference 21. A brief description of how the model is used for predicting liner-wall temperatures is given in the following paragraphs.

Consider a typical combustor liner and its predicted isothermal lines for an x-y plane; e.g., in line with primary jets, such as shown in Figure 7. The 3-D combustor-performance model predicted a reverse flow region near the dome, as shown by broken lines. This particular combustor has three cooling slots on the OD liner wall and four cooling slots on the ID wall. The wall-cooling model is used for predicting both inner- and outer-liner wall temperature with initial conditions for the three stations shown, defined by the combustor-performance model. The number of x-y planes to be solved depends upon a particular combustion system. If the predicted combustor internal flow is highly three-dimensional, then one may have to solve as many planes as the number of θ -nodes used in the 3-D computation. However, as the flow field approaches a two-dimensional approximation, one need not analyze more than a few x-y planes to obtain an accurate wall-temperature prediction.

Since the present wall-cooling model is a two-dimensional model, it cannot analyze wall regions near primary, intermediate, and dilution orifices. Consequently, it is advisable to restart the model for each panel with initial conditions as given by the combustor-performance model. Care should be taken in analyzing

SYM-VAL \square 2300. Δ 2100. + 1900. X 1700. \diamond 1600. ∇ 1500. X 1400. Z 1300. Y 1150. X 1000.
 SYM-VAL \times 900. (K)

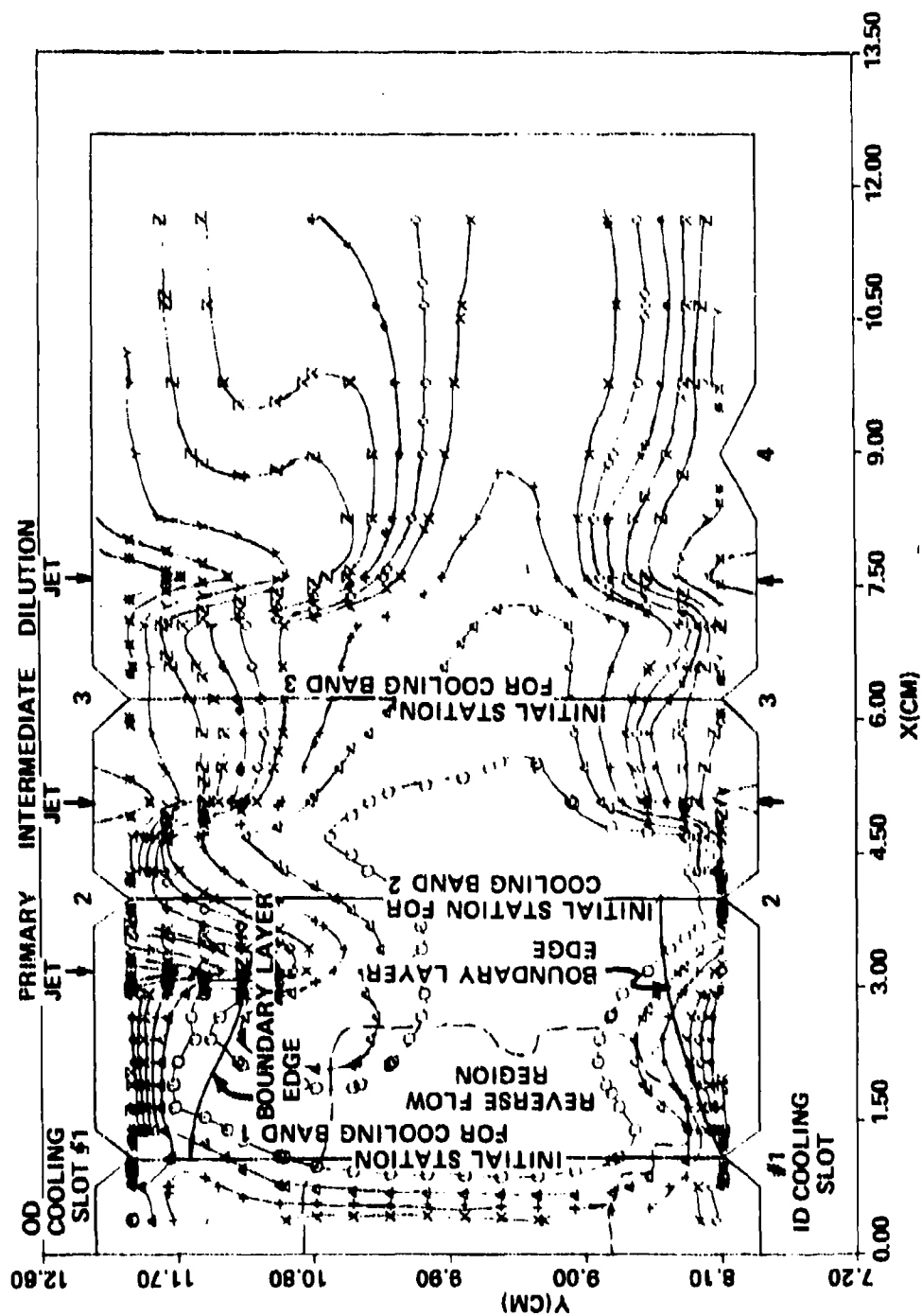


Figure 7. Typical Isothermal Plots of an Annular Combustor Along X-Y Plane In Line With Primary Jet.

the primary panel because of the presence of reverse-flow region. There are two possible approaches for analyzing this section. The first approach, the marching region lies between the liner walls and $u > 0$ with exchange rate specified for $u > 0$ line. In the second approach, one can define a boundary edge for which the edge conditions for dependent variables, including radiation flux, are defined based upon the combustor performance predictions. Then the wall-cooling model is run separately for the inner and outer primary panels.

In order to get more accurate wall temperature predictions, it is imperative to know the precise cooling slot exit conditions. In addition, one must accurately predict the effect of the splash-plate thickness on initial mixing between the cold-stream and main-combustion gases. The 3-D elliptic code can be used with minor modifications to predict the development of the jets exiting from the cooling-slot metering orifices. The effect of liner-pressure drop, orifice size and spacing, slot-lip length, and height on the slot-exit profiles can be analytically predicted. The 3-D elliptic code can also be used to predict the effect of the lip thickness on the initial mixing between hot and cold streams.

TRANSITION-LINER MIXING MODEL

The overall length of a gas turbine engine that employs a centrifugal compressor as the last stage of compression can be minimized by using a reverse-flow combustor. When the engine uses an axial turbine as its high-pressure turbine, a transition liner is needed between the combustor exit and the stator inlet. The transition-liner geometry, as shown in Figure 6, is quite complicated in that combustor exit flow, with mainly axial velocity component flowing from right to left, is bent through a 180-degree turn in order to flow into the turbine stator. The radii of curvature of both the inner- and outer-liner walls vary as a function of distance along the surface.

The flow in a practical transition liner is generally stream wise with little separation. Small regions of separated flows may exist along the ID transition liner surface. But, to insure structural durability of the liner, cooling air is generally injected in these separated areas so that the local liner-temperature levels and gradients are within allowable limits. As burner-exit temperatures increase along with reduction in burner length, cooling-film bands might be used for maintaining transition liner-wall temperature characteristics at an acceptable level.

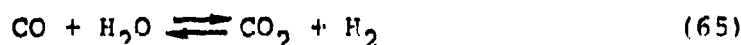
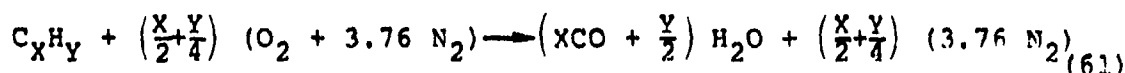
A significant fraction of the mixing of hot streaks with the cooler combustor gases takes place within the transition liner. With the advent of volume-limited turbopropulsion engines, there would be need to predict performance of the transition liner in regard to exhaust-temperature quality. In addition, the transition-liner-wall temperatures must be determined so as to estimate the liner life. A 2-D transition mixing model was therefore developed for this purpose. The program was adopted from the wall-cooling model described in the Liner Cooling Model paragraph. It solves governing equations for streamwise velocity and swirl velocity, specific enthalpy, turbulence kinetic energy, and dissipation. The effect of curvature on radial pressure gradient is taken into account. However, the pressure elliptic effects due to streamline curvature have been neglected.

GASEOUS EMISSIONS MODEL

Both the combustor-performance model and the wall-cooling model use a simple kinetic scheme in that the combustion process is described by two reaction steps, as given by Equations 18 and 19. Such a scheme is manageable for complex computer codes like the combustor-performance model. In addition, the model predicts both unburned fuel and CO which accounts for most of the combustion inefficiency. Since the engineer is generally interested in

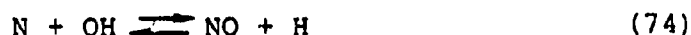
estimating combustion efficiency of a given combustor design, the combustor performance model is adequate for the purpose. However, when there is a need for estimating the NO_x emissions, one should preferably use a detailed kinetic scheme so as to predict intermediate species (such as O, N, and OH) that are considered important for the NO production. A number of calculation procedures exist for estimating the NO_x levels; e.g., those described in References 22 and 23. The approach taken here is explained as follows.

The wall-cooling model was modified to incorporate the following 16-step kinetic scheme involving 11 chemical species.



²²Sanborn, J. W., R. S. Reynolds, and H. C. Mongia, "A Quasi-Three-Dimensional Calculation Procedure for Predicting the Performance and Gaseous Emissions of Gas Turbine Combustors", AIAA Paper 76-642, 1976.

²³Mosier, S. A., and R. Roberts, "Low-Power Turbopropulsion Combustor Exhaust Emissions, Volume 3, Analysis", Technical Report AFAPL-TR-73-36, 1974.



A one-step global reaction is assumed for oxidation of fuel to CO as described by Equation 56. This reaction step is similar to the first reaction of the two-step kinetic scheme used in the combustor-performance model and the wall-cooling model. The reaction step is slightly different from that proposed by Edelman²⁴ where his postulation produces H₂ instead of H₂O, assumed here. A set of four reactions are used to describe oxidation of CO. Eight steps are used for reactions involving H₂, O₂ and their dissociation products. Finally, three reaction steps are used for the NO production. Although the program uses the 16-step kinetic scheme, a more extensive kinetic scheme such as that used by Edelman can be incorporated with relative ease.

The fuel-oxidation reaction is controlled by both chemical kinetics and turbulence similar to the scheme used in the two-step kinetic scheme described in paragraph B3. The remaining 15 reaction steps are controlled by chemical kinetics, although the modified eddy-breakup model could be used for these reactions also.

The numerical scheme used in the emission model is slightly different from that used in the wall-cooling model in regard to the way the source term \dot{d}_j of Equation 56 is calculated for the 11 chemical species. For each marching step

²⁴Edelman, R., J. Boccio, and G. Weilerstein, "The Role of Mixing and Kinetics in Combustion Generator NO_x", Paper presented at AIChE Symposium on Control of NO_x Emissions in Direct Combustion Power Sources, 1973.

size Δx of the parabolic program, d_j for the chemical species is computed by using the following 1-D equation

$$\frac{\partial \phi_j}{\partial x} = d_j^* \quad (77)$$

which is obtained by neglecting the cross-stream convection and diffusion terms of Equation 56. Equation 77 is solved for each of the species by taking a number of steps for the distance Δx . Typically, 50 steps are used for each Δx . With the source terms for the species now estimated, Equation 56 is then integrated for each of the species over the distance Δx . Such a modification results in approximately 70-percent reduction in computation time as compared to the numerical scheme used in the wall-cooling model.

FUEL-INSERTION MODEL

It may be recalled that a spray-combustion model is used in the combustor-performance code. This spray-combustion model includes heating, evaporation, and combustion of the spray, as well as the spray trajectories. The code also allows for the exchange of mass, momentum, and energy between the spray and the gas phase. Since a complete solution of the 3-D combustor-performance model takes a long computation time, on the order of three hours on the Cyber 174, an inexpensive calculation procedure was needed for initial selection of the fuel-nozzle characteristics. In addition, such a procedure would allow approximate evaluation of different nozzle designs in a flow field as computed by the combustor-performance model. A fuel-insertion model was therefore developed for this purpose.

Fuel-droplet evaporation rate and heat-transfer rate of the droplet are calculated according to the Priem-Heidmann model as described briefly in the following paragraphs. Vaporization of the droplet \dot{m}_f , lbm/sec is given by

$$\dot{m}_f = A_s K P_{vap}^\alpha \quad (78)$$

$$Nu_m = \frac{2 r_L K}{\rho_{vap} D} = 2 (1 + 0.3 S_c^{1/3} R_e^{1/2}) \quad (79)$$

$$\alpha = \frac{P_\infty}{P_{vap}} \ln \frac{P_\infty}{P_\infty - P_{vap}} \quad (80)$$

where A_s , K , Nu_m , P_{vap} , r_L , ρ_{vap} , D , S_c , R_e , and P_∞ are droplet-surface area, burning-rate constant, Nusselt number for mass transfer, fuel-vapor pressure, droplet radius, fuel-vapor density, diffusivity, Schmidt number, Reynolds number, and surrounding pressure, respectively.

Similarly, heat-transfer rate to the liquid surface q_v , Btu/sec is given by

$$q_v = A_s h (T_\infty - T_L) Z \quad (81)$$

$$Nu_H = \frac{2 h r_L}{k} = 2 (1 + 0.3 P_r^{1/3} R_e^{1/2}) \quad (82)$$

$$Z = \frac{Z}{e^Z - 1} \quad (83)$$

$$Z = \dot{m}_f C_{p,vap} / h A_s$$

where h , Nu_H , k , P_r , and $C_{p,vap}$ are heat-transfer coefficient, Nusselt number for heat transfer, thermal conductivity, Prandtl number, and isobaric-heat capacity of fuel vapor, respectively.

As in the spray combustion model of the combustor performance code, the spray is divided into five discrete droplet sizes. The physical and chemical properties of the jet fuels are varied as a function of the fraction evaporated, as described previously in Paragraph B5.

The following expressions for the spray SMD are currently incorporated in the code. These can be easily changed by the user if desired.

1. Simplex Nozzle.

$$SMD = \frac{225 * W_f^{0.205} \left(\frac{\mu}{1.5}\right)^{0.3}}{\Delta P_f^{0.354}} \quad (85)$$

2. Simplex Nozzle with Air Assist.

$$SMD = \frac{196 \sqrt{\frac{\sigma \cdot S}{\rho_a}} (II)^{0.095}}{0.438 \left(\frac{W_a}{W_f}\right)^{0.1} v_{aa} \left[0.5 + \frac{v_f^2}{v_{aa}^2} - \frac{v_f}{v_{aa}}\right]^{1/2}} \quad (86)$$

3. Duplex Nozzle.

$$SMD = \frac{330 W_f^{0.205} \left(\frac{\mu}{1.5}\right)^{0.3}}{\left[\frac{\Delta P_p W_{fp} + \Delta P_s W_{fs}}{(W_{fp} + W_{fs})}\right]^{0.354}} \quad (87)$$

4. Duplex Nozzle with Air Assist.

$$SMD = \frac{196 \sqrt{\frac{\sigma \cdot S}{\rho_a}} (II)^{0.095}}{0.438 \left(\frac{W_a}{W_f}\right)^{0.1} v_{aa} \left[0.5 + \frac{v_f^2}{v_{aa}^2} - \frac{v_f}{v_{aa}}\right]^{1/2}} \quad (88)$$

5. Air-Blast Nozzle.

$$SMD = 1.25 \left(\frac{\sigma \rho_f}{D_f} \right)^{1/2} \frac{\left(1 + \frac{W_f}{W_{a_n}} \right)}{V_a \cdot \rho_a} + 0.73 \left(\frac{v_f^2}{\rho_a \sigma} \right)^{0.425} \frac{\left[1 + \left(\frac{W_f}{W_{a_n}} \right) \right]^2}{D_f^{0.575}} \quad (89)$$

where:

- W_f = Fuel flow
- μ = Fuel viscosity
- ν = Fuel kinematic viscosity
- ΔP_f = Fuel-pressure drop
- σ = Fuel-surface tension
- S = Fuel-sheet thickness
- ρ_a = Air density
- W_a = Air-assist airflow
- V_{aa} = Air-assist air velocity
- V_f = Fuel velocity
- ΔP_p = Primary fuel-pressure drop
- ΔP_s = Secondary fuel-pressure drop
- W_{fp} = Primary fuel flow
- W_{fs} = Secondary fuel flow
- ρ_f = Fuel density
- D_f = Filming diameter
- W_{a_n} = Air-blast airflow rate

III. DESCRIPTION OF COMPUTER CODES

ANNULUS FLOW MODEL

The annulus-flow model calculates flow conditions around the combustor annulus by solving 1-D fluid-flow equations and provides information regarding annulus axial and tangential velocities, heat transfer from the liner wall, flow rates, jet velocities, jet angles and discharge coefficients of the various liner orifices, as well as the overall liner-pressure drop. Coding logic is provided so that the user may analyze can, and axial-flow and reverse-flow geometries. In addition, options allow the program to calculate the pressure drop for a given inlet flow rate or inlet flow for a given pressure drop. The program will also calculate either the flow through a specified orifice row or the orifice diameters required to pass a specified-flow rate. Finally, a plot, if desired, can be made giving the flow conditions around the combustor annulus and through the liner orifices.

The function of the MAIN program (a computer listing has been provided in Appendix B) is to call subroutine COMANN, which is the main controlling routine, and to perform file manipulations in the case of an axial-flow geometry. For this geometry, one item (usually not known) is the flow split between inner and outer panels. The user inputs essentially two separate cases, one for the OD panel and one for the ID. The program will then iterate on the flow split until the inner- and outer-panel pressure drops are equal. While calculations are being performed on one panel, information about the other is stored on scratch files.

Subroutine COMANN performs the iteration logic and calls the other subroutines as required. Iteration on pressure drop or

flow rate is performed until the calculated flow through the liner orifices agrees to within 0.05 percent of the inlet flow. However, if a solution is not obtained in 20 iterations, the program will stop, as errors in the input or high annulus Mach numbers could make convergence difficult. Of particular importance is the variable RELAX, defined at card C0.31. This is a relaxation parameter used in the convergence logic and has considerable influence on the convergence rate. The simple function provided has worked moderately well for various combustor geometries; however, for complex designs or high annulus mach numbers it is anticipated that the value of RELAX will need to be reduced to obtain a solution.

The names of the remaining subroutines are descriptive of their functions. All data cards are read in subroutine INPUT and then are printed out in subroutine PINPUT. INLET calculates the inlet conditions to the combustor annulus while LENGTH and FLOW perform calculations of annulus flow conditions and orifice flow conditions, respectively. FLOW, in turn, calls JET and DCOEF which calculate the orifice jet velocity and discharge coefficient. Some attention to cards DC.34 to DC.57 in DCOEF is warranted. As there was only qualitative agreement between the measured and calculated discharge coefficients, a constant multiplier was applied to the calculated values. Line printer output is produced in PROUT while the plots are generated in PICTUR and BOXES.

3-D-COMBUSTOR-PERFORMANCE MODEL.

The 3-D performance model is a three-dimensional recirculating-flow program that is capable of analyzing a variety of combustor configurations, including can, can-annular, and annular. The deck solves for the three velocity components, U, V, and W, three species concentrations, including UHC and CO,

turbulence qualities for the $K-\epsilon$ viscosity model, and three radiation fluxes. In addition, the use of primitive variables makes modifications to the boundary conditions easy, allowing the user to analyze complex inlet geometries. Also provided is a subroutine for calculating the trajectories and evaporation rates of a fuel-nozzle spray.

Program MAIN (a computer listing has been provided in Appendix C) is divided into two basic sections. Up to card MA.167, the routine is concerned with reading the input data and converting it to the program's internal units which are Système International (S.I.). The input sequence is covered in paragraph B of Section IV so only the units will be discussed. Cards MA.7 to MA.11 are used to define seven arrays which convert lengths associated with dimensions and lengths associated with velocity, energy, mass, temperature, pressure, and angles respectively. By proper specification in the data statements, the user may employ those input units that are most convenient. The output units are always S.I. From card MA.168 on, MAIN's function is to call the other various routines in their proper sequence.

Subroutine INITIAL performs some preliminary calculations (AL.10 to AL.155), prints the input data (AL.156 to AL.258), and defines the initial conditions and some of the boundary conditions on the various arrays (AL.259 on). In section AL.48 through AL.78, two arrays, JKIN and IKIN, are defined. They merely contain flags which indicate the locations of mass injection points. Cards AL.261 to AL.272 contain logic for the restart option. If Tape 8 from a previous run is saved and then made available for use during a subsequent run, the program will read the initial and boundary conditions from it.

Subroutine ALLMOD contains several entry points which perform miscellaneous calculations pertaining, usually, to the

boundary nodes where modifications to the standard equation are in order. The cyclic nature of the boundary conditions in the θ or K direction is evident in FMOD as well as limits to the fuel and carbon monoxide mass fractions. VELMOD allows the inlet swirl velocity to be increased gradually over a number of iterations and assures that overall continuity is maintained at the exit plane. DENMOD makes alterations to the density at the boundaries to maintain the correct mass-flow rate. GAMOD specifies the wall viscosity values as calculated by the wall functions. SOMAS is used to initialize an array DIVG which is used later in the program. The largest entry point SOMOD contains logic for modifying the equation coefficients and source terms when cooling slots, walls, and droplet evaporation are present. Each variable has its own section and accounts for transfer with the walls and mass addition from the evaporating fuel. SOMODZ deals only with the Z-direction radiation equation and is in a section alone as the data storage is slightly different for this variable.

Subroutine AUX performs the auxiliary calculations for temperature, density, viscosity, and source terms. Entry DENS uses AU.11 to AU.56 to calculate temperature. Cards AU.52 to AU.56 limit the values calculated in order to account for disassociation and early iteration fluctuations. With known temperature, density is then determined from AU.57 to AU.108. VISCO obtains effective viscosity from turbulent kinetic energy and dissipation and calculates y^+ for use by the wall function routine. SOURCE contains all calculations for source terms with the exception of the aforementioned modifications in SOMOD. Again each variable has its own section, with coding that is quite straightforward and requires no explanation.

Subroutine AUXRAD performs the same function as AUX except that it pertains only to the radiation equations.

SPRAY is used to determine the evaporation rate of the fuel-nozzle spray. A large section, from SP.106 to SP.269, deals with locating the droplet, determining free-stream conditions, and handling the situation where the droplet approaches a boundary. Next, various fuel- and free-stream properties are evaluated (to SP.292). The drag forces and time step are then determined and used to obtain new velocities and location. If the droplet is below the boiling temperature, no evaporation occurs (SP.340 to SP.347); but, when the boiling temperature is reached, evaporation rates are calculated, and the appropriate entries to the evaporation array (EVAP) are made. Information concerning momentum changes due to evaporation are also stored in their respective arrays and later (SP.382 to SP.425) on a scratch file for use when the three momentum equations are solved.

The coefficients for each variable are generated and the solution routine called in subroutine STRIDE. First, equations for U, V, and W are handled (ST.117 to ST.632), then the pressure perturbation (P') is obtained (SP.633 to ST.714) and used to correct the velocities (SP.716 to ST.753) so that mass errors are minimized. Then, the remaining variables are solved with the radiation equations having their own special section (ST.915 to ST.937).

STRAD is a subroutine used in the radiation model which performs the same function as STRIDE performed for the other variables.

SOLVE provides a solution to the equations generated in STRIDE. A full three-dimensional solution would be time consuming and would require enormous computer storage. Therefore, an approximate solution is obtained by "sweeping" through the field several times alternately solving along one direction, while holding the values in the other two fixed. The variable ICTDMA

(UV) at S0.36 is used to specify the number of such sweeps. As the program converges, and the variables assume their final values, the solution becomes more and more accurate.

LINER COOLING MODEL

This program is derived from the 2-D parabolic GENMIX program of S.V. Patankar and D.B. Spalding²¹. Modifications have included the addition of a two-equation viscosity model, two-step reaction scheme, two-flux radiation model, plus subroutines for calculating wall temperatures and liquid-fuel-evaporation rates.

The basic geometry for which this program has been geared is continuous inner and outer walls or continuous inner axis of symmetry and outer wall. Other situations may be analyzed provided the proper internal modifications are made to the code.

The MAIN program (a computer listing has been provided in Appendix D) handles several functions, including input, establishment of initial profiles, logic for boundary conditions, calling the additional routines in sequence, and output. The initial section of MAIN (through MA.369) deals with input and initial conditions. Input begins at MA.44 with the case title followed by control indices and grid parameters. More computer storage has been provided than is required for the six species involved in the two-step reaction-scheme, therefore, the extra arrays are zeroed. Various other variables are initialized prior to reading the name list at MA.187. The initial profiles are read from MA.212 to MA.222 and values are assigned to all the arrays from MA.292 to MA.269. The main marching loop (MA.272) begins with the calculation of pressure, temperature, and density (through MA.472). STRIDE(1) called at MA.497 calculates the

²¹Patankar, S. V. and D. B. Spalding.

physical dimension of y from the transformed cross-stream variable ω . The forward step size is next determined along with checks for specified X -locations. The boundary conditions are established between MA.528 and MA.743, and in this deck can be either an inner wall or axis of symmetry and an outer wall. Sections dealing with others are bypassed. The wall temperatures of the inner and outer walls, if required, are determined by the two call statements MA.747 and MA.748, while STRAD (MA.750) is a subroutine used to calculate the radiation flux. Duct geometry and pressure gradient occupy the next section MA.755 to MA.857 and provides two methods for pressure gradient calculation which are selected by IDPDX. When the value is 01, the program uses a guess-correction method, whereas for a value of 02, the program immediately corrects the velocity and pressure fields if the duct area and flow area differ. Entrainment rates are calculated from MA.907 to MA.934 but are not used in any calculations by this code. DROP, a subroutine called at MA.937, calculates the evaporation rates of the liquid-fuel spray. This is followed by STRIDE(2), which performs some preliminary calculations needed prior to solving the equations. The remainder of MAIN is devoted to printout with the exception of STRIDE(3), called at MA.1195 which actually solves the finite difference equations.

Subroutine AUX has two parts; the first (through AU.37) calculates the effective viscosity from the two equation turbulence model, while the second computes the source terms for each equation.

As mentioned above, DROP calculates evaporation rates. Note that the input data for the fuel nozzle is read at AUS.15. With the location of a particular droplet established (AUS.42 to AUS.68), properties of the fuel and free stream are determined (AUS.76 to AUS.94). Some preliminaries are performed before iterative loop AUS.111 to AUS.151 is entered. Calculations are performed until the guessed value of the distance the droplet

travels agrees with the calculated value. With this distance and the droplet velocity known, the time step and evaporation rate can be determined. The proper entries in the evaporation array EVAP are then made at AUS.173 and AUS.190.

STRAD performs all calculations relative to the two-flux radiation model. Modifications to the source terms due to the presence of a wall are made at GA.130 to GA.136. The central difference coefficients are then computed and solved using the standard tri-diagonal algorithm.

WTEMP uses an energy balance on the wall to determine the wall temperature. Cold-side convection, cold-side radiation, hot-side radiation, and hot-side convection are calculated in turn, and a Newton-Raphson iteration procedure is employed to solve the resulting heat-flux equation. The cold-side velocity and temperature are updated at each marching step, accounting for the heat transferred to the annulus.

STRIDE performs the bulk of the numerical calculations and has been documented in literature.

WF is used to evaluate the Couette-flow-equation solutions and to obtain wall shear stress and other transfer data.

PLOTS is a line printer plot routine.

TRANSITION LINER MIXING MODEL

This computer code is derived from the 2-D parabolic GENMIX program of S.V. Patankar and D.B. Spalding. The primary modifications include the ability to have a varying step size across the grid, since, for a given number of marching steps, the distance traveled along the outer-transition liner is considerably greater than along the inner. Other modifications include the addition of $K-\epsilon$ viscosity model.

A computer code that could handle all geometrical configurations would be greatly increased in size; therefore, this deck has been tailored to the geometry of a reverse-flow annular-combustor transition liner. Other configurations can be analyzed if the proper modifications are made to the computer code.

The MAIN program (a computer listing has been provided in Appendix E) handles several functions, including input, establishment of initial profiles, logic for boundary conditions, calling additional routines in sequence, and output. The initial section of MAIN, through card MA.255, contains input and data initialization coding. Note that the x and r values of the boundaries are read at cards MA.64 and MA.65, but that the value of z , the actual marching direction, is computed at MA.74 and MA.77. ISC VE and IPRNT perform the functions their names suggest, determining which variables are solved for and printed. Various constants are initialized in the next few cards. MA.157 is of some significance since it is here that the name list is read, and finally the various profiles are read in and defined. Starting at MA.256, the main marching loop begins with the calculation of pressure, temperature, and density (MA.293 to MA.315). STRIDE(1), called at MA.345, is a subroutine which extracts the physical cross-stream dimension from the transformed cross-stream variable, ω . The forward step size is calculated in the next section (MA.349 through MA.403), which was necessitated by having a smaller step size at the inner boundary than the outer, plus some checks for specified z -locations. Next, the boundary conditions are assigned (MA.406 to MA. 479), and since they are always walls in the transition liner, only those appropriate sections are entered. The actual duct area is determined in section MA.481 through MA.505, plus the area required by the flow. Should these two not agree, compensation in the pressure gradient for the next marching step will be made. The pressure gradient is calculated between MA.507 and MA.598. Two methods are provided and are selected by IDPDX. When the value is 01, the program uses a guess-correction method (MA.539 through MA.543),

whereas for a value of 02, the program immediately corrects the velocity and pressure fields (MA.521 through MA.536). The pressure gradient across the grid due to radius-of-curvature effects is calculated at MA.579 and incorporated into the axial-pressure gradient at MA.595. Statement MA.645 calls AUXO(0), which calculates the effective viscosity from the K- ϵ model. Since there is no entrainment for the geometry employed, cards MA.646 through MA.670 are bypassed. STRIDE(2), called at MA.673, performs some preliminaries necessary prior to the equation solution. The rest of MAIN is devoted to outputs of various types with the exception being MA.902 where STRIDE(3) is called, solving the equations for that marching step.

Subroutine AUX performs two functions; it calculates effective viscosity (up to AU.37) and the source terms for the equations (AU.38 on). Subroutine STRIDE performs the bulk of the numerical calculations and has been heavily documented in literature. Subroutine WF is used to evaluate the Couette-layer-equation solutions near a wall, to extract shear stress and other transfer data needed in the solution of the equations, and finally PLOTS is a line printer plot routine.

EMISSIONS MODEL

The emission model is a 2-D parabolic program derived from the GENMIX deck of S.V. Patankar and D. B. Spalding. The principal modifications include the addition of a 16-step reaction scheme and the ability to handle cooling slots and radial injection orifices.

The MAIN program (a computer listing has been provided in Appendix F) is concerned with input, establishment of initial conditions, logic for boundary conditions calling other subroutines in sequence, and output. The coding is similar to that already described for the liner-cooling model; therefore, only

those items unique to the emissions model will be discussed. Two additional input items are (1) extra specie-input profiles are required (MA.213 to MA.217), and (2) data describing the cooling slots and radial-injector orifices is read at MA.223 to MA.275. To accompany the additional input, there is also logic for the special boundaries, conditions associated with the cooling slots and radial injections MA.562 to MA.618 and MA.659 to MA.715, respectively. When the program reaches the edge of a slot lip, a free boundary is assumed until the flow rate of the slot has been entrained. A similar procedure is used for radial-injection orifices where the boundary is assumed to be a porous wall. All the other subroutines perform the same functions as described in the Liner-Cooling Model paragraph; however, an additional subroutine, AUXS, has been added which calculates the specie source terms and writes them on a scratch file. AUXS solves the same equations as STRIDE except that cross-stream convection and diffusion are omitted. The equations are solved many times using a step size considerably smaller than the main program. In this manner, an estimation of the change in the specie value for the larger main program marching step is obtained from which an average source term over the interval can be calculated. This is then used when the complete equations are solved in STRIDE(3). The first section of AUXS (up to AUS.68) performs data initialization followed by the calculation of forward and backward rate constants (AUS.70 to AUS.95). The main loop is entered next where first the source terms and then the derivatives are determined. Note that the rate expression for the global fuel reaction contains the effect of turbulence (AUS.125) and that the kinetic source term contains a number of variables each raised to a respective power (AUS.123 and AUS.124). These powers, EPU, ERO, etc., are read in through the name list in the MAIN program. A step size, such that the species values do not change excessively, is then selected using the variables TERM1 and TERM2, also part of the name list. Examination of AUS.223 shows that the maximum change allowed during the marching step is the larger

of TERM2 and TERM1 times the upstream specie value. The Equations are then solved and the process is repeated until a distance equal to the main program step size, DX, has been traversed. ISMAX, which is also part of the name list in the MAIN program, is a limit on the maximum number of these steps. The average source term over the interval is then calculated and stored on a scratch file for later use.

FUEL INSERTION MODEL

The function of the fuel-insertion model is to determine the evaporation rates and trajectories of a fuel spray in a two-dimensional flow field. Information concerning the fuel nozzle and flow field are read in, and from these the program calculates the fuel SMD and the trajectories. If desired, a plot of the droplet paths can be made and the evaporation rates saved for use in other programs.

INJECT1 (a computer listing has been provided in Appendix G) is the main program and controls input, output, and the other subroutines. Up to INJ.67 several data statements initialize some fuel and air properties needed in the evaporation calculations. Input data is read to INJ.119 followed by some preliminary calculations. Additional input is read at INJ.187 to INJ.195 if a nonuniform flow field is specified. Calculations of SMD for the particular fuel nozzle type selected begin at INJ.206 continuing to INJ.310. The next section entered (INJ.311 through INJ.435) loops over the five droplet sizes, calculating, in turn, their trajectories. The remainder of INJECT1 provides output and plotting. Subroutine FEVAPC is used to save the evaporation rates for later use, if desired, while AIRPRP interpolates the 2-D nonuniform flow field to obtain the free-stream conditions. Subroutine EVAP performs the majority of the calculations, including the force balances on the droplets so that their trajectories and the evaporation rates can be calculated.

Each of the remaining routines provides some property of the fuel or air required by the calculations.

IV. ILLUSTRATIONS

ANNULUS FLOW MODEL

Figure 8 shows the annulus-loss model example geometry. It is a simple reverse-flow combustor with inner- and outer-panel cooling slots, plunged primary orifices and two dome inlets. For the purposes of analysis, the annulus was divided into elements denoted by the dashed lines. These divisions correspond to places at which mass was extracted or where the annulus was of irregular shape. The elements can be length-type for which skin-friction losses and heat transfer, etc., are calculated or flow-type for which mass extraction is calculated. Thus, the length element (2) is the annulus section between the inlet (1) and (2), and flow element (3) is the OD cooling slot.

Inspection of the input sheets, Figures 9 through 11, shows that Card 1 contains the case title and specifies some control parameters. The annulus-inlet conditions are specified on Card 2 along with the total number of elements used and the inlet-element number. Card 3 is for internal liner flow only and is omitted, whereas Card 4 specifies various constants. It now remains to describe the plenum and liner shape and the various orifices. This is done on the second input sheet with explanations of the various items given in Figure 11. Since, for this case, the flow split between the various orifices was known and not the orifice size, the flow-element cards are of the fixed-flow ratio type (FF). Had the orifice size been known instead, the fixed diameter type (FD) should have been used. If the C_D of a particular orifice row is known, it may be specified as has been done for flow elements 8 and 10. Even though these are actually annular slots in the dome, the program will still calculate an orifice diameter, which is, of course, meaningless; however, the effective and geometric areas are also provided in the output from which the correct annular-slot height can easily

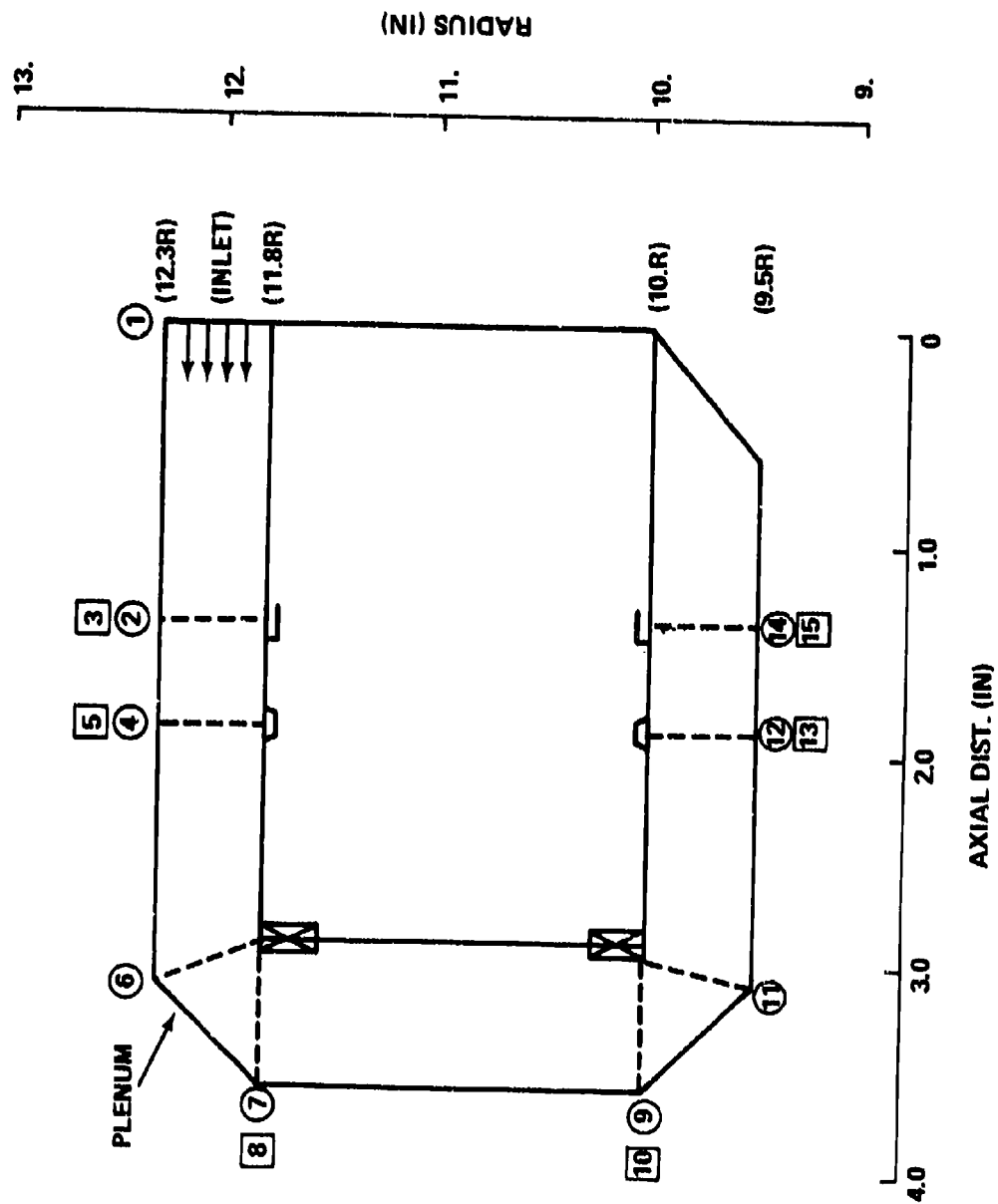


Figure 8. Annulus Loss Model Example Geometry.

	ITER	IPIC	IDBUG
	78	79	80
1 TITLE - MUST HAVE FOR EACH CASE			
1 ANNULUS LOSS MODEL EXAMPLE GEOMETRY	1	1	0
ANNULUS INLET FLOW CARD			
NEL NELI			
1 345678 11 W1 21 PT1 31 TT1 41 BETA1 51 DP/P 61 71			
2 1/015 001 1.6 14.7 1040. 20. .03 — —			
DOME INLET FLOW CARD (REQUIRED FOR INTERNAL LINER FLOW ONLY)			
NELI			
12 678 11 W 21 PT 31 TT 41 BETA 51 61 71			
3 ID — — — — — — — —			
CONSTANTS CARD			
1 11 FRIC 21 BLKF 31 TANS 41 CDB 51 SK 61 RG 71 IREAX			
4 C — — — 0. .83 .1 1.1 1.4 53.3 0.0			

- 1 Title - Run ident appears on printed output and plot
- ITER { = 1 some (or all) holes fixed, inlet flow fixed, iterate to get pressure drop.
= 2 some (or all) holes fixed, pressure drop fixed iterate to get inlet flow (input W1 is first guess).
- IPIC { = 0 no plot
= 1 plot drawn
- IDBUG { = 0 output printed after converged solution
= 1 output printed after each iteration | Use only to de-
= 2 output printed after each element | bugg
non-convergence
- 2 3 NEL = total number of element stations (card 2 only)
NELI = element ID no. (NELEM) at annulus or dome inlet 2 and 3
W₁ and W = air flow at inlet stations, lb/sec
PT₁ and PT = inlet total pressure, PSIA
TT₁ and TT = inlet total temperature, R
Beta₁, Beta = swirl angle at inlet
DP, P = total pressure drop, PSIA/PSIA (first guess if ITER = 1) card 2 only
- 4 FRIC { = 0, smooth wall friction factor
= -1, no wall friction
= roughness factor for rough walls
BLKF = annulus effective area factor (= .83 for fully developed turbine flow)
TANS = tangent of flow separation spread angle (.1 recommended)

Figure 9. Annulus Loss Model Input Sheet (Sheet 1 of 2)

CDB = drag coefficient of struts across annulus (1-1.2 RECM)
SK = ratio of air specific heats,
RG = air gas constant
IREAX { = 0. for reverse flow annular or can combustors
 = 1. for axial flow annular. First data set is for OD
 panel. Program expects a second set for ID panel

CASE TERMINATION

After last card of case:

- o In Column 1, Column 2 blank - case repeated with changes, next card is title card followed by cards with changes from previous run.
- oo In Columns 1 and 2, next card is EOF to quit or new title card followed by all cards for complete new case.

Figure 9. Annulus Loss Model Input Sheet (Sheet 2 of 2)

NELEM									
I	J	XP	RP	XL	RL	CL	T LINE	BLK I	DBK I
L	L	XP	RP	XL	RL	CL	T LINE	BLK I	DBK I
L	C	XP	RP	XL	RL	CL	T LINE	BLK I	DBK I
P	P	W/H	N HOLE	NHYP	CD		1 SEP		
P	D	W/H	N HOLE	NHYP	CD	D HOLES	1 SEP		
P	I	W/H					1 SEP		
P	I	WTN3/W	V SET	ANG 1	ABETA		1 SEP		

	1	2	345	11	21	31	41	51	61	71	76
1	L	001	0.	12.3	0.	11.8			1960.		
2	L	002	1.4	12.3	1.4	11.8			1960.		
3	FF	003	.15	120.	3.0				1.0		
4	L	004	1.9	12.3	1.9	11.8			1960.		
5	FF	005	.15	30.	2.0				1.0		
6	L	006	3.1	12.3	2.9	11.8			1960.		
7	L	007	3.6	11.8	2.9	11.8			1960.		
8	FF	008	.20	1.0	5.0	.50			1.0		
9	L	009	3.6	1.0	2.9	10.			1960.		
10	FF	010	.20	1.0	5.0	.50			1.0		
11	L	011	3.1	9.5	2.9	10.			1960.		
12	L	012	1.9	9.5	1.9	10.			1960.		
13	FF	013	.15	30.	2.0				1.0		
14	L	014	1.4	9.5	1.4	10.			1960		
15	FF	015	.15	120.	3.0				1.0		
16	00										
17											
18											
19											
20											
21											
22											
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33											
34											
35											
36											
37											
38											
39											
40											

Figure 10. Sample Work Sheet for Program 117.

NELEM					ALL NUMBERS MUST HAVE DECIMAL POINTS							
1	2	3	4	5	11	21	31	41	51	61	71	76
L	0	0	1		XP	RP	XL	RL	CL	T LINER	BLK I	DBK I
L	I	0	0	2	XP	RP	XL	RL	CL	T LINER	BLK I	DBK I
L	C	0	0	3	SP	RP	XL	RL	CL	T RISE	--	--
F	F	0	0	4	W/W1	N HOLES	NHTYP	CD	--	I SEP	--	--
F	D	0	0	5	W/W1	N HOLES	NHTYP	CD	D HOLES	I SEP	--	--
F	B	0	1	0	W/W1	--	--	--	--	I SEP	--	--
F	I	0	2	0	W/INJ/W	V JET	ANGJ	ABETA	--	I SEP	--	--

ELEMENT SPECIFICATION

Flow passage is divided into length (L) and flow (F) elements, element numbers, NELEM, can be in arbitrary order, i.e., 10, 1, 3, 4, 16, 30. The cards are stacked in order from inlet to last F because numbers are arbitrary, a new element can be inserted without renumbering other cards.

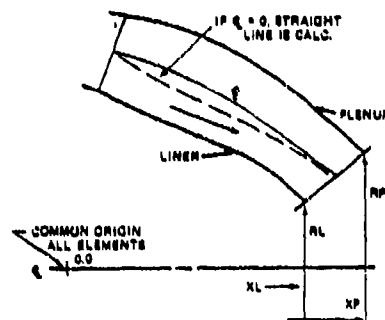
L. LENGTH ELEMENTS All Dimensions in Inches

First L card is annulus inlet (CL = 0) - For both external and internal cases. LENGTH ELEMENT
Internal and external flow cases must be run separately

For internal cases, 2nd card is dome inlet (LI) and LC cards are used with T RISE = ΔT due to combustion in this element (no L cards)

For external cases use only L Cards

XL, XP = X COORD to end of element L = Liner
RL, RP = Radius to end of element P = Plenum
(For internal flow XP, RP = OD, XL, RL = ID)
CL = Length of element (optional)
TLIN = Mean wall temp. over CL, °R
If = 0 then TLIN = TTI
BLKI = Frontal Area of Struts
Annulus Area
DBKI = Width of strut



F. ORIFICE FLOW ELEMENT

F Cards are inserted between L cards at points where flow is extracted. Flow conditions into F elem. are those from upstream L elem.

Types: FF = Fixed Flow Ratio, W/W1
FD = Fixed Orf. Diam. (W/W1 is First Guess)
FB = Bled flow (not included in liner flow)
FI = Internal flow elem. (input to these elements is obtained from an external flow solution)

W/W1 = Orifice Flow/Inlet Flow
NHOLES = No. of Orifices
NHTYP = Hole Type (For CD)
1. Flush Hole, Thin Wall
2. Plunged Hole
3. Cooling Skirt
4. Flush Hole, Thick Wall
5. CD Input
6. Rectangular Hole

CD = DISCH Coefficient (NHTYP = 5 Only)
DHOLES = Hole Diam. (For FD Only)
I SEP = 1, Separation is Reattached
VJET = Jet Injection Velocity, FPS
ANGJ = Jet Injection Angle, Deg.
ABETA = Swirl Angle in Annulus Outside FI Elem.

FLOW ELEMENTS

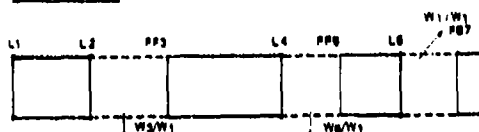


Figure 11. Program 117 Input Data Sheet
Input Format for Element Cards
Sheet 2.

be obtained. Other irregular shaped orifices, such as slotted-dilution holes, for example, can be handled in a similar manner. Card deck termination is specified by the double periods.

The output of the program is shown in Figures 12 through 14. Figure 12 is merely a printout of the input data. Figure 13 gives information of conditions in the annulus at the various stations the user has specified. Figure 14 has information regarding the orifices. Note that the program has calculated orifice-hole diameters and that the flow split is the same as was specified in the input. Overall output parameters such as pressure drop, corrected flow, etc., are also given. The numbers under the heading INPUT FOR SUB BOXES- are associated with the plot subroutine.

COMBUSTOR PERFORMANCE MODEL

The combustor geometry for the 3-D combustor-performance model example is shown in Figure 15. The reverse-flow annular liner has been divided into a grid network consisting of 30 nodes in the axial or X direction, 19 nodes in the radial or y direction, and 13 nodes in the tangential or θ directions. The decision of how large a θ segment to analyze is depending upon where radial planes of symmetry can be found, since the program assumes that there are cyclic boundary conditions in the θ direction. Therefore, any mass leaving the system along the K-13 plane is assumed to reenter the system through the K = 1 plane and vice versa. For this example, uniform grid spacing has been used, although this is obviously not required.

The completed input sheets for the case are shown in Figure 16. Additional input information can be found on the input sheet forms located in Appendix A. Cards 1 and 2 are titles used for printout and case identification. The grid size (30 by 19 by 13) has been entered on Card 3 along with indicators for axisymmetric geometry, K- ϵ viscosity model, kinetic and turbulence controlled

ANNULUS LOSS MODEL: EXAMPLE GEOMETRY

INPUT DATA -
 CALCULATION CONTROLS - SOME (OR ALL) HOLES FIXED SIZE, ITERATE TO FIND PRESSURE DROP (ITER = 1)
 PICTURE WILL BE PLOTTED (PIC = 1)
 OUTPUT PRINTING OCCURS AFTER FINAL SOLUTION ONLY (IDBUS = 0)
 OVERALL PRESSURE DROP - .0450
 ANNULUS EFFECTIVE AREA FACTOR - .8300
 AIR RATIO OF SPECIFIC HEATS - 1.400
 AIR GAS CONSTANT - 53.300
 ANNULUS WALL ROUGHNESS FACTOR - 0.0000
 TANGENT OF SEPARATION SPREAD ANGLE - .1000
 DRAG COEFFICIENT FOR INSERTED BLOCKAGE - 1.1000
 NUMBER OF POSITION ELEMENTS - 15

DIMEN. AT DOWNSTREAM END OF ELEMENT

ELEM NO.	ELEM TYPE	OUTER LENGTH	OUTER RADIUS	NO	XI	II	CL	WALL ELEMENT LENGTH	INSERT AREA FACTOR	INSERT DIAMETER IN.	MOLE IM.	NUMBER OF HOLES	MOLE TYPE	DISCH ORIFICE COEFF FLOW / FLOW IN
1	L	0.000	12.300	0.000	11.800	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500
2	L	1.400	12.300	1.400	11.800	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500
3	FF	1.900	12.300	1.900	11.800	-0.000	1960.0	1.000	1.000	1.000	1.0000	30	2	0.0000 .1500
4	L	3.100	12.300	2.900	11.800	-0.000	1960.0	1.000	1.000	1.000	1.0000	1	5	.5000 .2000
5	FF	3.600	12.300	2.900	11.800	-0.000	1960.0	1.000	1.000	1.000	1.0000	1	5	.5000 .2000
6	L	3.600	10.000	2.900	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	30	2	0.0000 .1500
7	L	3.600	10.000	2.900	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500
8	FF	3.100	9.500	2.900	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500
9	L	1.400	9.500	1.400	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500
10	FF	1.900	9.500	1.900	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500
11	L	3.100	9.500	2.900	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	30	2	0.0000 .1500
12	L	3.100	9.500	2.900	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	30	2	0.0000 .1500
13	FF	3.600	9.500	2.900	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500
14	L	1.400	9.500	1.400	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500
15	FF	1.900	9.500	1.900	10.000	-0.000	1960.0	1.000	1.000	1.000	1.0000	120	3	0.0000 .1500

START ITERATION NO. 1
 SOLUTION CONVERGED, TOTAL JET FLOW= 1.0000 FLOW ERROR= -.000000 FINAL PRESSURE DROP= .045000

Figure 12. Annulus Loss Model Output.

ANNULUS LOSS MODEL EXAMPLE GEOMETRY

OUTPUT RESULTS - PAGE 1

ELEM NO	ELEM TYPE	SWIRL ANGLE	FLOW RATE LBS/S	MACH NO	FLGM VEL FPS	AXIAL VEL FPS	TANG VEL FPS	TOTAL TEMP, R	STATIC TEMP, R	TOTAL PRESS, PSIA	STATIC PRESS, PSIA	DENSITY LB/FT ³	SYNTH HEAD, PSIA	BYN MO /PTOT ---
1	L	29.00	1.400	.1306	206.09	193.66	70.49	1040.0	1036.5	14.70	14.53	.0379	.174	.0118
2	L	19.70	1.600	.1311	207.75	195.57	70.08	1049.6	1048.0	14.69	14.52	.0375	.175	.0119
3	FF	22.89	1.360	.1136	180.08	165.88	70.08	1049.6	1048.0	14.69	14.52	.0376	.131	.0089
4	L	22.76	1.360	.1137	180.56	166.48	69.90	1053.2	1050.5	14.69	14.56	.0374	.132	.0090
5	FF	27.04	1.120	.0967	153.67	136.86	69.90	1053.2	1051.3	14.69	14.59	.0374	.096	.0045
6	L	28.45	1.120	.0913	145.65	128.05	69.41	1061.7	1059.9	14.66	14.60	.0372	.085	.0050
7	L	30.10	1.120	.0883	140.97	121.94	70.73	1064.2	1062.5	14.69	14.61	.0371	.080	.0054
8	FF	44.52	.800	.0631	100.85	71.87	70.73	1064.2	1063.3	14.69	14.65	.0372	.061	.0020
9	L	43.70	.800	.0740	118.85	85.90	82.14	1076.8	1075.6	14.68	14.63	.0367	.056	.0030
10	FF	57.89	.480	.0603	96.94	51.49	82.14	1076.8	1076.0	14.68	14.65	.0368	.037	.0025
11	L	50.55	.480	.0674	138.49	68.89	83.81	1086.2	1079.2	14.68	14.64	.0366	.047	.0032
12	L	47.66	.480	.0689	111.47	75.04	82.44	1092.1	1091.0	14.68	14.63	.0362	.049	.0033
13	FF	65.51	.240	.0559	90.56	37.49	82.44	1092.1	1091.4	14.68	14.65	.0363	.032	.0022
14	L	64.98	.240	.0551	89.53	37.81	81.16	1101.4	1100.7	14.68	14.65	.0360	.031	.0021
15	FF	89.69	.002	.0499	81.16	.38	81.16	1101.4	1100.8	14.68	14.65	.0360	.026	.0017

Figure 13. Annulus Loss Model Output.

ANNULUS LOSS MODEL EXAMPLE GEOMETRY

OUTPUT RESULTS - PAGE 2

***** ANNULUS GEOMETRIC PARAMETERS *****										***** DRIFCE PARAMETERS *****									
ELEM	NO.	TYPE	MEAN	CHANNEL	ANN	AN	EFF	MAKE	SEPAR	ATCH	MOLE	DISCH	JET	DRIF	ORIF	JET	ORIF	FLOW	ORIF
IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.	IN.
1	L	12.050	-500	37.86	29.53	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
2	L	12.050	-500	37.86	29.58	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
3	FF	12.050	-500	37.86	28.94	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
4	L	12.050	-500	37.86	28.97	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
5	FF	12.050	-500	37.86	27.98	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
6	L	12.050	-539	40.77	29.75	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
7	L	11.000	-700	51.90	30.81	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
8	FF	11.000	-700	51.90	30.70	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
9	L	10.000	-700	43.98	28.38	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
10	FF	10.000	-700	43.98	19.39	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
11	L	9.750	-534	32.99	17.39	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
12	L	9.750	-500	30.63	17.11	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
13	FF	9.750	-500	30.63	10.52	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
14	L	9.750	-500	30.63	10.74	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
15	FF	9.750	-500	30.62	12.12	1.000	1.000	1.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
OVERALL FLOW COEFFICIENT = .6282																			
INLET CORRECTED FLOW, LBS/S = 2.266																			
DISCHARGE PRESSURE, PSIA = 14.04																			
PRESSURE DROP / PT INLET = .0450																			
TOTAL GEOMETRIC AREA, IN2 = 23.981																			

INPUT FOR SUB BOXES -																			
2.750	-1.050	-7.050	-500	-7.050	-1.500	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
-3.075	2.350	1	-1.050	2.350	2	-2.050	4.575	3	-1.025	2.350	4	1.025	4.575	5	1.025	4.575	6	1.025	4.575
-1.025	4.575	5	2.050	2.350	6	1.025	4.575	7	1.025	4.575	8	1.025	4.575	9	1.025	4.575	10	1.025	4.575
2.050	2.350	9	-512	-6.225	13	-513	-6.225	14	-513	-6.225	15	-513	-6.225	16	-513	-6.225	17	-513	-6.225
-512	-6.225	13	-513	-6.225	14	-513	-6.225	15	-513	-6.225	16	-513	-6.225	17	-513	-6.225	18	-513	-6.225

Figure 14. Annulus Loss Model Output.

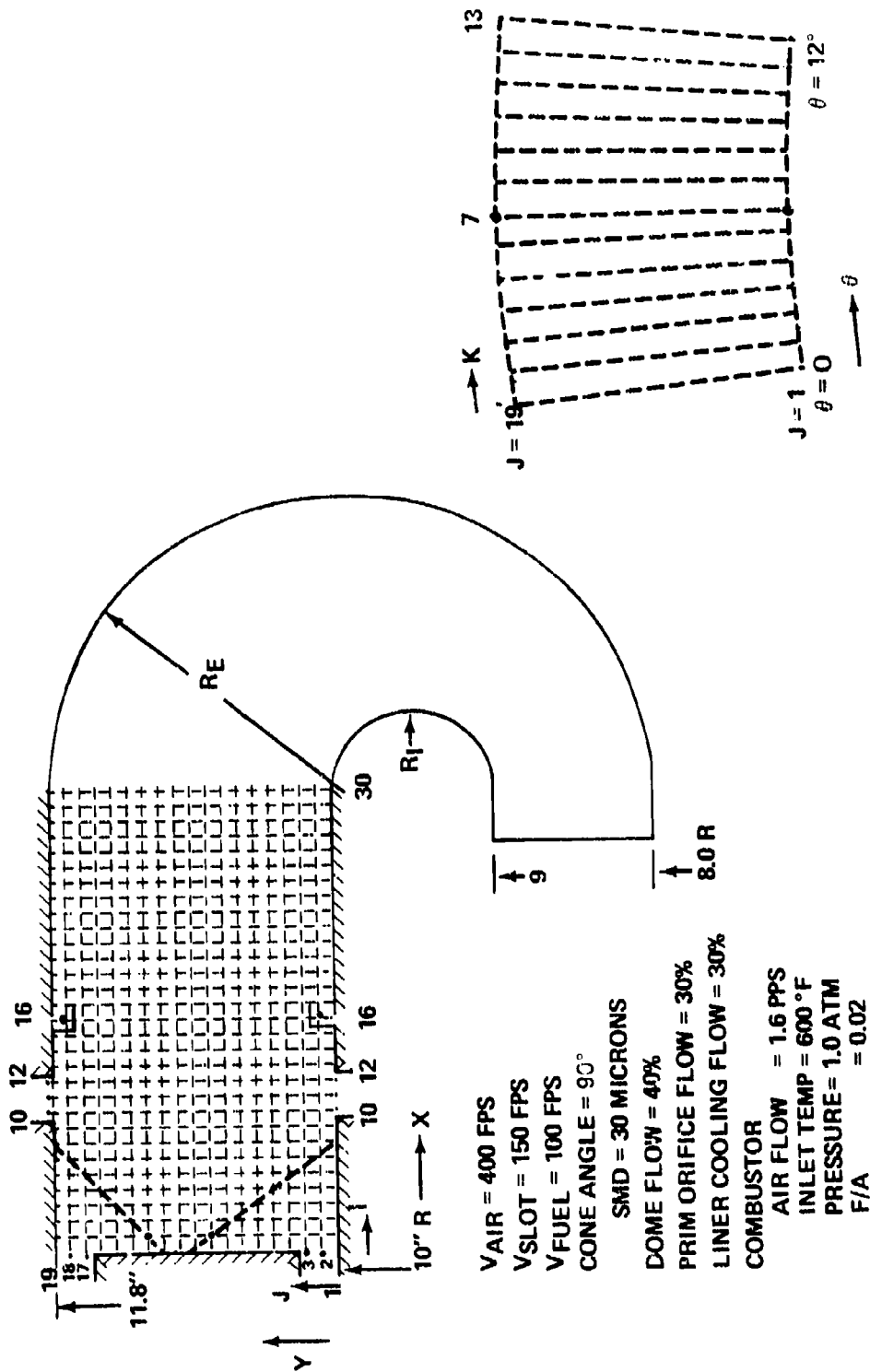


Figure 15. Combustor Geometry for 3-D Combustor-Performance Model.

1	22 VARIABLE TITLE CARDS (4A10) SAME ORDER AS IMPRINT							
2	CASE TITLE CARD (8A10)							
	3D PERFORMANCE MODEL EXAMPLE CASE							
3	LP1	MP1	LP1	IPLAX	MODEL	MODER	IPAR	ITRAD
	30	19	13	02	02	02	02	02
4	IU	MODEN	INTAPE	IDW	IRES			
	02	02	00	01	00			
5	<u>ISOLVE</u> (8(I2, 8X))							
	U	V	W	P'	KE	ϵ	θ	MFU
	01	01	01	01	01	01	01	01
	MCO	\tilde{R}	FX	FY	FZ			
	01	01	01	01	01			
6	<u>ICTDMA</u> (8(I2, 8X))							
	U	V	W	P'	KE	ϵ	θ	MFU
	01	01	01	06	01	01	01	01
	MCO	\tilde{R}						
	01	01						
7	<u>IMPRINT</u> (8(I2, 8X))							
	U	V	W	PRESS	KE	l_m	θ	MFU
	06	06	06	06	06	06	06	06

Figure 16. 3-D Combustor Performance Model (1 or 6)

TEMP	\tilde{h}	Favg	Fx	Fy	Fz	MCO	MH2O
06			06	06	06	06	

M02	MC02	MN2	μ_{EFF}	DENSITY	EVAP		
			06	06	06		

RELAXATION PARAMETERS (8E10.4)

U	V	W	P'	KE	ϵ	\bar{D}	MFU
8 .2	.2	.2	1.0	.5	.5	.8	.8

MCO	\tilde{h}	Fx	Fy	Fz	PRESS	DENSITY	VISCOS
.8	.8	1.	1.	1.	.5	.2	.1

LAMINAR PRANDTL NUMBERS (8E10.4)

U	V	W	P'	KE	ϵ	\bar{D}	MFU
9 1.	1.	1.	1.	1.	.7	.7	.7

MCO	\tilde{h}						
.7	.7						

TURBULENT PRANDTL NUMBERS (8E10.4)

U	V	W	P'	KE	ϵ	\bar{D}	MFU
10 1.	1.	1.	1.		.9	.9	.9

MCO	\tilde{h}						
.9	.9						

X-COORDINATES (1-LP1) (8E10.4)

11 0.	.1	.2	.3	.4	.5	.6	.7

.8	.9	1.0	1.1	1.2	1.3	1.4	1.5
----	----	-----	-----	-----	-----	-----	-----

Figure 16. 3-D Combustor Performance Model (2 of 6)

	1.6	1.7	1.8	1.9	2.0	2.1	2.2	2.3
	2.4	2.5	2.6	2.7	2.8	2.9		

RI Y-COORDINATES (2-MP1) (8E10.4)

12

10.	.1	.2	.3	.4	.5	.6	.7
-----	----	----	----	----	----	----	----

.8	.9	1.0	1.1	1.2	1.3	1.4	1.5
----	----	-----	-----	-----	-----	-----	-----

1.6	1.7	1.8					
-----	-----	-----	--	--	--	--	--

Z-COORDINATES (1-NP1) (8E10.4)

13

0.	1.	2.	3.	4.	5.	6.	7.
----	----	----	----	----	----	----	----

8.	9.	10.	11.	12.			
----	----	-----	-----	-----	--	--	--

--	--	--	--	--	--	--	--

IWEI JWIO (2(I2,8X))

14

02	19						
----	----	--	--	--	--	--	--

IWLI VALUES (8(I2,8X)) (SKIP 15 AND 16 IF IWEI = 2)

15

--	--	--	--	--	--	--	--

--	--	--	--	--	--	--	--

Figure 16. 3-D Combustor Performance Model (3 of 6)

16	JWLO VALUES (8(I2, 8X))							
17	PRESS	DEN	ABSOR	SCATR	AKFAC	ALFAC	(8E10.4)	
	1.0	-	.1	.01	.003	.02		
18	CX	HY	HFU	FUMCO			(8E10.4)	
	1.0	19.28	-49317.	.00001				
19	PREXP1	ARCON1	CR1	PREXP2	ARCON2	CR2	(8E10.4)	
	3.3E+14	27000.	3.0	6.0E+8	12500.	4.0		
20	C1	C2	CD	AMU	ERROR	TCYLW	TINLW TLIP	
	1.43	1.92	.09	185E-5	.01	1960.	1960. 1560.	
21	(2(I3, 7X), 6(I2, 8X))							
	LASTEP	IJUMP	JSW1	JSW2	NUINJ	NVINJ		
	150	999	02	03	02	06		
22	USW	VSW	SWNO	AFSW	FSW	TSW	(8E10.4)	
	400.	0.	0.	.02133	0.0	1060		
23	NFNZ	ISPRAY	TFUEL					
	01	9	540					
24	XO	YO	ZO	ALFA	BETA	DELTA	THETA 1 THETA 2	
	.05	.9	6.0	90	-90.	0.0	0. 360.	
	RSP	WF	SMD	VFUEL	(SKIP 24 IF NFNZ = 00)			
	20.	.001067	30.	100				

Figure 16. 3-D Combustor Performance Model (4 of 6)

(SKIP CARDS 25 - 30 IF NUINJ = 00)

I - LOCATION OF COOLING SLOTS (8(I2, 8X))

25	17	17						
----	----	----	--	--	--	--	--	--

J - LOCATION OF COOLING SLOTS (8 (I2, 8X))

26	02	18						
----	----	----	--	--	--	--	--	--

AXIAL SLOT VELOCITY (8E10.4)

27	150.	150.						
----	------	------	--	--	--	--	--	--

TANG. SLOT VELOCITY (8E10.4)

28	0.	0.						
----	----	----	--	--	--	--	--	--

SLOT FLOW RATE (8E10.4)

29	.008	.005						
----	------	------	--	--	--	--	--	--

SLOT TEMPERATURE (8E10.4)

30	1060.	1060.					
----	-------	-------	--	--	--	--	--

(SKIP CARDS 31 → 38 IF NVINJ = 00)

I - LOCATION OF RADIAL INJECTION (8 (12.8X))

31	10	11	12	10	11	12		
----	----	----	----	----	----	----	--	--

J - LOCATION OF RADIAL INJECTION (8(I2, 8X))

32	01	01	01	19	19	19		
----	----	----	----	----	----	----	--	--

K - LOCATION OF RADIAL INJECTION (8(I2, 8X))

33	07	07	07	07	07	07		
----	----	----	----	----	----	----	--	--

INJECTION VELOCITY (8E10.4)

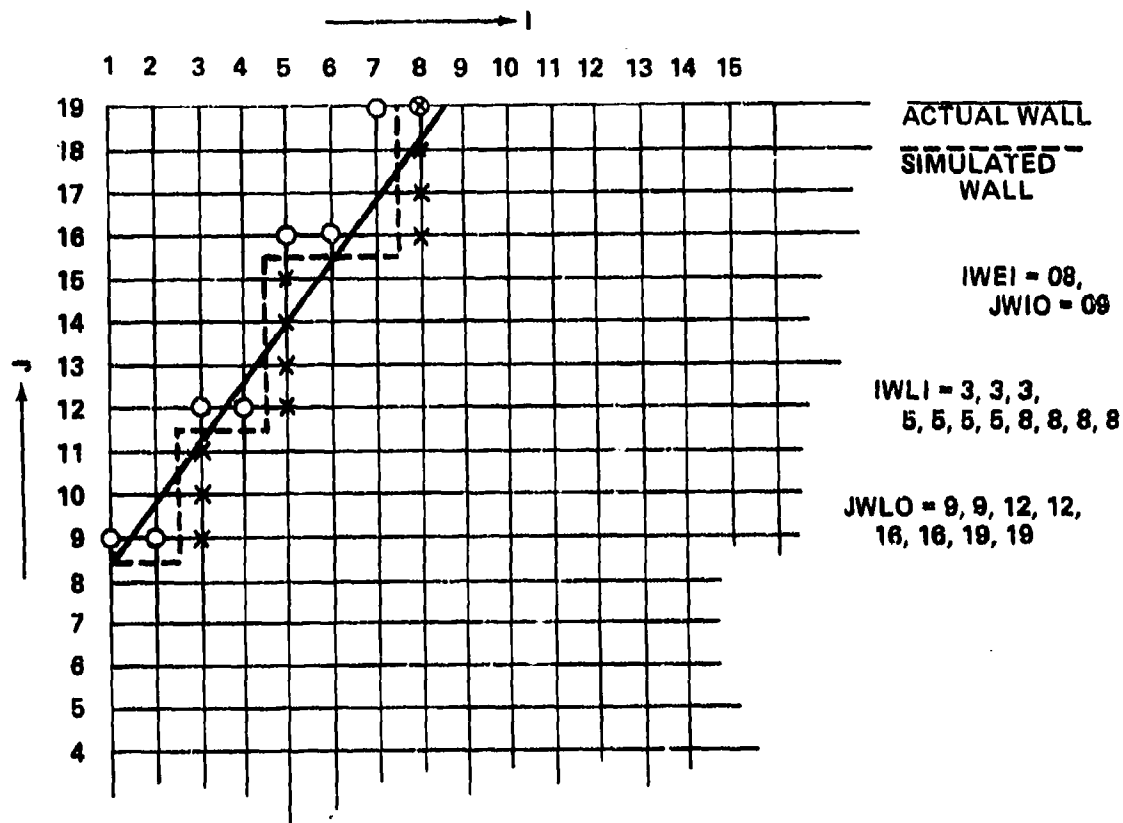
34	400.	400.	400.	-400.	-400.	-400.		
----	------	------	------	-------	-------	-------	--	--

Figure 16. 3-D Combustor Performance Model (5 of 6)

INJECTION TURBULENT KINETIC ENERGY (8E10.4)								
35	480.	480.	480.	480.	480.	480.		
INJECTION TURBULENT LENGTH SCALE (8E10.4)								
36	.0005	.0005	.0005	.0005	.0005	.0005		
INJECTION FLOW RATE (8E10.4)								
37	.002667	.002667	.002667	.002667	.002667	.002667		
INJECTION TEMPERATURE (8E10.4)								
38	1060.	1060.	1060.	1060.	1060.	1060.		

Figure 16. 3-D Combustor Performance Model (6 of 6)

combustion, relative pressure, and radiation to be included, respectively. The use of relative pressure, rather than absolute pressure, merely means that the pressure field is referenced to one particular grid node by subtracting that pressure value from the entire field. On Card 4, the user-selected-input units have been specified. The particular units employed are combinations of convenient ones and are specified by data statements in the main program, at lines MA.9 to MA.11. The user should redefine the arrays for his own input units or use S.I. by specifying IU = 01. Specifying the perfect gas-density calculation, not printing the initial values, the inner boundary as a wall and that this is not a restart, complete the information on Card 4. In order to restart a case, Tape 8 must be saved from the previous run and be made available to the program. Card 5 indicates that all the variables are to be solved. P' is the pressure perturbation used in the solution algorithm, h is stagnation enthalpy, and F_x , F_y , and F_z are the three radiation fluxes. Card 6 shows that all the variables will receive one sweep of the solution routine per iteration except P' , which will have six. The solution of the equations in early iterations is not exact, but this does not present a problem since the coefficients are changing from iteration to iteration anyway. However, it is beneficial to the convergence rate to obtain a more accurate solution to the P' equation. The variables to be printed are specified on Card 7. The 06 merely indicates that every 6th K-plane will be printed. The relaxation parameters specified on Card 8 have been used successfully on a wide range of problems and probably need not be altered. The Prandtl numbers and coordinates, Cards 9 through 13, are fairly self explanatory except that the first field, Card 12, is the radius of the inner boundary and that values of $y(2)$ to $y(MPL)$ are measured from that line. Cards 14 through 16 are used to specify an inclined wall at the inlet. Since there is none for this case, the values of IWEI and JWIO are set equal to 2 and MPL (i.e., 19) respectively, and Cards 15 and 16 are omitted. Were there an inclined wall, Figure 17 gives the necessary information



THE ACTUAL WALL IS SIMULATED BY STAIRSTEPS ALONG THE MIDPOINTS BETWEEN NODES. JWIO IS THE J-NODE WHERE THE INCLINED WALL STARTS, I.E., 09, AND IWEI IS THE I-NODE WHERE THE INCLINED WALL ENDS, I.E., 08. IWL1 IS THE 1ST I-NODE INSIDE THE SIMULATED WALL AT A PARTICULAR J-LOCATION. ELEVEN VALUES ARE REQUIRED SINCE THIS IS THE NUMBER OF J-NODES INCLUDED IN THE INCLINED WALL, $J = 9 - 19$, AND ARE MARKED BY *.

JWLO IS THE 1ST J-NODE OUTSIDE THE SIMULATED WALL AT A PARTICULAR I-LOCATION. EIGHT VALUES ARE REQUIRED SINCE THIS IS THE NUMBER OF I-NODES INCLUDED IN THE INCLINED WALL, $I = 1 - 8$, AND ARE MARKED BY \odot .

Figure 17. Information Necessary to Describe an Inclined Wall.

required to describe it. Cards 17 through 20 need no further explanation other than that given in input sheet forms. A total of 150 iteration steps, along with no intermediate printout, have been specified in the first two fields of Card 21. The basic program contains provisions for only one dome inlet, specified by JSW1 and JSW2; however, the example problem has two. The second inlet was handled by internal modifications to the program in the Subroutine ALLMOD, a process required on nearly every combustor analyzed, as a code which makes provisions for all possible configurations would be extremely complex and lengthy. Note that each primary orifice is simulated by three nodes, making the total of radial-injection points equal to six. Inlet conditions for the dome are provided on Card 22, while Cards 23 and 24 describe the fuel nozzle. A back angle (β) of zero would have the nozzle spraying in a purely tangential and in an increasing θ direction. Positive β would have the spray cone rotated toward the dome; therefore, a value of -90 degrees has the spray cone directed axially along the combustor as is required. Zero down angle (δ) was needed for this example. A positive value would, however, rotate the spray cone toward the inner wall. For geometries that have the entire spray cone in the calculation domain, such as this annular one, THETA1 and THETA2 never change from 0 and 360 degrees or their equivalent in whatever angular input units are selected. Cards 25 through 30 are used to describe the cooling slots, of which two were specified (NUINJ = 2 on Card 21). Note that even though the slots surround I-node 16, the I location is specified as one greater (or 17) due to internal conveniences in the program. Similarly, Cards 31 through 38 specify the radial injection points. Due to the sign convention on V-velocity (positive is in the positive y-direction), injection points on the outer wall have a negative V-velocity component, as shown on the last three fields of Card 34.

The output of the 3-D model is illustrated in Figure 18 (7 sheets). Sheet 1 is a printout of some input data, including fuel and air flow rates, injection velocities, and other important quantities. Note that the output units here are S.I. Sheets 2 and 3 show the u -velocities at $\theta = 6$ deg. (in line with the primary holes) after 150 iterations. The total error in mass, i.e., the sum of the mass error in all the grid cells, was 1.5 percent of the total flow, which was deemed accurate enough for this example. The two dome inlets $J = 2-3$ and $J = 17-18$ can be seen at $I = 2$. The u -velocities are calculated for slightly different control volumes than the other variables. The U -velocity printed at $I = 8$, for example is actually the U -velocity that occurs at the cell boundary between $I = 7$ and $I = 8$. This displacement results in the inlet U -velocity being stored at $I = 2$ rather than $I = 1$. A small recirculation zone exists behind the dome and is terminated by the primary orifices at $I = 10, 11$, and 12 . Small recirculation regions are also evident behind each jet at $I = 14$, while the presence of the two cooling slots can be seen at $I = 16$ and 17 . Sheets 3 and 4 of Figure 18 show the fuel mass fractions for the same θ plane. The figure also shows the extremely rich regions just behind the dome at $I = 2-4$ near the fuel nozzle. By the time the exit plane is reached, some unburned fuel still remains. Temperature is shown in Sheets 5 and 6. The fuel-rich region behind the dome (seen in Figure 15) exists at a relatively low temperature as the amount of oxygen is very limited. Farther down the combustor where the primary jets have recirculated ($I = 6, 7$) one sees temperatures closer to stoichiometric. The primary jets penetrate to the combustor centerline as evidenced by the temperature profile at $I = 12$. These jets produce a colder core with hot regions on either side that extend well past the cooling slots at $I = 16$. These slots provide a cool film that extends to the exit of the combustor. Sheets 6 and 7 show the evaporation rate of liquid fuel. One can clearly see the two sides of the spray cone and that some fuel is impinging on the wall at $I = 9$. Practically all the fuel has evaporated

3D PERFORMANCE MODEL EXAMPLE CASE

I. PHYSICAL INPUT

1. FUEL -

HYDROGEN-CARBON RATIO ----- 1.9280E+00 (KG/KGMOLE)
 MOLECULAR WEIGHT ----- 1.3928E+02 (CAL/GMOLE)
 HEAT OF FORMATION ----- -4.9317E+04 (KG/S)
 INLET-1 MASS FLOW RATE ----- 0.0

2. AIR -

PRESSURE ----- 1.0133E+05 (N/M².M)
 INLET-1 MASS FLOW RATE ----- 9.6753E-03 (KG/S)
 INLET-1 AXIAL VELOCITY ----- 1.2192E+02 (M/S)
 INLET-1 SWIRL NUMBER ----- 0.0

II. GEOMETRICAL INPUT

CHANNEL HEIGHT OF COMBUSTOR ----- 9.1440E-02 (M)
 LENGTH OF COMBUSTOR ----- 7.3660E-02 (M)
 ANGLE OF SECTOR ----- 2.0940E-01 (RAD-M)
 INLET-1 FLOW AREA ----- 7.3628E-04 (SQ.M)

III. AIR INJECTIONS

1. FILM COOLING AIR -

SLOT NO	I	J	K
1	17	2	000
2	17	18	000

2. DILUTION AND SECONDARY AIR -

SLOT NO	I	J	K
1	10	1	7
2	11	1	7
3	12	1	7
4	10	19	7
5	11	19	7
6	12	19	7

3. FUEL NOZZLES -

X0	Y0	Z0	ALFA	BETA	DELTA	THETA1	THETA2	NSL	MF	SWP	VFUEL
(M)	(M)	(M-R)	(RAD)	(RAD)	(RAD)	(RAD)	(RAD)		(KG/S)	(MICRON)	(M/S)
1.27E-03	2.29E-02	1.05E-01	1.57E+00	-1.57E+00	0.0	0.0	6.28E+00	2.00E+01	4.84E-04	3.00E+01	3.05E+01

IV. AIR-FUEL BALANCE

TOTAL FUEL FLOW RATE ----- 4.8399E-04 (KG/S)
 TOTAL AIR FLOW RATE ----- 2.4191E-02 (KG/S)
 FUEL TO AIR RATIO ----- 2.0007E-02

MASS FLOW (KG/S)
 3.629E-03
 3.629E-03

U-VELOCITY (M/S)
 0.0
 0.0

V-VELOCITY (M/S)
 2.545E-73
 2.545E-73

FUEL FLOW (KG/S)

MASS FLOW (KG/S)
 1.210E-03
 1.210E-03
 1.210E-03
 1.210E-03
 1.210E-03
 1.210E-03

U-VELOCITY (M/S)
 2.545E-73
 2.545E-73
 2.545E-73
 2.545E-73
 2.545E-73
 2.545E-73

V-VELOCITY (M/S)
 1.219E+02
 1.219E+02
 1.219E+02
 -1.219E+02
 -1.219E+02
 -1.219E+02

U-VELOCITY (M/S)
 2.545E-73
 2.545E-73
 2.545E-73
 2.545E-73
 2.545E-73
 2.545E-73

Figure 18. 3-D Performance Model Output (Sheet 1 of 7).

V. SOME IMPORTANT QUANTITIES

SPECIFIC HEAT	1.1578E+03	1.1578E+03
ACTIVATION ENERGY (E58)	2.7000E+04	2.7000E+04
PRE-EXPOSURE E151	3.3003E+14	3.3003E+14
LOSS BREAKUP CONSTANT (E55)	2.0000E+00	2.0000E+00
ACTIVATION ENERGY (E20)	1.2500E+04	1.2500E+04
PRE-EXPOSURE E151	6.0000E+04	6.0000E+04
EDDY BREAKUP CONSTANT (E20)	4.0000E+00	4.0000E+00
TURB. CONSTANT (E21)	1.5000E+00	1.5000E+00
TURB. CONSTANT (E21)	1.5000E+00	1.5000E+00
ADSORPTION COEFFICIENT	1.0000E+01	1.0000E+01
SCATTERING COEFFICIENT	1.0000E+02	1.0000E+02

U-VELOCITY (M/SEC)

1	2	3	4	5	6	7	8	9	10	11	12	13
19	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
18	1.27E+02	4.47E+01	5.23E+01	5.37E+01	5.29E+01	4.99E+01	4.39E+01	3.04E+01	-1.72E+00	3.34E+00	4.58E+00	1.42E+01
17	1.27E+02	4.47E+01	5.23E+01	5.37E+01	5.29E+01	4.99E+01	4.39E+01	3.04E+01	-1.72E+00	3.34E+00	4.58E+00	1.42E+01
16	0.0	-3.00E+00	9.93E+00	2.31E+01	3.10E+01	3.47E+01	3.32E+01	2.61E+01	3.30E+00	1.01E+01	6.25E+00	5.48E+00
15	0.0	-1.07E+00	1.92E+00	5.53E+00	1.43E+01	2.04E+01	2.37E+01	2.22E+01	9.97E+00	1.08E+01	6.95E+00	5.73E+00
14	0.0	2.04E+00	4.27E+01	3.40E+01	5.24E+00	1.84E+01	1.82E+01	1.80E+01	9.19E+00	5.03E+00	6.84E+00	7.11E+00
13	0.0	4.41E+00	2.55E+00	1.28E+01	1.11E+00	4.44E+00	9.55E+00	1.50E+01	4.51E+00	5.10E+00	6.13E+00	1.30E+01
12	0.0	4.47E+00	2.55E+00	5.40E+00	3.74E+00	3.22E+00	8.51E+01	-1.27E+01	-1.67E+01	-5.64E+00	2.22E+00	2.01E+01
11	0.0	2.97E+00	1.23E+00	5.30E+01	-2.14E+01	-3.09E+01	-6.82E+01	-7.29E+01	-5.37E+01	-2.92E+01	2.54E+00	4.23E+01
10	0.0	-1.07E+01	-2.39E+01	-3.32E+01	-4.17E+01	-5.40E+01	-1.24E+01	-1.24E+01	-2.44E+01	-6.48E+01	6.48E+00	6.50E+01
9	0.0	1.27E+00	2.89E+00	-9.87E+00	-8.54E+00	-3.19E+00	-4.21E+01	1.24E+01	2.49E+00	6.55E+00	6.48E+00	2.15E+01
8	0.0	4.05E+00	2.00E+00	-8.54E+00	-3.19E+00	-4.21E+01	1.24E+01	1.24E+01	1.04E+01	1.01E+01	6.53E+00	9.43E+00
7	0.0	3.16E+00	8.70E+01	1.51E+00	1.40E+00	1.37E+01	1.50E+01	2.44E+01	1.04E+01	1.18E+01	6.53E+00	2.42E+00
6	0.0	4.95E+01	7.12E+01	6.07E+00	1.44E+01	2.28E+01	2.42E+01	2.44E+01	1.04E+01	1.18E+01	6.53E+00	2.42E+00
5	0.0	-2.14E+00	1.24E+01	2.54E+01	3.30E+01	3.58E+01	3.50E+01	2.61E+01	9.35E+00	1.07E+01	5.05E+00	2.24E+00
4	1.27E+02	4.04E+01	6.40E+01	6.29E+01	5.54E+01	5.35E+01	4.41E+01	2.61E+01	6.20E+00	7.44E+00	4.80E+00	5.14E+00
3	1.27E+02	4.04E+01	6.40E+01	6.29E+01	5.54E+01	5.35E+01	4.41E+01	2.61E+01	6.20E+00	7.44E+00	4.80E+00	5.14E+00
2	1.27E+02	4.04E+01	6.40E+01	6.29E+01	5.54E+01	5.35E+01	4.41E+01	2.61E+01	6.20E+00	7.44E+00	4.80E+00	5.14E+00
1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

Figure 18. 3-D Performance Model Output (Sheet 2 of 7).

U-VELOCITY (M/SEC)										
J	I	26	27	28	29	30				
19	0.0	0.0	0.0	0.0	0.0	0.0				
18	3.32E+01	3.28E+01	3.24E+01	3.25E+01	3.25E+01	3.26E+01				
17	2.07E+01	2.13E+01	2.20E+01	2.27E+01	2.28E+01	2.28E+01				
16	2.64E+01	2.63E+01	2.62E+01	2.61E+01	2.61E+01	2.63E+01				
15	2.94E+01	2.92E+01	2.91E+01	2.91E+01	2.91E+01	2.92E+01				
14	3.06E+01	3.05E+01	3.05E+01	3.04E+01	3.04E+01	3.07E+01				
13	3.14E+01	3.14E+01	3.13E+01	3.14E+01	3.14E+01	3.17E+01				
12	3.25E+01	3.24E+01	3.27E+01	3.27E+01	3.27E+01	3.30E+01				
11	3.42E+01	3.41E+01	3.42E+01	3.42E+01	3.42E+01	3.46E+01				
10	3.62E+01	3.63E+01	3.63E+01	3.63E+01	3.63E+01	3.70E+01				
9	3.63E+01	3.63E+01	3.63E+01	3.63E+01	3.63E+01	3.65E+01				
8	3.00E+01	3.01E+01	3.02E+01	3.04E+01	3.04E+01	3.06E+01				
7	2.62E+01	2.63E+01	2.64E+01	2.66E+01	2.66E+01	2.67E+01				
6	2.71E+01	2.72E+01	2.73E+01	2.73E+01	2.73E+01	2.74E+01				
5	2.59E+01	2.58E+01	2.58E+01	2.58E+01	2.58E+01	2.59E+01				
4	2.35E+01	2.35E+01	2.35E+01	2.35E+01	2.35E+01	2.36E+01				
3	1.94E+01	2.01E+01	2.08E+01	2.15E+01	2.15E+01	2.16E+01				
2	3.43E+01	3.56E+01	3.55E+01	3.54E+01	3.54E+01	3.55E+01				
1	0.0	0.0	0.0	0.0	0.0	0.0				

FUEL MASS FRACTION

K = 7												
J	I	2	3	4	5	6	7	8	9	10	11	12
19	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
18	0.0	1.37E-02	1.46E-02	1.47E-02	1.44E-02	1.43E-02	1.41E-02	1.39E-02	1.55E-02	8.44E-04	4.89E-04	1.90E-03
17	0.0	5.10E-02	4.35E-02	3.54E-02	2.89E-02	2.21E-02	1.61E-02	1.55E-02	1.20E-02	1.20E-03	5.25E-04	1.93E-03
16	0.0	2.04E-01	1.31E-01	7.50E-02	5.29E-02	3.88E-02	3.44E-02	2.74E-02	1.24E-02	1.65E-03	5.99E-04	1.97E-03
15	0.0	2.28E-01	1.84E-01	9.98E-02	5.89E-02	5.68E-02	5.24E-02	3.66E-02	1.47E-02	2.22E-03	7.08E-04	1.81E-03
14	0.0	2.40E-01	2.45E-01	1.76E-01	1.04E-01	8.31E-02	6.04E-02	4.36E-02	2.06E-02	3.06E-03	8.47E-04	1.76E-03
13	0.0	2.48E-01	3.03E-01	3.25E-01	2.15E-01	1.88E-01	6.72E-02	4.81E-02	2.66E-02	3.66E-03	9.57E-04	1.72E-03
12	0.0	2.62E-01	3.75E-01	3.78E-01	2.22E-01	1.80E-01	6.40E-02	4.44E-02	1.36E-02	3.50E-03	9.58E-04	1.69E-03
11	0.0	3.03E-01	4.66E-01	4.66E-01	2.63E-01	1.82E-01	2.33E-02	1.17E-02	1.60E-03	2.73E-03	9.58E-04	1.66E-03
10	0.0	2.69E-01	2.55E-01	1.53E-01	7.29E-02	2.97E-02	1.35E-02	8.27E-03	5.48E-03	4.80E-03	1.83E-03	9.69E-04
9	0.0	3.26E-01	4.95E-01	4.95E-01	1.84E-01	1.13E-01	7.96E-02	4.94E-02	2.36E-02	7.60E-03	1.93E-03	8.91E-04
8	0.0	2.92E-01	4.24E-01	4.20E-01	2.33E-01	1.39E-01	7.91E-02	5.42E-02	5.42E-02	8.12E-03	1.93E-03	8.36E-04
7	0.0	2.79E-01	3.58E-01	3.86E-01	2.30E-01	1.39E-01	9.92E-02	7.67E-02	4.83E-02	7.31E-03	1.72E-03	7.86E-04
6	0.0	2.72E-01	3.13E-01	2.44E-01	1.52E-01	1.18E-01	9.00E-02	6.94E-02	3.88E-02	4.84E-03	1.38E-03	7.41E-04
5	0.0	2.66E-01	2.62E-01	1.49E-01	9.98E-02	8.95E-02	7.90E-02	5.94E-02	2.70E-02	2.96E-03	1.12E-03	6.98E-04
4	0.0	2.50E-01	1.94E-01	1.23E-01	8.83E-02	6.44E-02	5.86E-02	4.50E-02	1.77E-02	1.73E-03	9.84E-04	6.66E-04
3	0.0	7.08E-02	6.26E-02	5.41E-02	4.56E-02	3.78E-02	2.83E-02	2.37E-02	1.46E-02	1.00E-03	9.32E-04	6.51E-04
2	0.0	1.82E-01	2.02E-02	2.02E-02	1.99E-02	1.97E-02	1.96E-02	1.95E-02	1.74E-02	5.81E-04	8.70E-04	6.52E-04
1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

Figure 18. 3-D Performance Model Output (Sheet 3 of 7).

J	I = 13	14	15	16	17	18	19	20	21	22	23	24
19	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
18	7.80E-03	9.52E-03	1.54E-02	4.72E-03	8.37E-04	9.74E-04	1.01E-03	1.02E-03	1.03E-03	1.02E-03	1.01E-03	1.00E-03
17	6.86E-03	4.18E-03	1.21E-02	9.33E-03	6.28E-03	2.86E-03	2.42E-03	1.59E-03	1.10E-03	7.98E-04	6.07E-04	4.80E-04
16	6.30E-03	2.78E-03	7.75E-03	6.00E-03	4.34E-03	3.10E-03	2.24E-03	1.64E-03	1.22E-03	9.24E-04	7.09E-04	5.51E-04
15	5.84E-03	2.05E-03	4.99E-03	4.07E-03	3.15E-03	2.41E-03	1.84E-03	1.42E-03	1.11E-03	8.70E-04	6.90E-04	5.53E-04
14	5.40E-03	1.70E-03	3.23E-03	2.78E-03	2.27E-03	1.82E-03	1.46E-03	1.17E-03	9.45E-04	7.65E-04	6.23E-04	5.10E-04
13	4.86E-03	2.07E-03	2.10E-03	1.87E-03	1.60E-03	1.35E-03	1.12E-03	9.35E-04	7.77E-04	6.44E-04	5.39E-04	4.51E-04
12	4.08E-03	3.01E-03	1.86E-03	1.38E-03	1.14E-03	9.64E-04	8.24E-04	7.04E-04	6.01E-04	5.13E-04	4.38E-04	3.74E-04
11	2.58E-03	3.00E-03	2.68E-03	2.30E-03	1.94E-03	1.41E-03	8.37E-04	5.25E-04	4.62E-04	3.89E-04	3.33E-04	2.87E-04
10	1.99E-03	2.13E-03	2.04E-03	1.96E-03	1.75E-03	1.41E-03	8.37E-04	5.25E-04	4.62E-04	3.89E-04	3.33E-04	2.87E-04
9	2.89E-03	2.10E-03	1.16E-03	7.55E-04	5.65E-04	4.49E-04	3.66E-04	3.07E-04	2.59E-04	2.19E-04	1.87E-04	1.61E-04
8	3.69E-03	1.52E-03	1.39E-03	1.18E-03	9.88E-04	8.22E-04	6.83E-04	5.88E-04	5.25E-04	4.74E-04	4.27E-04	3.82E-04
7	4.20E-03	1.55E-03	2.22E-03	1.85E-03	1.51E-03	1.22E-03	9.93E-04	9.17E-04	9.10E-04	8.68E-04	7.97E-04	7.15E-04
6	4.62E-03	1.80E-03	3.29E-03	2.69E-03	2.12E-03	1.66E-03	1.32E-03	1.55E-03	1.81E-03	1.69E-03	1.44E-03	1.23E-03
5	4.96E-03	2.48E-03	4.81E-03	3.79E-03	2.87E-03	2.15E-03	1.68E-03	3.76E-03	4.99E-03	3.48E-03	2.50E-03	1.83E-03
4	5.25E-03	3.50E-03	7.14E-03	5.37E-03	3.82E-03	2.68E-03	1.89E-03	1.26E-03	9.99E-04	7.47E-04	5.68E-04	4.50E-04
3	5.51E-03	5.14E-03	1.00E-02	8.11E-03	5.32E-03	3.23E-03	1.99E-03	1.28E-03	8.61E-04	6.11E-04	4.53E-04	3.50E-04
2	5.40E-03	8.63E-03	1.68E-02	5.24E-03	4.47E-04	5.75E-04	6.02E-04	6.15E-04	6.20E-04	6.19E-04	6.14E-04	6.10E-04
1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

J	I = 25	26	27	28	29	30
19	0.0	0.0	0.0	0.0	0.0	0.0
18	9.86E-04	9.69E-04	9.51E-04	9.31E-04	8.92E-04	0.0
17	3.93E-04	3.51E-04	2.87E-04	2.55E-04	2.12E-04	0.0
16	4.34E-04	3.66E-04	2.80E-04	2.30E-04	1.78E-04	0.0
15	4.47E-04	3.64E-04	2.98E-04	2.44E-04	1.89E-04	0.0
14	4.19E-04	3.47E-04	2.89E-04	2.42E-04	1.89E-04	0.0
13	3.78E-04	3.18E-04	2.69E-04	2.28E-04	1.82E-04	0.0
12	3.20E-04	2.75E-04	2.34E-04	2.04E-04	1.64E-04	0.0
11	2.49E-04	2.17E-04	1.89E-04	1.66E-04	1.38E-04	0.0
10	1.23E-04	1.04E-04	8.97E-05	7.85E-05	6.65E-05	0.0
9	1.40E-04	1.23E-04	1.09E-04	9.81E-05	8.64E-05	0.0
8	3.41E-04	3.05E-04	2.73E-04	2.47E-04	2.15E-04	0.0
7	6.30E-04	5.51E-04	4.79E-04	4.14E-04	3.39E-04	0.0
6	1.92E-03	8.37E-04	6.80E-04	5.65E-04	4.27E-04	0.0
5	1.37E-03	1.03E-03	7.87E-04	6.05E-04	4.25E-04	0.0
4	3.66E-04	3.04E-04	2.54E-04	2.14E-04	1.67E-04	0.0
3	2.80E-04	2.32E-04	1.98E-04	1.72E-04	1.38E-04	0.0
2	6.02E-04	5.92E-04	5.82E-04	5.70E-04	5.45E-04	0.0
1	0.0	0.0	0.0	0.0	0.0	0.0

FUEL MASS FRACTION

Figure 18. 3-D Performance Model Output (Sheet 4 of 7).

TEMPERATURE °K										
I =	25	26	27	28	29	30				
J	1	2	3	4	5	6	7	8	9	10
19	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
18	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
17	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
16	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
15	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
14	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
13	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
12	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
11	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
10	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
9	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
8	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
7	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
6	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
5	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
4	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

EVAPORATION RATE (KG/SEC)										
I =	1	2	3	4	5	6	7	8	9	10
J	1	2	3	4	5	6	7	8	9	10
19	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
18	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
17	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
16	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
15	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
14	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
13	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
12	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
11	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
10	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
9	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
8	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
7	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
6	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
5	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
4	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

Figure 18. 3-D Performance Model Output (Sheet 6 of 7).

I = 13										I = 25										I = 33										
J										J										J										
19	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	19	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	19	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
18	8.31E-07	2.38E-07	0.0	0.0	0.0	0.0	0.0	0.0	0.0	18	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	18	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
17	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	17	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	17	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
16	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	16	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	16	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
15	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	15	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	15	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
14	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	14	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	14	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
13	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	13	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	13	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
12	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	12	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	12	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
11	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	11	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	11	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
10	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	10	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	10	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
9	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	9	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	9	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
8	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	8	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	8	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
7	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	7	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	7	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
6	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	6	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	6	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
5	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	5	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	5	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
4	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	4	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	4	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
3	1.92E-07	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	3	1.92E-07	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	3	1.92E-07	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
2	4.56E-07	2.06E-07	1.76E-06	0.0	0.0	0.0	0.0	0.0	0.0	2	4.56E-07	2.06E-07	1.76E-06	0.0	0.0	0.0	0.0	0.0	0.0	2	4.56E-07	2.06E-07	1.76E-06	0.0	0.0	0.0	0.0	0.0	0.0	0.0
1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

EVAPORATION RATE (KG/SEC)

EVAPORATION RATE (KG/SEC)

Figure 18. 3-D Performance Model Output (Sheet 7 of 7).

by $I = 15$ with a few larger droplets persisting at $I = 20$, where they entered from neighboring K-planes.

LINER-COOLING MODEL.

The liner-cooling model was used to predict the wall temperatures downstream of the cooling slots in the combustor shown in Figure 15. Starting with the profiles at the exit of the slot, as predicted by the 3-D performance model, the program marched up to the beginning of the transition liner. At each marching step, the program performed a heat-flux balance at the wall and, thereby, obtained the wall temperature.

The input units, required by the liner-cooling model, are S.I., and since these are the output units of the 3-D performance model, data is easily transferred. Profiles for U-velocity, temperature, turbulent kinetic energy, turbulence length scale, fuel-mass fraction, total fuel, and CO are required along with information about the flow conditions in the inner and outer annuli. Since nearly all the liquid fuel has evaporated at the point where the marching process begins, no input for the droplet evaporation is needed.

The input data sheets (Figure 19, 3 sheets) begin with two cards devoted to case identification (additional input information can be found in the input sheet forms located in Appendix A). Next, 40 cross stream grid cells are specified. It was unlikely that this would be sufficient to obtain a grid-independent solution; however, since this was merely an example case, the maximum dimension allowed in the existing deck was selected. Axisymmetric geometry, solve species equations, two-equation turbulence model, reacting species, wall temperature, and enthalpy calculation completed the specifications on Card 2. Card 3 indicates that the various profiles will be printed every 20 marching steps. On Card 4 one sees that the marching process will start at

CASE TITLE (12A6)

1

LINER COOLING	MODEL	EXAMPLE	CASE			
---------------	-------	---------	------	--	--	--

CASE TITLE (12A6)

KPLANE= 7						
-----------	--	--	--	--	--	--

(8(12, 8X))

2

N	KRAD	MASSTR	ISWRL	MODEL	INERT	IFLUX	ITEMP
40	01	01	00	02	02	01	01

3

NSTAT	NPROF	NPLOT	ITEST	LASTEP			
99999	00020	99999		99999			

(5(15.5X))

4

XU	XULAST	FRA	XEND	XOUT	PRESS	POWER	(8E10.4)
.03937	.073	.02	10.	10.	101325	2.0	

NBP (12)

5

02							
----	--	--	--	--	--	--	--

(8E10.4)

6

X ₁	RI ₁	RE ₁	X ₂	RI ₂	RE ₂	X ₃	RI ₃
0.	.254	.29972	10.	.254	.29972		

RE₁ X₄ RI₄ RE₄ X₅ RI₅ RE₅... (8E10.4)

--	--	--	--	--	--	--	--

RA RB RD (8E10.4)

7

0.	.254	.29972					
----	------	--------	--	--	--	--	--

Figure 19. Liner Cooling Model Input Sheet (1 of 3)

NAME LIST								
8	SINPUT	ICREAD	=1	PREXP1	=3.3E+14	ARCONI	=27000	\$
CRI = 3.0, CX = 10, MY = 19.28								
9	UA	UD	(8E10.4)					
	0.	0.						
10	F2A	F2D	TA	TD	T _{wall}	(8E10.4)		
	0.	0.	589.	589.	589.			
11	NIN	(I2)						
	19							
12	Y VALUES						(8E10.4)	
13	U VALUES						(8E10.4)	
14							(8E10.4)	
15	TEMPERATURE VALUES						(8E10.4)	
16	MFU VALUES						(8E10.4)	
17	PHI VALUES						(8E10.4)	

Figure 19. Liner Cooling Model Input Sheet (2 of 3)

18	MCO VALUES						(8E10.4)
19	TURBULENT KINETIC ENERGY						(8E10.4)
20	TURBULENCE LENGTH SCALE						(8E10.4)
21	VELA _I	VELA _O	TAN _I	TAN _O	PR _I	PR _O	(8E10.4)
	24.7	58.8	589.	589.	.2413	.3124	
22	(12, 8X, 7E10.4)						
	NFNZ	XDP	YDP	UF	VF	SMD	WF TFUEL
	00						

Figure 19. Liner Cooling Model Input Sheet (3 of 3)

0.03937 meter and proceed to 0.073 meter, using a step size of 0.02 times the grid height. In order to obtain the best estimation of the radiation flux, it is necessary to analyze the entire channel height, which means the inner and outer boundaries are walls. XEND and XOUT are, therefore, set to some large number. The variable POWER is used to distort the grid, since more nodes are required near the wall whose temperature is being predicted. This means, of course, that two runs must be made, one with the grid nodes concentrated near the outer wall (POWER ≤ -1.0), and one with the nodes concentrated near the inner wall (POWER ≥ 1.0). If POWER equals 1.0 or -1.0, the resulting grid would be uniform in y.

Two straight walls require only two boundary point specifications, handled by Cards 5 and 6. The three radii specified on Card 7 are also easily understood. The name list is read next with the variables specified explained in the name list input sheet. The values on Cards 9 and 10 pertain to the free boundaries, which are not used on this program; however, entries are made for completeness. Cards 11 through 20 specify the initial profiles. The 19 points used correspond to the 19 radial nodes used by the 3-D performance model and are listed in Table 1. For this example the 3-D output was strictly used; however, it is usually the practice to combine the 3-D profiles with some additional information, if available, describing the profiles inside the slot lip. Card 21 lists data concerning the annulus flow conditions and dimensions while Card 22 is blank due to the absence of liquid fuel.

The output from the program is shown in Figure 20 (3 sheets). Sheet 1 begins with the titles, some control indices, and the values of omega for the transformed cross-stream variable. Information about the annuli is printed next along with the initial profiles. The printing of the variable arrays starts with the value at the inner boundary and continues outward.

TABLE 1. INITIAL PROFILES FOR LINER COOLING EXAMPLE.

Node	Y	U	KE	l _m	φ	MFU	MCO	TEMP
19	0.04572	45.7	6.27	7.62E-5	0	0	0	589
18	0.04318	45.7	6.27	7.62E-5	0	0	0	589
17	0.04064	26.1	13.5	2.86E-4	0.0273	7.8E-3	0.0190	1135
16	0.03810	28.2	51.9	3.68E-4	0.0270	5.17E-3	0.0205	1210
15	0.03556	25.5	65.7	4.22E-4	0.0270	3.61E-3	0.0198	1270
14	0.03302	22.2	71.7	4.76E-4	0.0269	2.53E-3	0.0182	1320
13	0.03048	20.3	73.3	4.81E-4	0.0265	1.73E-3	0.0158	1355
12	0.02794	21.8	77.5	4.66E-4	0.0239	1.26E-3	0.0141	1300
11	0.02540	40.6	126	3.11E-4	0.0154	1.87E-3	0.00976	1018
10	0.02286	53.4	277	2.74E-4	0.0117	1.86E-3	0.00713	905
9	0.02032	21.0	123	4.72E-4	0.0233	6.6E-4	0.0120	1315
8	0.01778	15.3	83.3	5.17E-4	0.0283	1.08E-3	0.0129	1460
7	0.01524	16.2	76.8	4.87E-4	0.0288	1.68E-3	0.0166	1425
6	0.01270	19.2	71.5	4.52E-4	0.0291	2.41E-3	0.0195	1385
5	0.01016	23.0	65.5	4.15E-4	0.0294	3.33E-3	0.0215	1350
4	0.00762	25.9	52.3	3.62E-4	0.0298	4.60E-3	0.0228	1305
3	0.00508	24.1	12.9	2.87E-4	0.0302	6.72E-3	0.0227	1250
2	0.00254	45.7	6.27	7.62E-5	0	0	0	589
1	0.0000	45.7	6.27	7.62E-5	0	0	0	589

U-Values are for K = 7, I = 17 Other Values are for K = 7
and the avg. of I = 16 and 17.

STEP=	0	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84	85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100	101	102	103	104	105	106	107	108	109	110	111	112	113	114	115	116	117	118	119	120	121	122	123	124	125	126	127	128	129	130	131	132	133	134	135	136	137	138	139	140	141	142	143	144	145	146	147	148	149	150	151	152	153	154	155	156	157	158	159	160	161	162	163	164	165	166	167	168	169	170	171	172	173	174	175	176	177	178	179	180	181	182	183	184	185	186	187	188	189	190	191	192	193	194	195	196	197	198	199	200	201	202	203	204	205	206	207	208	209	210	211	212	213	214	215	216	217	218	219	220	221	222	223	224	225	226	227	228	229	230	231	232	233	234	235	236	237	238	239	240	241	242	243	244	245	246	247	248	249	250	251	252	253	254	255	256	257	258	259	260	261	262	263	264	265	266	267	268	269	270	271	272	273	274	275	276	277	278	279	280	281	282	283	284	285	286	287	288	289	290	291	292	293	294	295	296	297	298	299	300	301	302	303	304	305	306	307	308	309	310	311	312	313	314	315	316	317	318	319	320	321	322	323	324	325	326	327	328	329	330	331	332	333	334	335	336	337	338	339	340	341	342	343	344	345	346	347	348	349	350	351	352	353	354	355	356	357	358	359	360	361	362	363	364	365	366	367	368	369	370	371	372	373	374	375	376	377	378	379	380	381	382	383	384	385	386	387	388	389	390	391	392	393	394	395	396	397	398	399	400	401	402	403	404	405	406	407	408	409	410	411	412	413	414	415	416	417	418	419	420	421	422	423	424	425	426	427	428	429	430	431	432	433	434	435	436	437	438	439	440	441	442	443	444	445	446	447	448	449	450	451	452	453	454	455	456	457	458	459	460	461	462	463	464	465	466	467	468	469	470	471	472	473	474	475	476	477	478	479	480	481	482	483	484	485	486	487	488	489	490	491	492	493	494	495	496	497	498	499	500	501	502	503	504	505	506	507	508	509	510	511	512	513	514	515	516	517	518	519	520	521	522	523	524	525	526	527	528	529	530	531	532	533	534	535	536	537	538	539	540	541	542	543	544	545	546	547	548	549	550	551	552	553	554	555	556	557	558	559	560	561	562	563	564	565	566	567	568	569	570	571	572	573	574	575	576	577	578	579	580	581	582	583	584	585	586	587	588	589	590	591	592	593	594	595	596	597	598	599	600	601	602	603	604	605	606	607	608	609	610	611	612	613	614	615	616	617	618	619	620	621	622	623	624	625	626	627	628	629	630	631	632	633	634	635	636	637	638	639	640	641	642	643	644	645	646	647	648	649	650	651	652	653	654	655	656	657	658	659	660	661	662	663	664	665	666	667	668	669	670	671	672	673	674	675	676	677	678	679	680	681	682	683	684	685	686	687	688	689	690	691	692	693	694	695	696	697	698	699	700	701	702	703	704	705	706	707	708	709	710	711	712	713	714	715	716	717	718	719	720	721	722	723	724	725	726	727	728	729	730	731	732	733	734	735	736	737	738	739	740	741	742	743	744	745	746	747	748	749	750	751	752	753	754	755	756	757	758	759	760	761	762	763	764	765	766	767	768	769	770	771	772	773	774	775	776	777	778	779	780	781	782	783	784	785	786	787	788	789	790	791	792	793	794	795	796	797	798	799	800	801	802	803	804	805	806	807	808	809	810	811	812	813	814	815	816	817	818	819	820	821	822	823	824	825	826	827	828	829	830	831	832	833	834	835	836	837	838	839	840	841	842	843	844	845	846	847	848	849	850	851	852	853	854	855	856	857	858	859	860	861	862	863	864	865	866	867	868	869	870	871	872	873	874	875	876	877	878	879	880	881	882	883	884	885	886	887	888	889	890	891	892	893	894	895	896	897	898	899	900	901	902	903	904	905	906	907	908	909	910	911	912	913	914	915	916	917	918	919	920	921	922	923	924	925	926	927	928	929	930	931	932	933	934	935	936	937	938	939	940	941	942	943	944	945	946	947	948	949	950	951	952	953	954	955	956	957	958	959	960	961	962	963	964	965	966	967	968	969	970	971	972	973	974	975	976	977	978	979	980	981	982	983	984	985	986	987	988	989	990	991	992	993	994	995	996	997	998	999	1000
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Figure 20. Liner Cooling Model Output (Sheet 3 of 3).

Since y is always referenced from the inner boundary, $y(1)$ is always zero, so the radius of the inner boundary is printed in its place. It can also be seen that the y values are more closely spaced near the inner boundary, since this was the wall temperature that was calculated during this run. Sheets 2 and 3 of Figure 20 show a printout after 80 marching steps as indicated by ISTEP. The program has traversed to an X -location (XU) of 0.0706 meter, which is very near the end of the combustor. At this position the inner-wall temperature is 958°K . The other profiles are also printed with KE being the turbulent kinetic energy, LEN the turbulence length scale, PHI the total fuel, RAD the radiation-composite flux, and $AMU(I)$ the effective viscosity. It should be noted that the boundary values of the radiation-composite flux are never used and are therefore left at their initial values.

TRANSITION MIXING MODEL

The 3-D performance model was used to predict the flow field up to the end of the combustor liner (Figure 15), but it is not capable of handling the geometric configuration of the transition liner. For that, the transition-mixing model (TMM) is used. Using initial profiles as predicted by the 3-D program, the TMM marches through the transition liner, thereby predicting the temperature distribution at what would be the turbine-stator inlet.

An enlarged drawing of the transition liner is shown in Figure 21. The inlet and exit planes are marked along with several intermediate ones. The location of these is a matter of user choice, but should be enough to simulate the actual liner-wall geometry. The radius of curvature is constant. In this case it is 0.5 inch for the inner wall and 1.9 inches for the outer wall. The input sheets are shown in Figure 22 (3 sheets). (Additional input information can be found in the input sheet forms located in Appendix A.) Card 1 is allocated to case identification. Card 2 shows that 40 cross-stream intervals are selected along with axisymmetric geometry, $K-\epsilon$ viscosity model, and

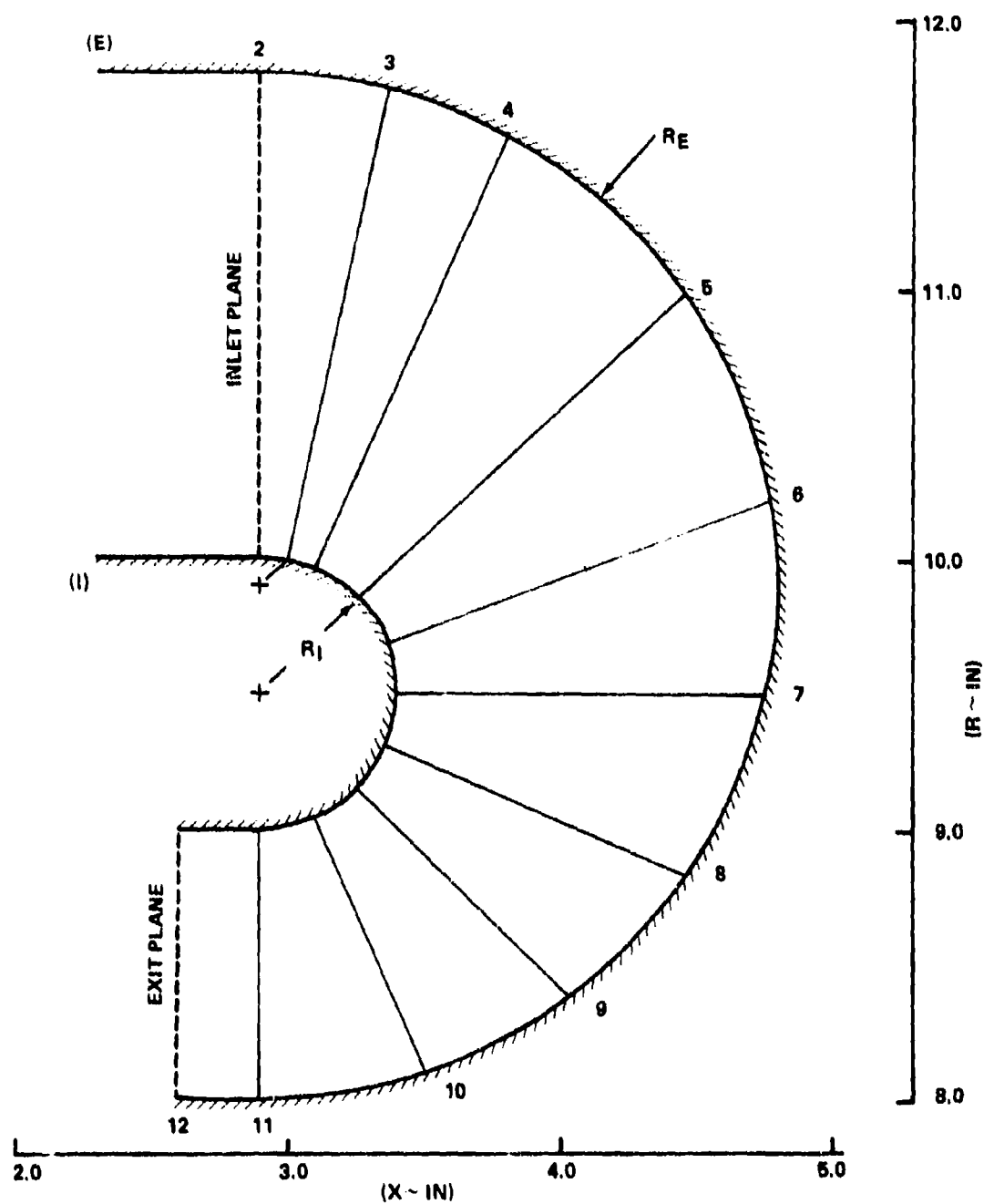


Figure 21. Transition Mixing Example Geometry.

CASE TITLE CARD (12A6)							
1	TRANSITION MIXING	MODEL	EXAMPLE				
CASE TITLE CARD (12A6)							
	KPLANE = 7						
(8(12, 8X))							
2	N	KRAD	MASSTR	ISWRL	MODEL	INERT	IFLUX ITEMP
	40	01	00	00	02	01	00 01
(5(15, 5X))							
3	NSTAT	NPROF	NPLOT	ITEST	LASTEP		
	99999	00020	99999		99999		
(8E10.4)							
4	ZUI	ZUE	ZULAST	FRA	ZEND	ZOUT	PRESS POWER
	.07366	.07366	.2316	.02	10.	10.	101325 1.0
(8(12, 8X))							
5	NBP	ICURV	NRCVI	NRCVE			
	12	01	06	06			
(8E10.4)							
6	RI ₁	XI ₁	RI ₂	XI ₂	RI ₃	XI ₃	RI ₄ XI ₄ ...
(8E10.4)							
	RE ₁	XE ₁	RE ₂	XE ₂	RE ₃	XE ₃	RE ₄ XE ₄ ...
(8E10.4)							
7	ZI ₁	RCVI ₁	ZI ₂	RCVI ₂	ZI ₃	RCVI ₃	ZI ₄ RCVI ₄ ...

Figure 22. Transition Mixing Model Input Sheet (1 of 3)

(8E10.4)							
	ZE ₁	RCVE ₁	ZE ₂	RCVE ₂	ZE ₃	RCVE ₃	ZE ₄ RCVE ₄ ...
8	RA	RB	RD	(8E10.4)			
	0.	.254	.29972				
9	NAMELIST						
	\$INPUT	KREAD	= 1				\$
10	UA	UD	(8E10.4)				
	0	0					
11	F2A	F2D	TA	TD	T _{wall}	(8E10.4)	
	0	0					
12	NIN	(I2)					
	19						
13	Y VALUES						(8E10.4)
14	U VALUES						(8E10.4)
15							
16	TEMPERATURE VALUES						(8E10.4)

Figure 22. Transition Mixing Model Input Sheet (2 of 3)

17							
18							
19							
20	TURBULENT KINETIC ENERGY					(8E10.4)	
21	TURBULENCE LENGTH SCALE					(8E10.4)	

Figure 22. Transition Mixing Model Input Sheet (3 of 3)

nonisothermal flow. Card 3 will allow a printout of the variable profiles at every 20 marching steps. The initial and final values of Z and the marching direction are placed on Card 4 along with the control on step size. Since the boundaries are always walls, ZOUT and ZEND are set to a large number while POWER equal to 1.0 forces the initial grid to be uniform in y . POWER >1.0 will distribute more nodes near the inner wall while $0 < \text{POWER} < 1.0$ will distort the grid toward the outer wall. Next, the number of boundary points and number of radius-of-curvature points are specified separated by a flag to indicate that radius-of-curvature effects are to be included. Card set 6 and 7 reads the actual boundary and curvature values which are listed in Table 2. The values listed are in inches and had to be converted to meters since the TMM requires S.I. units. The initial and final values of radius-of-curvature were just chosen to be a large (1000m) number. Cards 8 and 9 are quite obvious with the name-list variables listed with the input forms. Cards 10 and 11 deal with "free" boundaries, which are not used for this program, so the values listed are only for completeness. Card 12 indicates that 19 points on the input initial profile were used and correspond to the 19 radial nodes employed by the 3-D program. The various profiles are read on Cards 13 to 21 and are listed in Table 3. These profiles are merely the exit plane profiles for $\theta = 6$ degrees (in line with the primary orifices) as obtained from the 3-D output.

The output of the TMMs is illustrated in Figure 23 (4 sheets). It begins with a list of control indices and important quantities followed by ω , the transformed cross-stream variable. The specified boundary values of X and R for the inner and outer wall along with the value of Z , the distance along the wall, are listed next. Following these are the values of radius-of-curvature and the initial profiles. Printing of the variable arrays starts with the value at the inner boundary and continues outward. Since y is always referenced from the inner boundary,

TABLE 2. TRANSITION MIXING MODEL GEOMETRY INPUT.

<u>Point</u>	<u>XI</u>	<u>RI</u>	<u>XE</u>	<u>RE</u>
1	0.0	10.0	0.0	11.8
2	2.9	10.0	2.9	11.8
3	3.01	9.99	3.37	11.73
4	3.10	9.96	3.80	11.56
5	3.26	9.85	4.45	10.98
6	3.37	9.68	4.76	10.20
7	3.40	9.50	4.75	9.50
8	3.37	9.30	4.45	8.79
9	3.26	9.14	4.02	8.38
10	3.10	9.04	3.51	8.10
11	2.90	9.00	2.90	8.00
12	2.60	9.00	2.60	8.00

<u>Point</u>	<u>ZI</u>	<u>RCVI</u>	<u>ZE</u>	<u>RCVE</u>
1	0.0	39370.0	0.0	39370.0
2	2.9	39370.0	2.9	39370.0
3	3.01	0.5	3.37	1.9
4	4.27	0.5	8.19	1.9
5	4.47	39370.0	8.81	39370.0
6	4.77	39370.0	9.11	39370.0

TABLE 3. INITIAL PROFILES (SI UNITS) FOR TRANSITION MIXING
EXAMPLE

Node	r	u	KE	lm	Temp.
19	0.04572	32.6	15.6	5.86E-4	879
18	0.04318	32.6	15.6	5.86E-4	879
17	0.04064	22.8	18.0	6.03E-4	1310
16	0.03810	26.3	27.0	6.16E-4	1470
15	0.03556	29.2	30.3	6.50E-4	1530
14	0.03302	30.7	30.6	6.64E-4	1560
13	0.03048	31.7	29.6	6.65E-4	1570
12	0.02794	33.0	28.7	6.59E-4	1560
11	0.02540	34.6	29.9	6.42E-4	1530
10	0.02286	37.0	61.8	4.65E-4	1470
9	0.02032	34.5	42.9	6.24E-4	1550
8	0.01778	30.6	27.0	6.58E-4	1660
7	0.01524	28.7	26.4	6.57E-4	1700
6	0.01270	27.4	27.8	6.59E-4	1720
5	0.01016	25.9	28.3	6.49E-4	1690
4	0.00762	23.6	25.3	6.21E-4	1570
3	0.00508	21.6	20.4	6.10E-4	1370
2	0.00254	33.5	16.4	5.88E-4	879
1	0.00000	33.5	16.4	5.88E-4	879

K = 7

Y(1) is always zero; therefore, the radius of the inner boundary is printed instead. Note that the pressure variation across the grid (PRESS) is essentially zero due to the large values of radius-of-curvature (RCVI, RCVE) specified at the inlet plane. Sheets 2 and 3 of Figure 23 show the printout after 160 marching steps. Along the outer boundary, the program has marched to 0.1639 meter (ZUE), but the inner boundary is only to 0.09497 meter (ZUI). At this point, there exists a considerable radial pressure gradient with the inner wall at 744 N/m^2 lower pressure than the outer. In addition, the velocity profile is distorted so that the maximum is very near the inner wall. Sheets 3 and 4 of Figure 23 show the output at the exit plane. The radial-pressure gradient disappears as the radius-of-curvature effects are no longer present. A plot of velocity and temperature is also made. The top line of the plot corresponds to the inner boundary while the bottom line is the outer. However, it must be remembered that the inner boundary here is located at what would be the stator-blade tip and the outer at what would be the blade root.

EMISSION MODEL

The calculation domain that would be used by the emission model to predict the emission output of the example combustor is illustrated in Figure 24. Starting with the initial profiles near the dome, the program marches using the recirculation zone as the inner boundary. The mass and specie concentrations in the recirculation zone can be estimated or calculated by several methods, and this provides an entrainment rate and boundary conditions. Once the centerline of the combustor is reached, the inner boundary switches to an axis of symmetry. Cooling slots and radial-injection points can be handled without stopping the marching process. To input the information necessary to perform the above calculation would be quite lengthy and illustrates nothing about the emission program. Usually, the boundary along

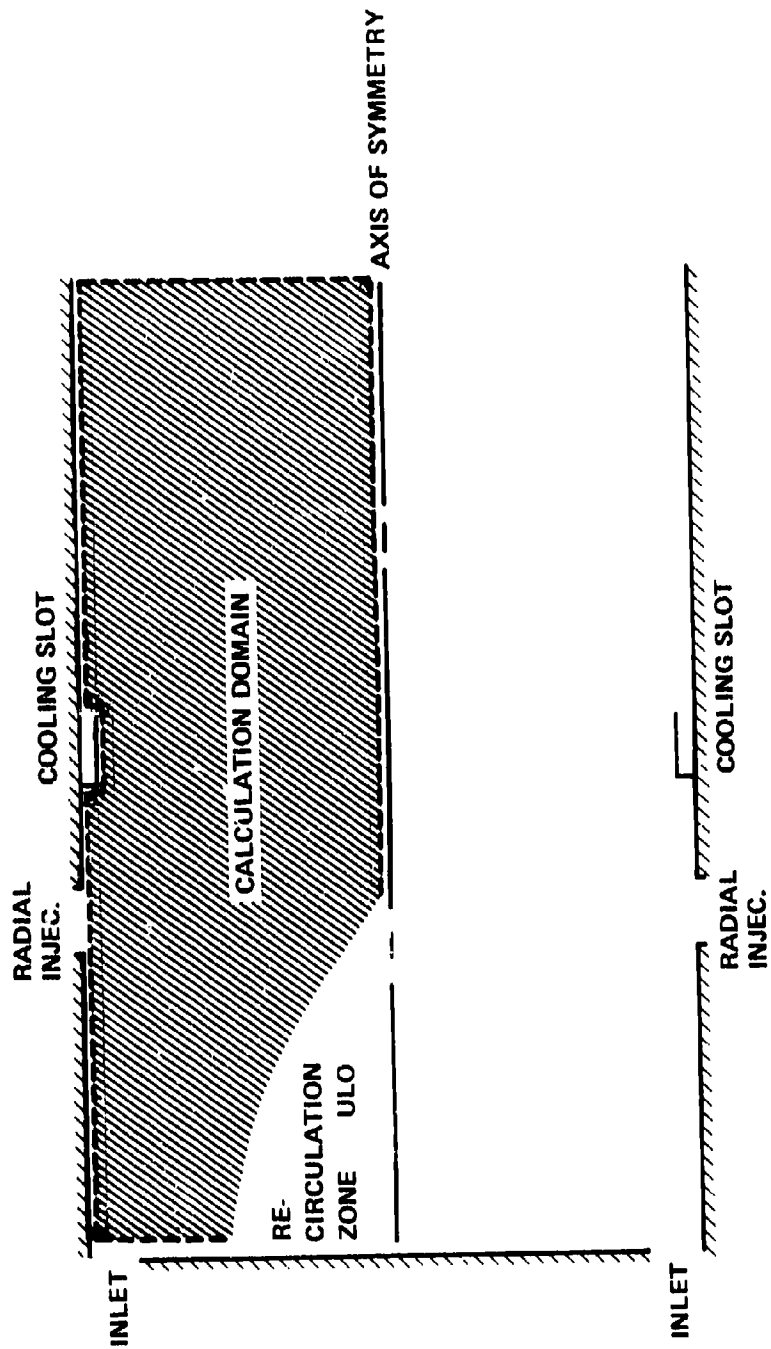


Figure 24. Calculation Domain for Predicting Emission Output of Example Combustor.

the recirculation zone must be handled in a manner that requires internal modifications to the program similar to the Cards MA.528 through MA.743 that are unique to each case analyzed. Therefore, for the example case (Figure 25) the program is started at the downstream edge of the cooling-slot lip and marched to the exit of the liner.

As illustrated in Figure 25, card set 1 is available for case identification. Card 2 specifies 30 cross-stream intervals, axisymmetric geometry, species, two-equation turbulence model, reaction and nonisothermal conditions, while Card 3 produces a profile printout at every 40 marching steps. The initial and final x locations are read on Card 4 and have units of meters, since all the units of the emission model are S.I. The step size was chosen to be small as is necessary with the 16-step kinetic scheme. Since the boundaries are always walls, XOUT AND XEND are set to a large number. A value of POWER equal to 1.0 provides an initial grid that is uniform in y. POWER >1.0 places more nodes near the inner boundary while POWER <-1.0 places more nodes near the outer boundary. Since both walls are straight, only two boundary points are needed, Cards 5 and 6. Cards 7 and 8 define the initial grid, inner and outer radii, and the name-list quantities. Cards 9 and 10 deal with quantities at free boundaries, which are not used, so the data is included only for completeness. The initial profiles are the same as those used in the wall-cooling model example. Nineteen points are used and correspond to the 19 radial nodes used in the 3-D performance model. Three additional profiles, listed in Table 4, are needed for the 16-step-reaction scheme. Since for this case there are no cooling slots or radial injections, the remaining Cards, 24 through 51, are omitted.

CASE TITLE CARD (12A6)

1	EMISSION	MODEL	EXAMPLE				
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CASE TITLE CARD (12A6)

KPLANE	=7						
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(8(I2, 8X))

N	KRAD	MASSTR	ISWRL	MODEL	INERT	IFLUX	ITEMP
2	30	01	01	00	02	02	00

(5(I5, 5X))

NSTAT	NPROF	NPLOT	ITEST	LASTEP			
3	99999	00040	99999		99999		

(8E10.4)

XU	XULAST	FRA	XEND	XOUT	PRESS	POWER	
4	.03937	.073	.01	10.	10.	101325	1.0

(I2)

NBP							
5	02						

X_1	RI_1	RE_1	X_2	RI_2	RE_2	X_3	RI_3
6	0	.254	.29972	10.	.254	.29972	

RE_3	X_4	RI_4	RE_4	X_5	RI_5	$RE \dots$	(8E10.4)

(8E10.4)

RA	RB	RD					
7	0	.254	.29972				

Figure 25. Emissions Model Input Sheet (1 of 4)

NAMelist

8

SINPUT	KREAD=1	PREXD1=2	PEH16	ARGON1=54000		\$
--------	---------	----------	-------	--------------	--	----

 CRI=3.0, CX=10, MY=19.28, ERO=1.5, EFU=.5, EO2=1.0
 EH2O=0.

9

UA	UD	VTA	VD	(8E10.4)			
0	0	0	0				

10

F2A	F2D	TA	TD	T _{wall}	(8E10.4)		
0	0	589	589	589			

11

NIN	NUI	NUE	NVI	NVE	(5 (I2, 8X))		
19	00	00	00	00			

12

Y VALUES (8E10.4)							

13

U VALUES (8E10.4)							

14

V _θ VALUES (8E10.4)							

15

TEMPERATURE VALUES (8E10.4)							

16

MFU VALUES (8E10.4)							

17

MCO ₂ VALUES (8E10.4)							

Figure 25. Emissions Model Input Sheet (2 of 4)

18	MCO VALUES							(8E10.4)
19	MOX VALUES							(8E10.4)
20	MH ₂ O VALUES							(8E10.4)
21	MH ₂ VALUES							(8E10.4)
22	TURBULENT KINETIC ENERGY							(8E10.4)
23	TURBULENCE LENGTH SCALE							(8E10.4)
SKIP FOLLOWING CARD SET IF NUI = 0								
24	X - LOC. OF INTERNAL COOLING SLOTS							(8E10.4)
25	LIP LENGTH OF INTERNAL COOLING SLOTS							(8E10.4)
26	U - VELOCITY OF INTERNAL COOLING SLOTS							(8E10.4)
27	VT - VELOCITY OF INTERNAL COOLING SLOTS							(8E10.4)

Figure 25. Emissions Model Input Sheet (3 of 4)

		TEMPERATURE OF INTERNAL COOLING SLOTS						(8E10.4)
		FLOW RATE OF INTERNAL COOLING SLOTS						(8E10.4)
29								
		SLOT HEIGHT OF INTERNAL COOLING SLOTS						(8E10.4)
30								
		SLOT TO METERING AREA RATIO FOR INT SLOTS						(8E10.4)
31								
<div> <div>SKIP FOLLOWING CARD SET IF NUE = 0</div> <div></div> </div>								
		X-LOC OF EXTERNAL COOLING SLOTS						(8E10.4)
32								
		LIP LENGTH OF EXTERNAL COOLING SLOTS						(8E10.4)
33								
		U - VELOCITY OF EXTERNAL COOLING SLOTS						(8E10.4)
34								
		V_T - VELOCITY OF EXTERNAL COOLING SLOTS						(8E10.4)
35								

Figure 25. Emissions Model Input Sheet (4 of 4)

TABLE 4. ADDITIONAL PROFILES FOR EMISSION MODEL.

Node	M_{CO_2}	M_{OX}	M_{H_2O}
19	0	0.232	0
18	0	0.232	0
17	0.0318	0.170	0.0243
16	0.0368	0.163	0.0272
15	0.0311	0.157	0.0291
14	0.0484	0.153	0.0304
13	0.0534	0.151	0.0309
12	0.0494	0.157	0.0282
11	0.0274	0.188	0.0169
10	0.0199	0.200	0.0123
9	0.0527	0.156	0.0282
8	0.0657	0.140	0.0339
7	0.0596	0.142	0.0338
6	0.0537	0.146	0.0333
5	0.0486	0.149	0.0325
4	0.0438	0.152	0.0314
3	0.0400	0.158	0.0293
2	0	0.232	0
1	0	0.232	0

The output of the emission model is shown in Figures 26 and 27. The initial printout consists of some control parameters, the value omega (the transformed cross-stream variable), and the initial profiles. The printing of the variable arrays starts with the value at the inner boundary and continues outward. Since y is always referenced from the inner boundary, y(1) is always zero; therefore, the radius of the inner boundary is printed instead. Figure 27 shows the profiles at the exit of the combustor, $XU = 0.073$ meter. The profiles of NO show small values (much less, however, than one would expect as the principal area of NO formation) occur upstream of where the emission model is started.

FUEL-INSERTION MODEL

The fuel-insertion model could have been used to predict the droplet trajectories of the nozzle in the 3-D performance model example case, Figure 28; however, since that program contains its own spray model, a simple illustrative example was selected instead. A two-dimensional grid 5.0 X 1.5 inches, with the spray originating in the lower left-hand corner and processing a non-uniform flow field, was analyzed.

Card 1 (Figure 28, Sheet 1) allows for case identification. Card 2 specifies the atomizer type, in this case an airblast nozzle with a 10 flow no. and 90-degree cone angle. The other fields are left blank as they pertain to dual orifice and/or simplex nozzles. Cards 3 and 4 are omitted as they are used to input the ΔP versus fuel-flow curve for the secondaries of a dual-orifice nozzle. Card 5 specifies some dimensions of the airblast nozzle, the filming diameter, and exit-flow area along with the airflow rate and temperature. The fuel type, flow rate, and temperature are given on Card 6, plus the flag to specify a nonuniform 2-D field. Other quantities on Card 6 are required only for other

1 TITLE										80
FUEL INSERTION MODEL EXAMPLE										
PRIM SEC. AIR ** FLOW FLOW ASSIST ATOM AIR NO. NO. CONE SHROUD PRIM SEC TYPE ASSIST(JP4) (JP4) ANGLE EFF ORIFICE ORIFICE PPH/ $\sqrt{\text{PSI}}$ IN ² IN IN 1 - 6 - 11 21 31 41 51 61 71 80										
2	3	1	10.		90.					
*ATOMIZER TYPE: 00001 = SIMPLEX 00002 = DUAL ORF 00003 = AIR BLAST **AIR ASSIST: 00001 = NO ASSIST 00002 = WITH ASSIST *FOR ATOM TYPE = 00002 (DUAL ORIF) ONLY (LEAVE OUT FOR OTHERS) INPUT SECONDARY FLOW SCHEDULE W_s = SECONDARY FUEL FLOW, LB/HR ΔP_s = $\Delta P_{\text{SEC. ORIF}}$ + $\Delta P_{\text{FLOW DIVIDER VALVE}}$ P/D CRACK POINT FLOW W_{s1} W_{s2} W_{s3} W_{s4} W_{s5} 51 1 11 21 31 41 51 3										
CRACK PRESSURE ΔP_1 ΔP_2 ΔP_3 ΔP_4 ΔP_5 51 1 11 21 31 41 51 4										
*FOR ATOM TYPE = 00003 (AIRBLAST) ONLY (LEAVE OUT FOR OTHERS) FILMING NOZZLE FLOW AIR DIA AIRFLOW AREA TEMP IN. LB/SEC IN ² °R 1 11 21 31 5										
0.5 .05 .2 1060.										

Figure 28. Fuel Insertion Model Input (1 of 3)

 *** AIR FUEL FUEL FUEL AIR AIR
 FUEL FLOW TEMP FLOW ΔP ΔP ASSIST ASSIST
 TYPE OPTION °R LB/HR PSI PSI °R
 1 - 6 - 11 21 31 41 51 61 71
 6

2	2	520.	60.					
---	---	------	-----	--	--	--	--	--

***FUEL 00002=JP5 ***AIR
 TYPE 00004=JP4 FLOW
 OPTION 00001=UNIFORM GAS STREAM
 00002=2-D FIELD OPTION

T_{GAS}, °R V_{GAS}, P_{GAS}, X_{MAX}, Y_{MAX}, ← UNIFORM STREAM
 1 11 FPS 21 PSIA 31 IN. 4 °R 51 OPTION
 7

.2	.2	147.	5.0	1.5			
----	----	------	-----	-----	--	--	--

X_{NOZ} IN. Y_{NOZ} IN. P_{GAS} PSIA X_{MAX} IN. Y_{MAX} IN. ← Z-D FIELD OPTION

CARDS 8 THROUGH 13 SKIPPED IF AIR FLOW OPTION = 00001

IN = NO. OF X-DIR POINTS IN 2-D FIELD
 JN = NO. OF Y-DIR POINTS
 8

03	03						
----	----	--	--	--	--	--	--

X VALUES (8E10.4) X - LOCATIONS OF GRID POINTS (FT)
 9

0.	.2083	.4167					
----	-------	-------	--	--	--	--	--

Y VALUES (8E10.4) Y - LOCATIONS OF GRID POINTS (FT)
 10

0.	.0625	.125					
----	-------	------	--	--	--	--	--

READ ALONG + X LINES STARTING WITH
 U VALUES (8E10.4) SMALLEST Y VALUE (FT/SEC)
 11

30.	75.	100.					
35.	80.	110.					

40.	85.	115.					
-----	-----	------	--	--	--	--	--

Figure 28. Fuel Insertion Model Input (2 of 3)

		READ ALONG + X LINES STARTING WITH SMALLEST Y VALUE (FT/SEC)							
12	V VALUES (SE10.4)	0.	0.	0.					
		0.	0.	0.					
		0.	0.	0.					
13	T VALUES (SE10.4)	1060	1060	1060					
		1060	1060	1060					
		1060	1060	1060					

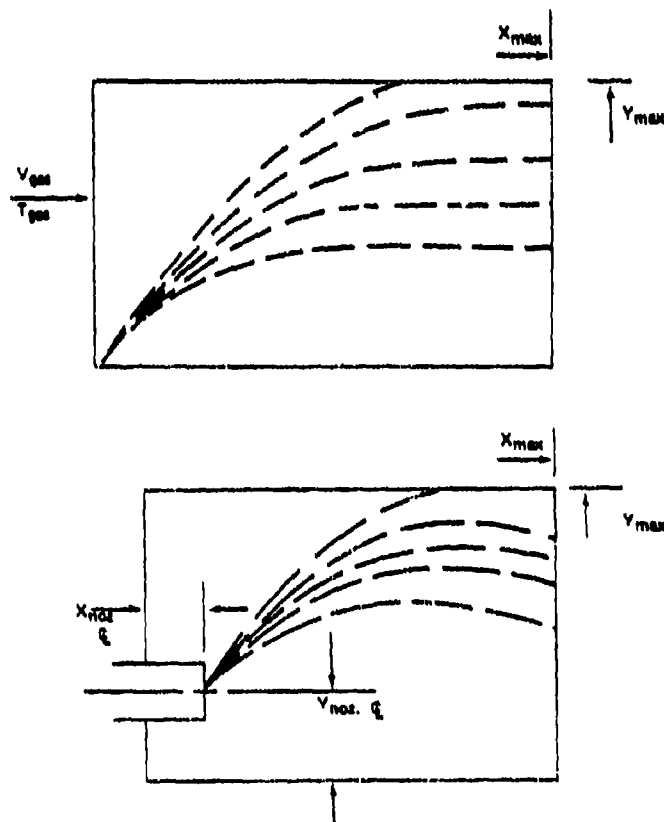


Figure 28. Fuel Insertion Model Input (3 of 3)

nozzle types. The values of Card 7 can have two meanings, depending on the type of flow field. In this case, they give the X and y location of the origin of the spray, the pressure, and limits of the two-dimensional grid. Cards 8 through 13 are required in this example, and it can be seen that only a 3 X 3 grid was used which requires 9 values of U, V, and temperature.

The program output is illustrated in Figures 29 and 30. The first items printed are some of the input quantities, along with the specific gravity and viscosity of the specified fuel. The fuel ΔP and velocity are given next, along with the calculated value of SMD. For each of the five droplets, the locations are then given at the point that selected fractions of the fuel that had evaporated. In this case, droplets 1 and 2 evaporated within the specified boundaries. Figure 30 shows the trajectory output for each of the five droplets. The output consists of a pair of lines, the first giving the X and Y location of the droplet and the second giving the diameter, temperature, velocity, and fraction evaporated.

135

Figure 29. Fuel Insertion Model Output.

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APPENDIX A INPUT SHEETS

ANNULUS LOSS MODEL INPUT SHEET

TITLE - MUST HAVE FOR EACH CASE											ITER	IPIC	IDBUG					
											78	79	80					
1																		
ANNULUS INLET FLOW CARD																		
NELNELI																		
1	3	4	5	6	7	8	11	W1	21	PT1	31	TT1	41	BETA1	51	DP/P	61	71
2	<input checked="" type="checkbox"/>			<input checked="" type="checkbox"/>														
DOME INLET FLOW CARD (REQUIRED FOR INTERNAL LINER FLOW ONLY)																		
NELI																		
12	6	7	8	11	W	21	PT	31	TT	41	BETA	51	61	71				
3	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>																
CONSTANTS CARD																		
1	11FRIC21BLKF31TANS41CDB51SK61RG71IREAX																	
4	<input checked="" type="checkbox"/>																	

- 1 Title - Run ident appears on printed output and plot
- ITER {
 = 1 some (or all) holes fixed, inlet flow fixed, iterate to get pressure drop.
 = 2 some (or all) holes fixed, pressure drop fixed iterate to get inlet flow (input W1 is first guess).
- IPIC {
 = 0 no plot
 = 1 plot drawn
- IDBUG {
 = 0 output printed after converged solution
 = 1 output printed after each iteration } Use only to de-
 = 2 output printed after each element } bugg
 non-convergence
- 2 3 NEL = total number of element stations (card 2 only)
 NELI = element ID no. (NELEM) at annulus or dome inlet 2 and 3
 W₁ and W = air flow at inlet stations, lb/sec
 PT₁ and PT = inlet total pressure, PSIA
 TT₁ and TT = inlet total temperature, R
 Beta₁, Beta = swirl angle at inlet
 DP/P = total pressure drop, PSIA/PSIA (first guess if ITER = 1) card 2 only
- 4 FRIC {
 = 0, smooth wall friction factor
 = -1, no wall friction
 = roughness factor for rough walls
 BLKF = annulus effective area factor (= .83 for fully developed turbine flow)
 TANS = tangent of flow separation spread angle (.1 recommended)

CDB = drag coefficient of struts across annulus (1-1.2 RECM)
SK = ratio of air specific heats,
RG = air gas constant
IREAX } = 0. for reverse flow annular or can combustors
 } = 1. for axial flow annular. First data set is for OD
 panel. Program expects a second set for ID panel

CASE TERMINATION

After last card of case:

- o In Column 1, Column 2 blank - case repeated with changes, next card is title card followed by cards with changes from previous run.
- oo In Columns 1 and 2, next card is EOF to quit or new title card followed by all cards for complete new case.

SELEM									
L		NP	RP	XL	RL	CL	T LINER	BLK 1	DBK 1
L		SP	RP	XL	RL	CL	T LINER	BLK 1	DBK 1
L		SP	RP	XL	RL	CL	T RISE		
F	P	W/W1	N HOLES	NHTYP	CD		I SEP		
F	D	W/W2	N HOLES	NHTYP	CD	D HOLES	I SEP		
F	B	W/W1					I SEP		
F	T	WING W	V JET	ANG 1	ABETA		I SEP		

	1	2	145	11	11	11	41	51	61	71	76
1											
2											
3											
4											
5											
6											
7											
8											
9											
10											
11											
12											
13											
14											
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37											
38											
39											
40											

PROGRAM 117 INPUT DATA SHEET
INPUT FORMAT FOR ELEMENT CARDS - SHEET 1

NELEM					ALL NUMBERS MUST HAVE DECIMAL POINTS									
1	2	3	4	5	11	21	31	41	51	61	71	76		
L	0	0	1		XP	RP	XL	RL	CL	T LINER	BLK I	DBK I		
L	1	0	0	2	XP	RP	XL	RL	CL	T LINER	BLK I	DBK I		
L	C	0	0	3	SP	RP	XL	RL	CL	T RISE	--	--		
F	F	0	0	4	W/WI	N HOLES	NHTYP	CD	--	I SEP	--	--		
F	D	0	0	5	W/WI	N HOLES	NHTYP	CD	D HOLES	I SEP	--	--		
F	B	0	1	0	W/WI	--	--	--	--	I SEP	--	--		
F	I	0	2	0	W/INJ/W	V JET	ANGJ	ABETA	--	I SEP	--	--		

ELEMENT SPECIFICATION

Flow passage is divided into length (L) and flow (F) elements. element numbers, NELEM, can be in arbitrary order, i.e., 10, 1, 3, 4, 16, 30. The cards are stacked in order from inlet to last F because numbers are arbitrary, a new element can be inserted without renumbering other cards.

L. LENGTH ELEMENTS All Dimensions in inches

First L card is annulus inlet (CL = 0) - For both external and internal cases. Internal and external flow cases must be run separately

For internal cases, 2nd card is dome inlet (LI) and LC cards are used with T RISE = AT due to combustion in this element (no L cards)

For external cases use only L Cards

XL, XP = X COORD to end of element L = Liner
RL, RP = Radius to end of element P = Plenum
(For internal flow XP, RP = OD, XL, RL = ID)

CL = Length of element (optional)

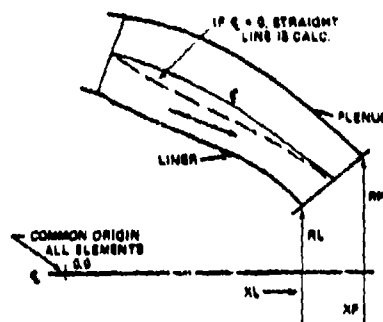
TLIN = Mean wall temp. over CL, °R

If = 0 then TLIN = TTI

BLKI = Frontal Area of Struts

Annulus Area

DBKI = Width of strut



F. ORIFICE FLOW ELEMENT

F Cards are inserted between L cards at points where flow is extracted. Flow conditions into F elem. are those from upstream L elem.

Types: FF = Fixed Flow Ratio, W/WI
FD = Fixed Orf. Diam. (W/WI is First Guess)
FB = Bleed flow (not included in liner flow)
FI = Internal flow elem. (input to these elements is obtained from an external flow solution)

W/WI = Orifice Flow/Inlet Flow

NHOLES = No. of Orifices

NHTYP = Hole Type (For CD)

1. Flush Hole, Thin Wall
2. Plunged Hole
3. Cooling Skirt
4. Flush Hole, Thick Wall
5. CD Input
6. Rectangular Hole

CD = DISCH Coefficient (NHTYP = 5 Only)

DHOLES = Hole Diam. (For FD Only)

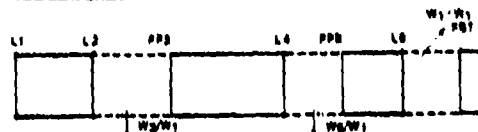
I SEP = 1, Separation is Reattached

VJET = Jet Injection Velocity, FPS

ANGJ = Jet Injection Angle, Deg.

ABETA = Swirl Angle in Annulus Outside FI Elem.

FLOW ELEMENTS



3D COMBUSTOR PERFORMANCE MODEL

22 VARIABLE TITLE CARDS (4A10) SAME ORDER AS IMPRINT

1

--	--	--	--	--	--	--	--

CASE TITLE CARD (8A10)

2

--	--	--	--	--	--	--	--

LP1 MP1 LP1 IPLAX MODEL MODER IPAR ITRAD

3

--	--	--	--	--	--	--	--

IU MODEN INTAPE IDW IRES

4

--	--	--	--	--	--	--	--

ISOLVE (8(12, 8X))

U V W P' KE ϵ D MFU

5

--	--	--	--	--	--	--	--

MCO \bar{R} FX FY FZ

--	--	--	--	--	--	--	--

ICTDMA (8(12, 8X))

U V W P' KE ϵ D MFU

6

--	--	--	--	--	--	--	--

MCO \bar{R}

--	--	--	--	--	--	--	--

IMPRINT (8(12, 8X))

U V W PRESS KE ϵ_m D MFU

7

--	--	--	--	--	--	--	--

TEMP	\bar{h}	Favg	Fx	Fy	Fz	MCO	MH2O

MO2	MCO2	MN2	μ_{EFF}	DENSITY	EVAP

RELAXATION PARAMETERS (8E10.4)

U	V	W	P'	KE	ϵ	\bar{D}	MFU

MCO	\bar{h}	Fx	Fy	Fz	PRESS	DENSITY	VISCOS

LAMINAR PRANDTL NUMBERS (8E10.4)

U	V	W	P'	KE	ϵ	\bar{D}	MFU

MCO	\bar{h}

TURBULENT PRANDTL NUMBERS (8E10.4)

U	V	W	P'	KE	ϵ	\bar{D}	MFU

MCO	\bar{h}

X-COORDINATES (1-LP1) (8E10.4)

--	--	--	--	--	--	--	--

--	--	--	--	--	--	--	--

--	--	--	--	--	--	--	--

12 RI Y-COORDINATES (2-MP1) (8E10.4)

--	--	--	--	--	--	--	--

--	--	--	--	--	--	--	--

--	--	--	--	--	--	--	--

13 Z-COORDINATES (1-NP1) (8E10.4)

--	--	--	--	--	--	--	--

--	--	--	--	--	--	--	--

--	--	--	--	--	--	--	--

14 IWEI JWIO (2(I2,8X))

--	--	--	--	--	--	--	--

15 IWLI VALUES (8(I2,8X)) (SKIP 15 AND 16 IF IWEI = 2)

--	--	--	--	--	--	--	--

--	--	--	--	--	--	--	--

16	JWLO VALUES (8 (12, 8X))							
17	PRESS DEN ABSOR SCATR AKFAC ALFAC (8E10.4)							
18	CX HY HFU FUMCO (8E10.4)							
19	PREXP1 ARCON1 CR1 PREXP2 ARCON2 CR2 (8E10.4)							
20	(8E10.4) C1 C2 CD AMU ERROR TCYLW TINLW TLIP							
21	(2 (13, 7X), 6 (12, 8X)) LASTEP IJUMP JSW1 JSW2 NUINJ NVINJ							
22	USW VSW SWNO AFSW FSW TSW (8E10.4)							
23	NFNZ 1SPRAY TFUEL							
24	XO YO ZO ALFA BETA DELTA THETA 1 THETA 2							
	RSP WF SMD VFUEL (SKIP 24 IF NFNZ = 00)							

(SKIP CARDS 25 → 30 IF NUINJ = 00)

I - LOCATION OF COOLING SLOTS (8(I2, 8X))

25

--	--	--	--	--	--	--	--

J - LOCATION OF COOLING SLOTS (8(I2, 8X))

26

--	--	--	--	--	--	--	--

AXIAL SLOT VELOCITY (8E10.4)

27

--	--	--	--	--	--	--	--

TANG. SLOT VELOCITY (8E10.4)

28

--	--	--	--	--	--	--	--

SLOT FLOW RATE (8E10.4)

29

--	--	--	--	--	--	--	--

SLOT TEMPERATURE (8E10.4)

30

--	--	--	--	--	--	--	--

(SKIP CARDS 31 → 38 IF NVINJ = 00)

I - LOCATION OF RADIAL INJECTION (8(I2, 8X))

31

--	--	--	--	--	--	--	--

J - LOCATION OF RADIAL INJECTION (8(I2, 8X))

32

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K - LOCATION OF RADIAL INJECTION (8(I2, 8X))

33

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INJECTION VELOCITY (8E10.4)

34

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INJECTION TURBULENT KINETIC ENERGY (8E10.4)

35

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INJECTION TURBULENT LENGTH SCALE (8E10.4)

36

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INJECTION FLOW RATE (8E10.4)

37

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INJECTION TEMPERATURE (8E10.4)

38

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3D COMBUSTOR PERFORMANCE MODEL INPUT SHEET DESCRIPTION

Card Set	Description
1	Each card is a heading for a particular three-dimensional array that is printed out. These never change.
2	Case title card
3	<p>LPI - Number of grid nodes in axial (x) dir. MPI - Number of grid nodes in radial (y) dir. NPI - Number of grid nodes in tang. (z) dir. IPLAX - 01 For plane geometry - 02 For axisymmetric geometry MODEL - 01 For laminar viscosity - 02 For K-E viscosity model MODER - 01 For kinetic controlled combustion - 02 For kinetic and turbulence controlled combustion IPAR - 01 For absolute pressure - 02 For relative pressure ITRAD - 01 No radiation - 02 With radiation</p>
4	<p>IU - 01 Input units are international system (i.e., meters, kilograms, degrees kelvin, newtons, joules, radians, seconds or combinations thereof) - 02 User selected input units MODEN - 01 Density is fixed at the value of "Den" on Card 17 - 02 Density calculated from perfect gas law INTAPE - 00 Initial conditions not printed - 08 Initial conditions printed IDW - 00 Inner boundary is axis of symmetry - 01 Inner boundary is wall IRES - 00 This is a new case - 01 This is a restart of previous case</p>
5	An 01 in proper field indicates that this particular variable will be solved for; an 00 indicates that it will not be.
6	Indicates the number of "sweeps" made in the solve routine for each variable.

- 7 An 01 indicates that this variable will be printed,
 an 00 indicates that it will not be.
- 8 Relaxation parameters for each variable.
- 9 Laminar Prandtl numbers for each variable.
- 10 Turbulent Prandtl numbers for each variable.
- 11 X-coordinates (LPI values)
- 12 RI - Radius of inner boundary
 Y-coordinates as measured from inner
 boundary (MPI-1) values. Since Y(1) is
 always 00, RI is read in its place.
- 13 Z - coordinates (NPI values)
- 14 IWEI - I-node at which inclined wall ends
 JWIO - J-node at which inclined wall starts
- 15 IWLI - Starting I-nodes of the calculation domain
 when inclined wall is present
- 16 JWLO - Ending J-nodes of the calculation domain
 when inclined wall is present
- 17 PRESS - System pressure
 DEN - The value of density if option MODEN = 01
 is selected
 ABSOR - Absorption coefficient in radiation model
 SCATR - Scattering coefficient in radiation model
 AKFAC - Internally defined turbulent kinetic
 energies are AKFAC times the appropriate
 velocity squared
 ALFAC - Internally defined turbulent length scales
 are ALFAC times the appropriate distance
- 18 CX - Carbon atoms in fuel molecule
 HY - Hydrogen atoms in fuel molecule
 HFU - Heat of formation of fuel
 FUMCO - Initial value assigned to M_{CO}
- 19 PREXPI - Preexponent of 1st reaction
 ARCONI - Activation energy divided by gas constant
 of 1st reaction (E/R)
 CR1 - Constant in turbulence controlled reaction
 rate for 1st reaction
 PREXP2 - Preexponent of 2nd reaction

- ARCON2 - Activation energy divided by gas constant of 2nd reaction (E/R)
- CR2 - Constant in turbulence controlled reaction rate for 2nd reaction

- 20 C1 - Turbulence model constant
- C2 - Turbulence model constant
- CD - Turbulence model constant
- AMU - The value of the viscosity if option model = 01 is specified. Also the laminar viscosity used in the "wall functions"
- ERROR - Program will terminate if total error in mass becomes less than this value
- TCYLW - Temperature of cylindrical portion of combustor wall
- TINLW - Temperature of inclined wall portion of combustor and of dome.
- TLIP - Temperature of cooling slot lip.

- 21 LASTEP - Maximum number of iterations
- IJUMP - Number of iterations between array printout
- JSW1 - J-node at start of dome inlet
- JSW2 - J-node at end of dome inlet
- NUINJ - Number of axial injection points (cooling slots)
- NUINJ - Number of radial injection points

- 22 USW - Axial velocity of dome inlet
- VSW - Radial velocity of dome inlet
- SWNO - Ratio of tangential to axial velocity at dome inlet
- AFSW - Flow rate of fuel and air through dome inlet
- FSW - Flow rate of fuel through dome inlet
- TSW - Temperature at dome inlet

- 23 NFNZ - 00 No liquid fuel nozzle
- 01 Liquid fuel nozzle present
- ISPRAY - Droplet evaporation routine is called every ISPRAY iterations
- TFUEL - Initial temperature of liquid fuel

- 24 XO - X-location of origin of fuel nozzle spray
- YO - Y-location of origin of fuel nozzle spray
- ZO - Z-location of origin of fuel nozzle spray
- ALFA - Nozzle cone angle
- BETA - Nozzle back angle
- DELTA - Nozzle down angle
- THETA1 - Initial spray cone segment angle
- THETA2 - Final spray cone segment angle

RSP - Number of spray cone rays
WF - Fuel flow rate
SMD - Sauter mean diameter
VFUEL - Initial fuel droplet velocity

- 25 I node location of cooling slots
- 26 J node location of cooling slots
- 27 Cooling slot axial velocity
- 28 Cooling slot tangential velocity
- 29 Cooling slot mass flow rate
- 30 Cooling slot temperature
- 31 I node location of radial injection
- 32 J node location of radial injection
- 33 K node location of radial injection
- 34 Radial injection velocity
- 35 Radial injection turbulent kinetic energy
- 36 Radial injection turbulence length scale
- 37 Radial injection mass flow rate
- 38 Radial Injection temperature

LINER COOLING MODEL INPUT SHEET

1 CASE TITLE (12A6)

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CASE TITLE (12A6)

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(8 (12, 8X))

2 N KRAD MASSTR ISWRL MODEL INERT IFLUX ITEMP

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3 NSTAT NPROF NPLOT ITEST LASTEP (5 (15.5X))

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4 XU XULAST FRA XEND XOUT PRESS POWER (8E10.4)

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5 NBP (12)

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6 (8E10.4)

X ₁	RI ₁	RE ₁	X ₂	RI ₂	RE ₂	X ₃	RI ₃

RE₃ X₄ RI₄ RE₄ X₅ RI₅ RE_{5...} (8E10.4)

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7 RA RB RD (8E10.4)

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NAME LIST

8 \$INPUT

							\$
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9

UA	UD						
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 (8E10.4)

10

F2A	F2D	TA	TD	T _{wall}			
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 (8E10.4)

11

NIN							
-----	--	--	--	--	--	--	--

 (I2)

12

Y VALUES							
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 (8E10.4)

13

U VALUES							
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 (8E10.4)

14

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 (8E10.4)

15

TEMPERATURE VALUES							
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 (8E10.4)

16

MFU VALUES							
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 (8E10.4)

17

PHI VALUES							
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 (8E10.4)

18 MCO VALUES (8E10.4)

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19 TURBULENT KINETIC ENERGY (8E10.4)

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20 TURBULENCE LENGTH SCALE (8E10.4)

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21 VELA_I VELA_O TAN_I TAN_O PR_I PR_O (8E10.4)

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22 NFNZ XDP YDP UF VF SMD WF TFUEL (12, 8X, 7E10.4)

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LINER COOLING MODEL INPUT SHEET DESCRIPTION

Card Set	Description
1	Case title cards
2	<p>N - Number of cross stream intervals</p> <p>KRAD - 00 For plane geometry 01 For axisymmetric geometry</p> <p>MASSTR - 00 Species equations not solved 01 Species equations solved</p> <p>ISWRL - 00 Always</p> <p>MODEL - 01 Laminar viscosity 02 Two-equation K-E viscosity model</p> <p>INERT - 01 Species are inert 02 Species will react</p> <p>IFLUX - 00 Wall adiabatic 01 Wall temperature calculated</p> <p>ITEMP - 00 Isothermal 01 Enthalpy solved</p>
3	<p>NSTAT - Number of steps between printout of output variables</p> <p>NPROF - Number of steps between printout of output variables and profiles</p> <p>NPLOT - Number of steps between line-printer plots</p> <p>ITEST - 00 No extra printout 01 Extra printout</p> <p>LASTEP - Maximum number of marching steps</p>
4	<p>XU - Initial X-location</p> <p>XULAST - Final X-location</p> <p>FRA - Fraction of grid height to be used as step size</p> <p>XEND - X-location of end of inner wall</p> <p>XOUT - X-location of end of outer wall</p> <p>PRESS - Pressure</p> <p>POWER - Control for node spacing</p>
5	NBP - Number of boundary pairs
6	<p>X_1 - X-Location at which boundary is specified</p> <p>RI_1 - Inner boundary radius</p> <p>RE_1 - Outer boundary radius</p>
7	<p>RA - Radius of axis of symmetry</p> <p>RB - Inner boundary radius at initial X-location</p> <p>RD - Outer boundary radius at initial X-location</p>

- 8 Namelist, see page 158 for variables
- 9 UA - Axial velocity at "free" inner boundary
 UD - Axial velocity at "free" outer boundary
- 10 F2A - Fuel mass fraction at "free" inner boundary
 F2D - Fuel mass fraction at "free" outer boundary
 TA - Temperature at "free" inner boundary
 TD - Temperature at "free" outer boundary
 TWALL - Wall temperature
- 11 NIN - Number of points on input initial profile
- 12 Y-values of input initial profile (NIN values)
- 13 U-values of input initial profile
- 14 Blank card(s)
- 15 Temperature values of input initial profile
- 16 MFU values of input initial profile
- 17 Total fuel values of input initial profile
- 18 M_{CO} values of input initial profile
- 19 KE values of input initial profile
 (Read only if KREAD = 1)
- 20 /m Values of input initial profile
 (Read only if KREAD = 1)
- 21 VELA_I - Inner annulus velocity
 VELA_O - Outer annulus velocity
 TAN_I - Inner annulus temperature
 TAN_O - Outer annulus temperature
 PR_I - Radius of inner plenum
 PR_O - Radius of outer plenum
- 22 NFNZ - 00 No fuel nozzle
 01 Fuel nozzle present
 XDP - X-location of fuel nozzle
 YDP - Y-location of fuel nozzle
 UF - Axial velocity of fuel droplets
 VF - Radial velocity of fuel droplets
 SMD - Sauter mean diameter
 WF - Fuel mass flow rate
 TFUEL - Fuel temperature

LINER COOLING MODEL
NAMELIST INPUT

VBL	Value	Description
IUTRAP	2	Test for negative U's, see STRIDE(2)
ULIM	0.05	Entrainment control
PEILIM	0.01	Max. fractional mass flow change per step
AFAC	0.2	Relaxation on duct area deviation
AEXDLM	0.02	Max. duct area fractional deviation per step
NOVEL	2	01-U not solved for, 02-solve for U
ARCON1	28500	Activation energy divided by gas constant for fuel reaction
PREXP1	5E + 15	Preexponent for fuel reaction
CR1	6.0	Eddy breakup constant for fuel reaction
ARCON2	12500	Activation energy divided by gas constant for CO reaction
PREXP2	6E + 8	Preexponent for CO reaction
CR2	4.0	Eddy breakup constant for CO reaction
CP	1048	Specific heat
IPDDX	1	01 - Std genmix pressure grad. calculation 02 - "Grid filling duct" version
C1	1.42	Turb. Constant
C2	1.92	Turb. Constant
CD	0.09	Turb. Constant
C2VT	0.36	Turb. Constant
AKFAC	0.03	Factor for internally generated kinetic energy profiles, $KE = AKFAC * U^2$
ALFAC	0.02	Factor for internally generated length scale profiles, $l_m = ALFAC * \Delta Y$
PREF	--	Turbulent Prandtl numbers
CX	1.0	Molecular carbon value of fuel
HY	4.0	Molecular hydrogen value of fuel
HFU	-49317	Heat of formation of fuel
MODER	2	1 - Kinetic only, 02 - Kinetic + Diffusion
ITHIN	1	Thin output profiles by printing every ITHIN value
KREAD	0	0 - K & E profiles generated internally 1 - K & l_m read in
URAT	0.83	Cooling slot velocity shape factor
ABSOR	0.1	Absorption coefficient in radiation model
EMISW	0.8	Emissivity of liner wall

TRANSITION MIXING MODEL INPUT SHEET

CASE TITLE CARD (12A6)

1							
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CASE TITLE CARD (12A6)

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(8 (12, 8X))

N KRAD MASSTR ISWRL MODEL INERT IFLUX ITEMp

2							
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NSTAT NPROF NPLOT ITEST LASTEP

(5 (15, 5X))

3							
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(8E10.4)

ZUI ZUE ZULAST FRA ZEND ZOUT PRESS POWER

4							
---	--	--	--	--	--	--	--

NBP ICURV NRCVI NRCVE

(8 (12, 8X))

5							
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(8E10.4)

RI₁ XI₁ RI₂ XI₂ RI₃ XI₃ RI₄ XI₄...

6							
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(8E10.4)

RE₁ XE₁ RE₂ XE₂ RE₃ XE₃ RE₄ XE₄...

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(8E10.4)

ZI₁ RCVI₁ ZI₂ RCVI₂ ZI₃ RCVI₃ ZI₄ RCVI₄...

7							
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								(8E10.4)
	ZE ₁	RCVE ₁	ZE ₂	RCVE ₂	ZE ₃	RCVE ₃	ZE ₄	RCVE ₄ ...
8	RA	RB	RD					(8E10.4)
9	NAMELIST							
	\$INPUT							\$
10	UA	UD						(8E10.4)
11	F2A	F2D	TA	TD	T _{wall}			(8E10.4)
12	NIN							(I2)
13	Y VALUES							(8E10.4)
14	U VALUES							(8E10.4)
15								
16	TEMPERATURE VALUES							(8E10.4)

17

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18

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19

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20

TURBULENT KINETIC ENERGY				(8E10.4)			

21

TURBULENCE LENGTH SCALE				(8E10.4)			

TRANSITION MIXING MODEL
INPUT SHEET DESCRIPTION

Card Set	Description
1	Case title cards
2	N - Number of cross stream intervals KRAD - 00 For plane geometry 01 For axisymmetric geometry MASSTR - 00 Always ISWRL - 00 Always MODEL - 01 Laminar viscosity 02 Two-equation K-E viscosity model INERT - 01 Always IFLUX - 00 Walls are adiabatic 01 Wall temperature is specified ITEMP - 00 Isothermal 01 Enthalpy solved
3	TAT - Number of steps between printout of output variables NPROF - Number of steps between printout of output variables and profiles NPLOT - Number of steps between line-printer plots ITEST - 00 No extra printout 01 Extra printout LASTEP - Maximum number of marching steps
4	ZUI - Initial Z-location on inner boundary ZUE - Initial Z-location on outer boundary ZULAST - Final Z location FRA - Fraction of grid height to be used as step size ZEND - Z-location of end of inner wall ZOUT - Z-location of end of outer wall PRESS - Pressure POWER - Control for node spacing
5	NBP - Number of boundary pairs ICURV - 00 No radius of curvature effects 01 Radius of curvature effects NRCVI - Number of radius of curvature points specified on inner boundary NRCVE - Number of radius of curvature points specified on outer boundary
6	RI ₁ - Inner boundary radius XI ₁ - Inner boundary X-location RE ₁ - Outer boundary radius XE ₁ - Outer boundary X-location

- 7 ZI_i - Z-location on inner boundary at which
 radius of curvature is specified
 $RCVI_i$ - Radius of curvature of inner boundary
 ZE_i - Z-location on outer boundary at which
 radius of curvature is specified
 $RCVE_i$ - Radius of curvature of outer boundary
- 8 RA - Radius of axis of symmetry
 RB - Inner boundary radius at initial Z-location
 RD - Outer boundary radius at initial Z-location
- 9 Namelist, see page 164 for variables
- 10 UA - Axial velocity at "free" inner boundary
 UD - Axial velocity at "free" outer boundary
- 11 F2A - Fuel mass fraction at "free" inner boundary
 F2D - Fuel mass fraction at "free" outer boundary
 TA - Temperature at "free" inner boundary
 TD - Temperature at "free" outer boundary
 TWALL - Wall temperature
- 12 NIN - Number of points on input initial profile
- 13 Y values of input initial profile (NIN values)
- 14 U values of input initial profile
- 15 Blank card(s)
- 16 Temperature values of input initial profile
- 17 Blank card(s)
- 18 Blank card(s)
- 19 Blank card(s)
- 20 RE values of input initial profile
 (Read only if KREAD = 1)
- 21 μ m values of input initial profile
 (Read only if KREAD = 1)

TRANSITION MIXING MODEL
NAMELIST INPUT

VBL	Value	Description
IUTRAP	2	Test for negative U's, see STRIDE(2)
ULIM	0.05	Entrainment control
PEILIM	0.01	Max. fractional mass flow change per step
AFAC	0.2	Relaxation on duct area deviation
AEXDLM	0.02	Max. duct area fractional deviation per step
NOVEL	2	01 - U not solved for, 02 - solve for U
ARCON1	28500	Activation energy divided by gas constant for fuel reaction
PREXP1	5E + 15	Preexponent for fuel reaction
CR1	6.0	Eddy break-up constant for fuel reaction
ARCON2	12500	Activation energy divided by gas constant for CO reaction
PREXP2	6E + 8	Preexponent for CO reaction
CR2	6.0	Eddy break-up constant for CO reaction
CP	1255	Specific heat
IDPDX	01	01 - Std genmix pressure grad. calculation 02 - "grid filling duct" version
C1	1.42	Turb. Constant
C2	1.92	Turb. Constant
CD	0.09	Turb. Constant
C2VT	0.36	Turb. Constant
AKFAC	0.03	Factor for internally generated turb. kinetic energy profiles, $KE = AKFAC * U^2$
ALFAC	0.02	Factor for internally generated length scale profiles, $l_m = ALFAC * \Delta Y$
PREF	--	Turbulent Prandtl numbers
CX	1.0	Molecular carbon value of fuel
HY	4.0	Molecular hydrogen value of fuel
HFU	4E + 7	Heat of combustion of fuel
MODER	2	01 - Kinetic only, 02 - Kinetic + Diffusion
ITHIN	1	Thins output profiles by printing every ITHIN value
KREAD	0	00 - KE & l_m profiles generated internally 01 - KE & l_m read in

EMISSIONS MODEL INPUT SHEET

CASE TITLE CARD (12A6)

1							
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CASE TITLE CARD (12A6)

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(8 (I2, 8X))

2	N	KRAD	MASSTR	ISWRL	MODEL	INERT	IFLUX	ITEMP

NSTAT NPROF NPLOT ITEST LASTEP (5 (I5, 5X))

3							
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XU XULAST FRA XEND XOUT PRESS POWER (8E10.4)

4							
---	--	--	--	--	--	--	--

NBP (I2)

5							
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X₁ RI₁ RE₁ X₂ RI₂ RE₂ X₃ RI₃

6							
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RE₃ X₄ RI₄ RE₄ X₅ RI₅ RE ... (8E10.4)

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RA RB RD (8E10.4)

7							
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NAMELIST							
8	\$INPUT						\$
9	UA	UD	VTa	VTd			(8E10.4)
10	F2A	F2D	TA	TD	T _{wall}		(8E10.4)
11	NIN	NUI	NUE	NVI	NVE		(5 (12, 8X))
12	Y VALUES						(8E10.4)
13	U VALUES						(8E10.4)
14	V ₀ VALUES						(8E10.4)
15	TEMPERATURE VALUES						(8E10.4)
16	MFU VALUES						(8E10.4)
17	MCO ₂ VALUES						(8E10.4)

18 MCO VALUES (8E10.4)

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19 MOX VALUES (8E10.4)

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20 MH_2O VALUES (8E10.4)

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21 MH_2 VALUES (8E10.4)

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22 TURBULENT KINETIC ENERGY (8E10.4)

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23 TURBULENCE LENGTH SCALE (8E10.4)

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—— SKIP FOLLOWING CARD SET IF NUI = 0 ——

24 X - LOC. OF INTERNAL COOLING SLOTS (8E10.4)

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25 LIP LENGTH OF INTERNAL COOLING SLOTS (8E10.4)

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26 U - VELOCITY OF INTERNAL COOLING SLOTS (8E10.4)

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27 VT - VELOCITY OF INTERNAL COOLING SLOTS (8E10.4)

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TEMPERATURE OF INTERNAL COOLING SLOTS (8E10.4)

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FLOW RATE OF INTERNAL COOLING SLOTS (8E10.4)

29

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SLOT HEIGHT OF INTERNAL COOLING SLOTS (8E10.4)

30

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SLOT TO METERING AREA RATIO FOR INT SLOTS (8E10.4)

31

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SKIP FOLLOWING CARD SET IF NUE = 0

X-LOC OF EXTERNAL COOLING SLOTS (8E10.4)

32

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LIP LENGTH OF EXTERNAL COOLING SLOTS (8E10.4)

33

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U - VELOCITY OF EXTERNAL COOLING SLOTS (8E10.4)

34

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V_T - VELOCITY OF EXTERNAL COOLING SLOTS (8E10.4)

35

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TEMPERATURE OF EXTERNAL COOLING SLOTS (8E10.4)
36

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FLOW RATE OF EXTERNAL COOLING SLOTS (8E10.4)
37

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SLOT HEIGHT OF EXTERNAL COOLING SLOTS (8E10.4)
38

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SLOT TO METERING AREA RATIO FOR EXT SLOTS (8E10.4)
39

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SKIP FOLLOWING CARD SET IF NVI = 0

X - LOC OF INTERNAL RADIAL INJECTION (8E10.4)
40

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U - VELOCITY OF INTERNAL RADIAL INJECTION (8E10.4)
41

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V - VELOCITY OF INTERNAL RADIAL INJECTION (8E10.4)
42

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VT - VELOCITY OF INTERNAL RADIAL INJECTION (8E10.4)
43

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TEMPERATURE OF INTERNAL RADIAL INJECTION (8E10.4)

44

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FLOW RATE OF INTERNAL RADIAL INJECTION (8E10.4)

45

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SKIP FOLLOWING CARD SET IF NVE = 0

X - LOC. OF EXTERNAL RADIAL INJECTION (8E10.4)

46

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U - VELOCITY OF EXTERNAL RADIAL INJECTION (8E10.4)

47

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V - VELOCITY OF EXTERNAL RADIAL INJECTION (8E10.4)

48

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VT - VELOCITY OF EXTERNAL RADIAL INJECTION (8E10.4)

49

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TEMPERATURE OF EXTERNAL RADIAL INJECTION (8E10.4)

50

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FLOW RATE OF EXTERNAL RADIAL INJECTION (8E10.4)

51

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EMISSIONS MODEL
INPUT SHEET DESCRIPTION

Card Set	Description
1	Case title cards
2	<p>N - Number of cross stream intervals</p> <p>KRAD - 00 For plane geometry 01 For axisymmetric geometry</p> <p>MASSTR - 00 Species equations not solved 01 Species equations solved</p> <p>ISWRL - 00 Swirl velocity not solved 01 Swirl velocity solved</p> <p>MODEL - 01 Laminar viscosity 02 Two-equation, K-E, viscosity model</p> <p>INERT - 01 Species are inert 02 Species will react</p> <p>IFLUX - 00 Wall adiabatic 01 Wall temperature specified</p> <p>ITEMP - 00 Isothermal 01 Enthalpy solved</p>
3	<p>NSTAT - Number of steps between printout of output variables</p> <p>NPROF - Number of steps between printout of output variables and profiles</p> <p>NPLOT - Number of steps between line printer plots</p> <p>ITEST - 00 No extra printout 01 Extra printout</p> <p>LASTEP - Maximum number of marching steps</p>
4	<p>XU - Initial X location</p> <p>XULAST - Final X location</p> <p>FRA - Fraction of grid height to be used as step size</p> <p>XEND - X location of end of inner wall</p> <p>XOUT - X location of end of outer wall</p> <p>PRESS - Pressure</p> <p>POWER - Control for node spacing</p>
5	NBP - Number of boundary pairs
6	<p>X_i - X location at which boundary is specified</p> <p>R_i_i - Inner boundary radius</p> <p>R_e_i - Outer boundary radius</p>
7	<p>RA - Radius of axis of symmetry</p> <p>RB - Inner boundary radius at initial X-location</p> <p>RD - Outer boundary radius at initial X-location</p>

- 8 Namelist, see page 174 for variables
- 9 UA - Axial velocity at "free" inner boundary
 UD - Axial velocity at "free" outer boundary
 VTA - Tang. velocity at "free" inner boundary
 VTD - Tang. velocity at "free" outer boundary
- 10 F2A - Fuel mass fraction at "free" inner boundary
 F2D - Fuel mass fraction at "free" outer boundary
 TA - Temperature at "free" inner boundary
 TD - Temperature at "free" outer boundary
 TWALL - Wall temperature
- 11 NIN - Number of points on the input initial
 profile
 NUI - Number of cooling slots on inner boundary
 NUE - Number of cooling slots on outer boundary
 NVI - Number of radial injection points on
 inner boundary
 NVE - Number of radial injection points on
 outer boundary
- 12 Y values of input initial profile (NIN values)
- 13 U values of input initial profile
- 14 V_θ values of input initial profile
- 15 Temperature values of input initial profile
- 16 M_{F_u} values of input initial profile
- 17 M_{CO_2} values of input initial profile
- 18 M_{CO} values of input initial profile
- 19 M_{Ox} values of input initial profile
- 20 M_{H_2O} values of input initial profile
- 21 M_{H_2} values of input initial profile
- 22 KE values of input initial profile
 (Read only if KREAD = 1)
- 23 μ values of input initial profile
 (Read only if KREAD = 1)
- 24 to 31 Information pertaining to cooling slots on inner
 boundary

- 32 to 39 Information pertaining to cooling slots on outer boundary
- 40 to 45 Information pertaining to radial injections on inner boundary
- 46 to 51 Information pertaining to radial injections on outer boundary

EMISSIONS MODEL
NAMELIST INPUT

VBL	Value	Description
IUTRAP	2	Test for negative U's, see STRIDE(2)
ULIM	0.05	Entrainment control
PEILIM	0.01	Max. fractional mass flow change per step
AFAC	0.2	Relaxation on duct area deviation
AEXDLM	0.02	Max. duct area fractional deviation per step
NOVEL	2	01 - U not solved for, 02 - Solve for U
ARCON1	28500	Activation energy for fuel reaction
PREXP1	5E + 15	Preexponent for fuel reaction
CR1	6.0	Eddy breakup constant for fuel reaction
CP	1048	Specific heat
IPDDX	1	01 - Std genmix pressure grad. calculation 02 - "grid filling duct" version
C1	1.42	Turb. Constant
C2	1.92	Turb. Constant
CD	0.09	Turb. Constant
C2VT	0.36	Turb. Constant
AKFAC	0.03	Factor for internally generated kinetic energy profiles, $KE = AKFAC * U$
ALFAC	0.02	Factor for internally generated length scale profiles, $l_m = ALFAC * \Delta Y$
PREF	--	Turbulent Prandtl numbers
CX	1.0	Molecular carbon value of fuel
HY	4.0	Molecular hydrogen value of fuel
HFU	-49317	Heat of formation of fuel
MODER	2	1 - Kinetic only, 02 - Kinetic + Diffusion
ITHIN	1	Thins output profiles by printing every ITHIN value
KREAD	0	0 - K & E profiles generated internally 1 - K & l_m read in
URAT	0.83	Cooling slot velocity shape factor
TERM1	0.1	Control on specie equation step size
TERM2	1.E-4	Control on specie equation step size
ISMAX	500	Maximum specie equation steps
EFU	1.0	Power on fuel in fuel reaction rate
E _{O2}	0.5	Power on O ₂ in fuel reaction rate
E _{H2O}	0.5	Power on H ₂ O in fuel reaction rate
ERO	2.0	Power on density in fuel reaction rate
EPR	0.0	Power on pressure in fuel reaction rate

FUEL INSERTION MODEL INPUT

1	TITLE										80
		PRIM	SEC.		AIR						
*	**	FLOW	FLOW	CONE	SHROUD	PRIM	SEC				
ATOM	AIR	NO.	NO.	ANGLE	EFF	ORIFICE	ORIFICE				
TYPE	ASSIST	(JP4)	(JP4)	DEG	AREA	DIA,	DIA,				
		PPH/ $\sqrt{\text{PSI}}$			IN ²	IN	IN				
1	→ 6	→ 11	21	31	41	51	61	71	80		
2											
<p>*ATOMIZER TYPE: 00001 = SIMPLEX 00002 = DUAL ORF 00003 = AIR BLAST</p> <p>**AIR ASSIST: 00001 = NO ASSIST 00002 = WITH ASSIST</p> <p>*FOR ATOM TYPE = 00002 (DUAL ORIF) ONLY (LEAVE OUT FOR OTHERS) INPUT SECONDARY FLOW SCHEDULE W_S = SECONDARY FUEL FLOW, LB/HR ΔP_S = $\Delta P_{\text{SEC. ORIF}}$ + $\Delta P_{\text{FLOW DIVIDER VALVE}}$ P/D</p>											
<p>CRACK POINT FLOW</p> <p>W_{S1} W_{S2} W_{S3} W_{S4} W_{S5}</p>											
1	11	21	31	41	51						
3											
<p>CRACK PRESSURE</p> <p>ΔP_1 ΔP_2 ΔP_3 ΔP_4 ΔP_5</p>											
1	11	21	31	41	51						
4											
<p>*FOR ATOM TYPE = 00003 (AIRBLAST) ONLY (LEAVE OUT FOR OTHERS)</p> <p>FILMING NOZZLE FLOW AIR DIA AIRFLOW AREA TEMP IN. LB/SEC IN² °R</p>											
1	11	21	31								
5											

 *** AIR FUEL FUEL FUEL AIR AIR
 FUEL FLOW TEMP FLOW ΔP ASSIST ASSIST
 TYPE OPTION °R LB/HR PSI PSI °R
 1 → 6 → 11 21 31 41 51 61 71
 6

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 FUEL 0.00002=JP5 **AIR } 0.00001=UNIFORM GAS STREAM
 TYPE 0.00004=JP4 FLOW } 0.00002=2-D FIELD OPTION
 OPTION

T_{GAS}, °R V_{GAS}, P_{GAS}, X_{MAX}, Y_{MAX}, ← UNIFORM STREAM
 1 11 FPS 21 PSIA 31 IN. 4 °R 51 OPTION
 7

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 ↑ ↑ ↑ ↑ ↑ ← Z-D FIELD OPTION
 X_{NOZ} IN. Y_{NOZ} IN. P_{GAS} PSIA X_{MAX} IN. Y_{MAX} IN.

CARDS 8 THROUGH 13 SKIPPED IF AIR FLOW OPTION = 00001

IN = NO. OF X-DIR POINTS IN 2-D FIELD
 JN = NO. OF Y-DIR POINTS
 IN JN (2(I2, 8X))
 8

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X VALUES (8E10.4) X - LOCATIONS OF GRID POINTS (FT)
 9

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Y VALUES (8E10.4) Y - LOCATIONS OF GRID POINTS (FT)
 10

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READ ALONG + X LINES STARTING WITH
 U VALUES (8E10.4) SMALLEST Y VALUE (FT/SEC)
 11

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V VALUES (8E10.4) READ ALONG + X LINES STARTING WITH
SMALLEST Y VALUE (FT/SEC)

12

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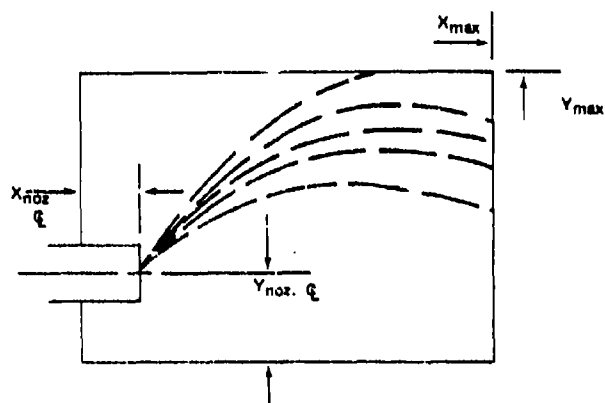
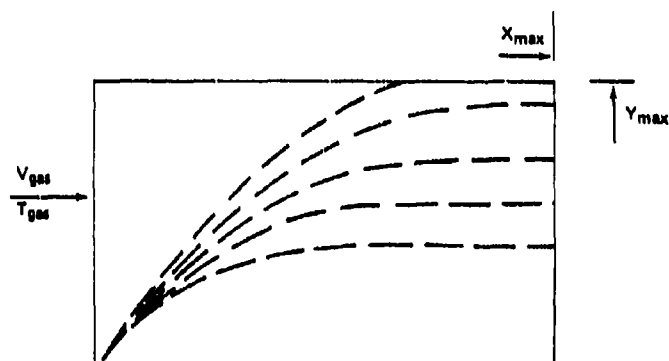
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T VALUES (8E10.4) READ ALONG + X LINES STARTING WITH
SMALLEST Y VALUE (DEG. R)

13

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[illegible]

[illegible]

CARD NO. SEVERITY DETAILS SYMPTOMS OF DISEASE

[illegible]

186


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1 SUBROUTINE FLOW (L)
2 CALL FLOW (L)
3 IF (L) GO TO 10
4 CALL FLOW (L)
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99 CALL FLOW (L)
100 CALL FLOW (L)

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FTM 4-60439

09.38.39
09/26/78

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0-276
OPT-0 TRACE

13F 3M1108085

[illegible]

SEQUENCE	ARM	73/74	DATA-3 TRACE	FTN 4.00030	08/24/70	00.55.30	PAGE
1			SUBROUTINE ARMIDAA,DTT,DF,DD,YS,SE,EM1,EM2				1
5			ARMIDAA,DTT,DF,DD,YS,SE,EM1,EM2				
10			ARMIDAA,DTT,DF,DD,YS,SE,EM1,EM2				
15			ARMIDAA,DTT,DF,DD,YS,SE,EM1,EM2				
20			ARMIDAA,DTT,DF,DD,YS,SE,EM1,EM2				

200

204

00/24/78 14-08-46

FTN 4-0-439

50000TIME INITIAL 73/74 OPT-0 TRACE

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155 1 (1)-A(102)*MNR(TSN,12)
156 1 (1)-A(102)*MNR(TSN,12)
157 1 (1)-A(102)*MNR(TSN,12)
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230 1 (1)-A(102)*MNR(TSN,12)
231 1 (1)-A(102)*MNR(TSN,12)

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215

216

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390      FILL(NVK)=K
      DY=JULI(4)-Y(JJ)
      IF (JULI(4)-Y(JJ)) 1, 2, 3
      1 AL=AL+1
      2 AL=AL+1
      3 AL=AL+1
      418      DO 775 J=JW1,JSW2,5/(AL+1.E-30)
      775      IF (JW1-JSW2) 1, 2, 3
      1 IF (JW1-JSW2) 1, 2, 3
      2 IF (JW1-JSW2) 1, 2, 3
      3 IF (JW1-JSW2) 1, 2, 3
      400      FILL(NVK)=K
      405      FILL(NVK)=K
      410      FILL(NVK)=K
      415      FILL(NVK)=K
      420      FILL(NVK)=K
      425      FILL(NVK)=K
      430      FILL(NVK)=K
      435      FILL(NVK)=K
      440      FILL(NVK)=K
      445      FILL(NVK)=K
      450      FILL(NVK)=K
      455      FILL(NVK)=K
      460      FILL(NVK)=K

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218

223

227

00/20/70 10.00.46

FTM 4.0-039

SUBROUTINE ALLMOD 73/74 OPT=0 TRACE

IF (JUTMJJ(1)-ME.JPLANE) GO TO 1102

1C=JUTMJJ(1)-A

1104 1102

SUTL=0.0

1104 1102

SPLT=ME-L.E30

1104 1102

CONTINUE

1104 1102

1104 1102

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695

700

705

710

921

END

DIAGNOSIS OF PROBLEM

CARD NO. SEVERITY DETAILS

70 1
103 1
121 1
196 1

CONTROL VARIABLE IN COMMON OR EQUIVALENT OPTIMIZATION MAY BE INITIATED.
CONTROL VARIABLE IN COMMON OR EQUIVALENT OPTIMIZATION MAY BE INITIATED.
CONTROL VARIABLE IN COMMON OR EQUIVALENT OPTIMIZATION MAY BE INITIATED.
CONTROL VARIABLE IN COMMON OR EQUIVALENT OPTIMIZATION MAY BE INITIATED.
CONTROL VARIABLE IN COMMON OR EQUIVALENT OPTIMIZATION MAY BE INITIATED.

AL 1101
AL 1102
AL 1103
AL 1104
AL 1105
AL 1106
AL 1107
AL 1108
AL 1109
AL 1110
AL 1111
AL 1112
AL 1113
AL 1114
AL 1115
AL 1116
AL 1117
AL 1118
AL 1119


```

155 DO 2000 K=1,NP1
156   DO 2000 J=2,N
157     LPM=LMX(J)+JML(J)
158     IF (LPM.LT.0) LPM=0
159     IF (LPM.GT.15) IE=1
160     LPM=LPM+IE
161     GO TO 2001,2002,MODEL
162 2001 CONTINUE
163   LPM=LPM+1
164   GO TO 2000
165 2002 CONTINUE
166   LPM=LPM+1
167   IF (LPM.EQ.1) LPM=0
168   IF (LPM.EQ.15) IE=1
169   LPM=LPM+IE
170   GO TO 2000,2001,MODEL
171 2003 CONTINUE
172   LPM=LPM+1
173   IF (LPM.EQ.1) LPM=0
174   IF (LPM.EQ.15) IE=1
175   LPM=LPM+IE
176   GO TO 2000,2001,MODEL
177 2004 CONTINUE
178   LPM=LPM+1
179   IF (LPM.EQ.1) LPM=0
180   IF (LPM.EQ.15) IE=1
181   LPM=LPM+IE
182   GO TO 2000,2001,MODEL
183 2005 CONTINUE
184   LPM=LPM+1
185   IF (LPM.EQ.1) LPM=0
186   IF (LPM.EQ.15) IE=1
187   LPM=LPM+IE
188   GO TO 2000,2001,MODEL
189 2006 CONTINUE
190   LPM=LPM+1
191   IF (LPM.EQ.1) LPM=0
192   IF (LPM.EQ.15) IE=1
193   LPM=LPM+IE
194   GO TO 2000,2001,MODEL
195 2007 CONTINUE
196   LPM=LPM+1
197   IF (LPM.EQ.1) LPM=0
198   IF (LPM.EQ.15) IE=1
199   LPM=LPM+IE
200   GO TO 2000,2001,MODEL
201 2008 CONTINUE
202   LPM=LPM+1
203   IF (LPM.EQ.1) LPM=0
204   IF (LPM.EQ.15) IE=1
205   LPM=LPM+IE
206   GO TO 2000,2001,MODEL
207 2009 CONTINUE
208   LPM=LPM+1
209   IF (LPM.EQ.1) LPM=0
210   IF (LPM.EQ.15) IE=1
211   LPM=LPM+IE
212   GO TO 2000,2001,MODEL
213 2010 CONTINUE
214   LPM=LPM+1
215   IF (LPM.EQ.1) LPM=0
216   IF (LPM.EQ.15) IE=1
217   LPM=LPM+IE
218   GO TO 2000,2001,MODEL
219 2011 CONTINUE
220   LPM=LPM+1
221   IF (LPM.EQ.1) LPM=0
222   IF (LPM.EQ.15) IE=1
223   LPM=LPM+IE
224   GO TO 2000,2001,MODEL
225 2012 CONTINUE
226   LPM=LPM+1
227   IF (LPM.EQ.1) LPM=0
228   IF (LPM.EQ.15) IE=1
229   LPM=LPM+IE
230   GO TO 2000,2001,MODEL

```


[illegible]


```

1  SUBROUTINE SPRAY
2  SUBROUTINE SPRAY
3  SUBROUTINE SPRAY
4  SUBROUTINE SPRAY
5  SUBROUTINE SPRAY
6  SUBROUTINE SPRAY
7  SUBROUTINE SPRAY
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9  SUBROUTINE SPRAY
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100 SUBROUTINE SPRAY

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Page 3984

FTW 4-6-439

08124175 14.03.66

Page 3984

95/24/78 14.00.46

FTN 4.0+439

SUBROUTINE STRIDE 73/74 OPT=0 TRACE

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397 307=0
398 307=0
399 307=0
400 307=0
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09/26/78 14:08.46

STN 4.5439

SUBROUTINE STAIRS 377- OPT=0 TRACE

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455      IF (LZP) GO TO 47
456      IF (LZP) GO TO 47
457      IF (LZP) GO TO 47
458      IF (LZP) GO TO 47
459      IF (LZP) GO TO 47
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533      IF (LZP) GO TO 47

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925      C=1.0
926      C=1.0
927      C=1.0
928      C=1.0
929      C=1.0
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971      C=1.0
972      C=1.0
973      C=1.0
974      C=1.0
975      C=1.0

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CARD NO. SEVERITY DETAILS DIAGNOSTIC GC PROBLEM

```

45      CONTROL VARIABLE IN COMMON
46      CONTROL VARIABLE IN COMMON
47      CONTROL VARIABLE IN COMMON
48      CONTROL VARIABLE IN COMMON
49      CONTROL VARIABLE IN COMMON
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100     CONTROL VARIABLE IN COMMON

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SUBROUTINE FPRINT 73776 OPT=0 TRACE PAGE 2
CARD NO. SEVERITY DETAILS
41 DIAGNOSIS OF PROBLEM
CONTROL VARIABLE IN COMMON OR EQUIVALENCED, OPTIMIZATION MAY BE INITIATED.

APPENDIX D

LISTING OF LINER COOLING MODEL

PAGE 1

08/24/78 13.44.16

SYM 4-A439

73.74 OPT=0 TRACE

PROGRAM MAIN

```

1  PROGRAM MAIN (INPUT,OUTPUT,TABF5=INPUT,TABF6=OUTPUT)
2  *****
3  *****
4  ***** CCFRUSTS DESIGN (2) = 0 *****
5  ***** WALL COOLING MODEL *****
6  *****
7  *****
8  *****
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925 IF (NEXANE-Z) GO TO 97
930 IF (NEXANE-Z) GO TO 97
935 IF (NEXANE-Z) GO TO 97
940 IF (NEXANE-Z) GO TO 97
945 IF (NEXANE-Z) GO TO 97
950 IF (NEXANE-Z) GO TO 97
955 IF (NEXANE-Z) GO TO 97
960 IF (NEXANE-Z) GO TO 97
965 IF (NEXANE-Z) GO TO 97
970 IF (NEXANE-Z) GO TO 97
975 IF (NEXANE-Z) GO TO 97
980 IF (NEXANE-Z) GO TO 97
985 IF (NEXANE-Z) GO TO 97
990 IF (NEXANE-Z) GO TO 97
995 IF (NEXANE-Z) GO TO 97
1000 IF (NEXANE-Z) GO TO 97

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08/24/79 13-00-10

FTW 4-0-039

FUNCTION TAB 73/74 CRYPTO TRACE

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1  FUNCTION TAB (FUNCTION)
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DATA NO. SECURITY DETAILS DISCLOSED TO PEOPLE
 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66 67 68 69 70 71 72 73 74 75 76 77 78 79 80 81 82 83 84 85 86 87 88 89 90 91 92 93 94 95 96 97 98 99 100

08/26/74 13.44.19

PTM 6.0+330

SUBROUTINE 43E 73/74 DPT=0 TRACE

```

90      Y=11-1.00E+110.5
91      D=11-1.00E+110.5
92      D=11-1.00E+110.5
93      D=11-1.00E+110.5
94      D=11-1.00E+110.5
95      D=11-1.00E+110.5
96      D=11-1.00E+110.5
97      D=11-1.00E+110.5
98      D=11-1.00E+110.5
99      D=11-1.00E+110.5
100     D=11-1.00E+110.5
101     D=11-1.00E+110.5
102     D=11-1.00E+110.5
103     D=11-1.00E+110.5
104     D=11-1.00E+110.5
105     D=11-1.00E+110.5
106     D=11-1.00E+110.5
107     D=11-1.00E+110.5
108     D=11-1.00E+110.5
109     D=11-1.00E+110.5
110     D=11-1.00E+110.5
111     D=11-1.00E+110.5
112     D=11-1.00E+110.5
113     D=11-1.00E+110.5
114     D=11-1.00E+110.5
115     D=11-1.00E+110.5
116     D=11-1.00E+110.5
117     D=11-1.00E+110.5
118     D=11-1.00E+110.5
119     D=11-1.00E+110.5
120     D=11-1.00E+110.5
121     D=11-1.00E+110.5
122     D=11-1.00E+110.5
123     D=11-1.00E+110.5
124     D=11-1.00E+110.5
125     D=11-1.00E+110.5
126     D=11-1.00E+110.5
127     D=11-1.00E+110.5
128     D=11-1.00E+110.5
129     D=11-1.00E+110.5
130     D=11-1.00E+110.5
131     D=11-1.00E+110.5
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138     D=11-1.00E+110.5
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147     D=11-1.00E+110.5
148     D=11-1.00E+110.5
149     D=11-1.00E+110.5
150     D=11-1.00E+110.5
151     D=11-1.00E+110.5
152     D=11-1.00E+110.5
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158     D=11-1.00E+110.5
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161     D=11-1.00E+110.5
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163     D=11-1.00E+110.5
164     D=11-1.00E+110.5
165     D=11-1.00E+110.5
166     D=11-1.00E+110.5
167     D=11-1.00E+110.5
168     D=11-1.00E+110.5
169     D=11-1.00E+110.5
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171     D=11-1.00E+110.5
172     D=11-1.00E+110.5
173     D=11-1.00E+110.5
174     D=11-1.00E+110.5
175     D=11-1.00E+110.5
176     D=11-1.00E+110.5
177     D=11-1.00E+110.5
178     D=11-1.00E+110.5
179     D=11-1.00E+110.5
180     D=11-1.00E+110.5
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183     D=11-1.00E+110.5
184     D=11-1.00E+110.5
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187     D=11-1.00E+110.5
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189     D=11-1.00E+110.5
190     D=11-1.00E+110.5
191     D=11-1.00E+110.5
192     D=11-1.00E+110.5
193     D=11-1.00E+110.5
194     D=11-1.00E+110.5
195     D=11-1.00E+110.5
196     D=11-1.00E+110.5
197     D=11-1.00E+110.5
198     D=11-1.00E+110.5
199     D=11-1.00E+110.5
200     D=11-1.00E+110.5

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155  DVE=DTM
    IROUND=1
    GO TO 240
160  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
165  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
170  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
175  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
180  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
185  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
190  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
195  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
200  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1
205  DVE=DTM-DVE
    DVE=DTM-DVE
    DVE=DTM-DVE
    IROUND=1

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30 IF (1.09-1) T=AM(1,1)
   ARG=AM(1,1)+T*AM(2,1)+T*AM(3,1)+T*AM(4,1)+T*AM(5,1)
   GO TO 35
20 ARG=AL(1,1)+T*AM(1,1)+T*AM(2,1)+T*AM(3,1)+T*AM(4,1)+T*AM(5,1)
25 GO TO 40
35 C *****
   ENTRY MOR
   IF (1.09-1) T=AM(1,1)
   IF (1.09-1) GO TO 30
   ARG=AM(1,1)+T*AM(2,1)+T*AM(3,1)+T*AM(4,1)+T*AM(5,1)
   GO TO 35
40 C *****
   IF (1.09-1) T=AM(1,1)
   IF (1.09-1) GO TO 30
   ARG=AM(1,1)+T*AM(2,1)+T*AM(3,1)+T*AM(4,1)+T*AM(5,1)
   GO TO 35
35 C *****
   IF (1.09-1) T=AM(1,1)
   IF (1.09-1) GO TO 30
   ARG=AM(1,1)+T*AM(2,1)+T*AM(3,1)+T*AM(4,1)+T*AM(5,1)
   GO TO 35
40 C *****
   IF (1.09-1) T=AM(1,1)
   IF (1.09-1) GO TO 30
   ARG=AM(1,1)+T*AM(2,1)+T*AM(3,1)+T*AM(4,1)+T*AM(5,1)
   GO TO 35

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[illegible][illegible]

304

PAGE 3

08/24/79 13.46.16

FTM 4.00030

73/74 0814C TRACE

SUPROUTINE ATEND

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RETURN
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155

CARD NO. SEVERITY DETAILS DIAGNOSIS OF PROBLEM

101 I AM IS STATEMENT MAY BE MADE EFFICIENT T400 A 2 ON 2 BRANCH COMPUTED GO TO STATEMENT.


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235 3121-181210J111-C(211)D(17)
236 3122-181210J111-C(211)D(17)
237 3123-181210J111-C(211)D(17)
238 3124-181210J111-C(211)D(17)
239 3125-181210J111-C(211)D(17)
240 3126-181210J111-C(211)D(17)
241 3127-181210J111-C(211)D(17)
242 3128-181210J111-C(211)D(17)
243 3129-181210J111-C(211)D(17)
244 3130-181210J111-C(211)D(17)
245 3131-181210J111-C(211)D(17)
246 3132-181210J111-C(211)D(17)
247 3133-181210J111-C(211)D(17)
248 3134-181210J111-C(211)D(17)
249 3135-181210J111-C(211)D(17)
250 3136-181210J111-C(211)D(17)
251 3137-181210J111-C(211)D(17)
252 3138-181210J111-C(211)D(17)
253 3139-181210J111-C(211)D(17)
254 3140-181210J111-C(211)D(17)
255 3141-181210J111-C(211)D(17)
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257 3143-181210J111-C(211)D(17)
258 3144-181210J111-C(211)D(17)
259 3145-181210J111-C(211)D(17)
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261 3147-181210J111-C(211)D(17)
262 3148-181210J111-C(211)D(17)
263 3149-181210J111-C(211)D(17)
264 3150-181210J111-C(211)D(17)
265 3151-181210J111-C(211)D(17)
266 3152-181210J111-C(211)D(17)
267 3153-181210J111-C(211)D(17)
268 3154-181210J111-C(211)D(17)
269 3155-181210J111-C(211)D(17)
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274 3160-181210J111-C(211)D(17)
275 3161-181210J111-C(211)D(17)
276 3162-181210J111-C(211)D(17)
277 3163-181210J111-C(211)D(17)
278 3164-181210J111-C(211)D(17)
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280 3166-181210J111-C(211)D(17)
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282 3168-181210J111-C(211)D(17)
283 3169-181210J111-C(211)D(17)
284 3170-181210J111-C(211)D(17)
285 3171-181210J111-C(211)D(17)
286 3172-181210J111-C(211)D(17)
287 3173-181210J111-C(211)D(17)
288 3174-181210J111-C(211)D(17)
289 3175-181210J111-C(211)D(17)
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293 3179-181210J111-C(211)D(17)
294 3180-181210J111-C(211)D(17)
295 3181-181210J111-C(211)D(17)
296 3182-181210J111-C(211)D(17)
297 3183-181210J111-C(211)D(17)
298 3184-181210J111-C(211)D(17)
299 3185-181210J111-C(211)D(17)
300 3186-181210J111-C(211)D(17)

```

[illegible]


```

112 OUT1=SPR1(5+AMBE/80)SPR1(16467+AMBE/24.)
113 SPR1(16467+AMBE/24.)
113 OUT1=SPR1(16467+AMBE/24.)
113 S=SPR1(16467+AMBE/24.)
103 FM U(125)=MDE+MDE/ARS(Y(13)-Y(73))
103 OUT2=OUT2+MDE/ARS(Y(13)-Y(73))
C OUT1=1.0*OUT1+0.99*LAST
OUT1=OUT1+0.99*LAST
RETURN
C----- STAGNATION ENTHALPY, FIEL. OR-FU/NDFU
200 IF (RE=1) 132.25 GO TO 210
IF (MODEL=1) 132.25 GO TO 210
IF (AMG=1) 132.25 GO TO 210
PPAT=PP(1)/PP(1)
CJAY=PP(1)/PP(1)
OUT1=0.0
IF (1+EQ.JM) OUT1=(1-1.0)*5.0JREF002
OUT2=5.0JREF
IF (1+EQ.JM) OUT2=C.
OUT3=OUT2/R(1)
210 IF (AMG=1) 132.25 GO TO 211
GO TO 212
211 S=1.0/PP(1)
212 IF (1+EQ.JM) OUT1=(PP(1)-1.0)*5.0JREF002
OUT2=5.0JREF
IF (1+EQ.JM) OUT2=0.
OUT3=OUT2/R(1)
RETURN
END

```

[illegible]

SUBROUTINE PLOTS

73/74 OPT=0 TRACE

PTM 4.0439

08/24/78 13.44.16

PAGE

2

80

49 A(1)=BLANK
40 CONTINUE

50 DO 50 I=1,11
51 A(I)=10*(DAV(I)-1)
52 WRITE(6,100) (A(I), I=1,11)

100 FORMAT(11H I=1,11 A(I)=,10(I),A6,A6)

101 FORMATT(10,2) A(I)=,10(I),A6,A6)

102 FORMATT(10,2) A(I)=,10(I),A6,A6)

103 FORMATT(10,2) A(I)=,10(I),A6,A6)

104 FORMATT(10,2) A(I)=,10(I),A6,A6)

105 FORMATT(10,2) A(I)=,10(I),A6,A6)

106 FORMATT(10,2) A(I)=,10(I),A6,A6)

VALUF =.1PE10.3)

VALUF =.1PE10.3)

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VALUF =.1PE10.3)

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LISTING OF TRANSITION MIXING MODEL

316

[illegible]

321

28/26/78 10.30.04

FIM 4.5430

PROGRAM NAME 7376 DOT-5 TRACE

```

465      IF (STEP-EO-0) TAVE=0.
470      DO 75 J=1,4
475      IF (JUEUED-0) GO TO 84
480      IF (JUEUED-0) GO TO 84
485      IF (JUEUED-0) GO TO 84
490      IF (JUEUED-0) GO TO 84
495      IF (JUEUED-0) GO TO 84
500      IF (JUEUED-0) GO TO 84
505      IF (JUEUED-0) GO TO 84
510      IF (JUEUED-0) GO TO 84
515      IF (JUEUED-0) GO TO 84
520      IF (JUEUED-0) GO TO 84
525      IF (JUEUED-0) GO TO 84
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680      IF (JUEUED-0) GO TO 84
685      IF (JUEUED-0) GO TO 84
690      IF (JUEUED-0) GO TO 84
695      IF (JUEUED-0) GO TO 84
700      IF (JUEUED-0) GO TO 84
705      IF (JUEUED-0) GO TO 84
710      IF (JUEUED-0) GO TO 84
715      IF (JUEUED-0) GO TO 84
720      IF (JUEUED-0) GO TO 84
725      IF (JUEUED-0) GO TO 84
730      IF (JUEUED-0) GO TO 84
735      IF (JUEUED-0) GO TO 84
740      IF (JUEUED-0) GO TO 84
745      IF (JUEUED-0) GO TO 84
750      IF (JUEUED-0) GO TO 84
755      IF (JUEUED-0) GO TO 84
760      IF (JUEUED-0) GO TO 84
765      IF (JUEUED-0) GO TO 84
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775      IF (JUEUED-0) GO TO 84
780      IF (JUEUED-0) GO TO 84
785      IF (JUEUED-0) GO TO 84
790      IF (JUEUED-0) GO TO 84
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800      IF (JUEUED-0) GO TO 84
805      IF (JUEUED-0) GO TO 84
810      IF (JUEUED-0) GO TO 84
815      IF (JUEUED-0) GO TO 84
820      IF (JUEUED-0) GO TO 84
825      IF (JUEUED-0) GO TO 84
830      IF (JUEUED-0) GO TO 84
835      IF (JUEUED-0) GO TO 84
840      IF (JUEUED-0) GO TO 84
845      IF (JUEUED-0) GO TO 84
850      IF (JUEUED-0) GO TO 84
855      IF (JUEUED-0) GO TO 84
860      IF (JUEUED-0) GO TO 84
865      IF (JUEUED-0) GO TO 84
870      IF (JUEUED-0) GO TO 84
875      IF (JUEUED-0) GO TO 84
880      IF (JUEUED-0) GO TO 84
885      IF (JUEUED-0) GO TO 84
890      IF (JUEUED-0) GO TO 84
895      IF (JUEUED-0) GO TO 84
900      IF (JUEUED-0) GO TO 84
905      IF (JUEUED-0) GO TO 84
910      IF (JUEUED-0) GO TO 84
915      IF (JUEUED-0) GO TO 84
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970      IF (JUEUED-0) GO TO 84
975      IF (JUEUED-0) GO TO 84
980      IF (JUEUED-0) GO TO 84
985      IF (JUEUED-0) GO TO 84
990      IF (JUEUED-0) GO TO 84
995      IF (JUEUED-0) GO TO 84

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940      UCI=U(1)/H(1)
941      PII=P(1)/H(1)
942      QII=Q(1)/H(1)
943      CALL STRENGTH
944      CALL STRENGTH
945      CALL STRENGTH
946      CALL STRENGTH
947      CALL STRENGTH
948      CALL STRENGTH
949      CALL STRENGTH
950      CALL STRENGTH
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999      CALL STRENGTH
1000     CALL STRENGTH

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FM 4-6439

PROGRAM NAME 13/74 COPY=0 TRACE

[illegible]

CARD NO.	310	PROGRAM MAIN	73/74	OPT=0 TRACE	FTN 4.6+430	08/24/70	10-3C-04	PAGE	13
SEVERITY	1	DETAILS	DIAGNOSIS OF PROBLEM						
	1		AN IF STATEMENT MAY BE		INAM 4 2 OR 3	BRANCH COMPUTED	GO TO STATEMENT.		
	1		AN IF STATEMENT MAY BE		INAM 4 2 OR 3	BRANCH COMPUTED	GO TO STATEMENT.		
	1		AN IF STATEMENT MAY BE		INAM 4 2 OR 3	BRANCH COMPUTED	GO TO STATEMENT.		
	1		AN IF STATEMENT MAY BE		INAM 4 2 OR 3	BRANCH COMPUTED	GO TO STATEMENT.		
	1		AN IF STATEMENT MAY BE		INAM 4 2 OR 3	BRANCH COMPUTED	GO TO STATEMENT.		

FTM 4-6-439 08/24/78 10.30.04 PAGE 1

00 FURRAY 1 000 ERROR IN SUBROUTINE TAG 000, E15.6, 2151
END

CARD NO.	SEVERITY	DETAILS	DIAGNOSIS OF PROBLEM	ARRAY REFERENCE	OUTSIDE DIMENSION COUNTS.
7	I	XX			

	FUNCTION MODE	73/74	CPT=0 TRACE	FIM 4.6-4.39	08/24/78	10.30.04	PAGE 1
1							
	FUNCTION MODE {X,XS,M}						
	DIMENSION XX(1)						
	1P X=X.XX(1)-OM.X.CT.XX(M) GO TO 20						
5	DO -10 I=2,M						
	IF X-GE.XK(I),ABS-X.(LT.XK(I)) GO TO 15						
	10 CONTINUE						
	15 X=XK-I						
	RETURN						
10	END						
	FINISH (4.25) X.XX(1),XX(M)						
	25 PRINT F(1.00 ERROR IN FUNCTION MODE 00.3615.5)						
	END RETURN						
	END						

[illegible]


```

310      D(MP2)=D(MP2)+D(MP2)*D(MP2)-2.*D(MP2)*D(MP2)-D(MP2)*
      2315      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      2320      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      C 2325      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      315      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      320      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      325      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      330      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      335      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      340      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      345      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      350      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      355      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      360      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      365      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      370      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      375      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      380      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*
      385      D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*D(MP2)+D(MP2)*

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[illegible]

APPENDIX F LISTING OF EMISSIONS MODEL

PAGE 1

20/24/76 16.42.35

SVN 6.5-439

73/74 TOT-C 10ACE

PROGRAM MAIN

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1  PROGRAM MAIN (INPUT, OUTPUT, TAPES-INPUT, TAPES-OUTPUT, TAPES)
2  EMISSIONS MODEL
3
4  ***** COMBUSTION DESIGN CRITERIA *****
5
6  ***** EMISSIONS MODEL *****
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8  ***** EMISSIONS MODEL *****
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10 ***** EMISSIONS MODEL *****
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100 ***** EMISSIONS MODEL *****

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604      CALL MP31(TWJINJME1)
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 272 CONTINUE
700      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 206 CONTINUE
704      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 208 CONTINUE
710      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 210 CONTINUE
714      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 214 CONTINUE
718      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 218 CONTINUE
722      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 222 CONTINUE
726      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 226 CONTINUE
730      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 230 CONTINUE
734      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 234 CONTINUE
738      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 238 CONTINUE
742      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 242 CONTINUE
746      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 246 CONTINUE
750      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 250 CONTINUE
754      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 254 CONTINUE
758      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 258 CONTINUE
762      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 262 CONTINUE
766      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 266 CONTINUE
770      IF (ABS(TWJINJME1)-SUM) .GT. 1E-10 GO TO 206
        SUM=0.0
        DO I=1,NP3
          SUM=SUM+TWJINJME1(I)
        END DO
        ME-SUM*2.0/AVJINJ(ME1)-SUM2/AVJINJ(ME1)
        C 270 CONTINUE

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1005 C
1010 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1015 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1020 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1025 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1030 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1035 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1040 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1045 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1050 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1055 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1060 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1065 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1070 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/
1075 1 5M XE=12.7M BX=1PE11.3-4M PS11=ELL.3-4M PS1E=ELL.3/

```


FUNCTION VISC0 73/74 OPT=3 TRACE
 1 FUNCTION VISCOUT1
 5 VISCOUT1=1.00E-07 TO 10
 RETURN
 10 VISCOUT1=1.00E-07 TO 10
 RETURN
 CWD

FTN 4.0-430

08/24/78 14.02.39

PAGE 1

1A
 1A
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195 500-7505(AM,MP21)-2505(AM,MP11)
196 500-7505(AM,MP21)-2505(AM,MP11)
197 500-7505(AM,MP21)-2505(AM,MP11)
198 500-7505(AM,MP21)-2505(AM,MP11)
199 500-7505(AM,MP21)-2505(AM,MP11)
200 500-7505(AM,MP21)-2505(AM,MP11)
201 500-7505(AM,MP21)-2505(AM,MP11)
202 500-7505(AM,MP21)-2505(AM,MP11)
203 500-7505(AM,MP21)-2505(AM,MP11)
204 500-7505(AM,MP21)-2505(AM,MP11)
205 500-7505(AM,MP21)-2505(AM,MP11)
206 500-7505(AM,MP21)-2505(AM,MP11)
207 500-7505(AM,MP21)-2505(AM,MP11)
208 500-7505(AM,MP21)-2505(AM,MP11)
209 500-7505(AM,MP21)-2505(AM,MP11)
210 500-7505(AM,MP21)-2505(AM,MP11)
211 500-7505(AM,MP21)-2505(AM,MP11)
212 500-7505(AM,MP21)-2505(AM,MP11)
213 500-7505(AM,MP21)-2505(AM,MP11)
214 500-7505(AM,MP21)-2505(AM,MP11)
215 500-7505(AM,MP21)-2505(AM,MP11)
216 500-7505(AM,MP21)-2505(AM,MP11)
217 500-7505(AM,MP21)-2505(AM,MP11)
218 500-7505(AM,MP21)-2505(AM,MP11)
219 500-7505(AM,MP21)-2505(AM,MP11)
220 500-7505(AM,MP21)-2505(AM,MP11)
221 500-7505(AM,MP21)-2505(AM,MP11)
222 500-7505(AM,MP21)-2505(AM,MP11)
223 500-7505(AM,MP21)-2505(AM,MP11)
224 500-7505(AM,MP21)-2505(AM,MP11)
225 500-7505(AM,MP21)-2505(AM,MP11)
226 500-7505(AM,MP21)-2505(AM,MP11)
227 500-7505(AM,MP21)-2505(AM,MP11)
228 500-7505(AM,MP21)-2505(AM,MP11)
229 500-7505(AM,MP21)-2505(AM,MP11)
230 500-7505(AM,MP21)-2505(AM,MP11)

```

SUBROUTINE AUX 73/74 OPT=0 TRACE 674 5.0+039 00/24/70 16.02.35 PAGE 4

END

CARD NO. SEVERITY DETAILS DIAGNOSIS OF PROBLEM
 60 1 1
 107 1 1
 206 1 1

AM IF STATEMENT MAY BE MORE EFFICIENT THAN 1 2 ON 3 SEARCH COMPUTED GO TO STATEMENT.
 AM IF STATEMENT MAY BE MORE EFFICIENT THAN 1 2 ON 3 SEARCH COMPUTED GO TO STATEMENT.
 AM IF STATEMENT MAY BE MORE EFFICIENT THAN 1 2 ON 3 SEARCH COMPUTED GO TO STATEMENT.

372

```

1  FUNCTION GASP (IT, I)
2  DIMENSION AM(7,12), AL(7,12), NL(12)
3  SPECIES ORDER = PUEL, CD2, CO, O2, WZD, OH, O3, H2, H2O, H, NC, N2
4  DATA ((AM(I, J), I=1, 7), J=1, 12))
5  DATA ((AL(I, J), I=1, 7), J=1, 12))
6  DATA ((NL(I), I=1, 12))
7  DATA ((NL(I), I=1, 12))
8  DATA ((NL(I), I=1, 12))
9  DATA ((NL(I), I=1, 12))
10 DATA ((NL(I), I=1, 12))
11 DATA ((NL(I), I=1, 12))
12 DATA ((NL(I), I=1, 12))
13 DATA ((NL(I), I=1, 12))
14 DATA ((NL(I), I=1, 12))
15 DATA ((NL(I), I=1, 12))
16 DATA ((NL(I), I=1, 12))
17 DATA ((NL(I), I=1, 12))
18 DATA ((NL(I), I=1, 12))
19 DATA ((NL(I), I=1, 12))
20 DATA ((NL(I), I=1, 12))
21 DATA ((NL(I), I=1, 12))
22 DATA ((NL(I), I=1, 12))
23 DATA ((NL(I), I=1, 12))
24 DATA ((NL(I), I=1, 12))
25 DATA ((NL(I), I=1, 12))
26 DATA ((NL(I), I=1, 12))
27 DATA ((NL(I), I=1, 12))
28 DATA ((NL(I), I=1, 12))
29 DATA ((NL(I), I=1, 12))
30 DATA ((NL(I), I=1, 12))
31 DATA ((NL(I), I=1, 12))
32 DATA ((NL(I), I=1, 12))
33 DATA ((NL(I), I=1, 12))
34 DATA ((NL(I), I=1, 12))
35 DATA ((NL(I), I=1, 12))
36 DATA ((NL(I), I=1, 12))
37 DATA ((NL(I), I=1, 12))
38 DATA ((NL(I), I=1, 12))
39 DATA ((NL(I), I=1, 12))
40 DATA ((NL(I), I=1, 12))
41 DATA ((NL(I), I=1, 12))
42 DATA ((NL(I), I=1, 12))
43 DATA ((NL(I), I=1, 12))
44 DATA ((NL(I), I=1, 12))
45 DATA ((NL(I), I=1, 12))
46 DATA ((NL(I), I=1, 12))
47 DATA ((NL(I), I=1, 12))
48 DATA ((NL(I), I=1, 12))
49 DATA ((NL(I), I=1, 12))
50 DATA ((NL(I), I=1, 12))
51 DATA ((NL(I), I=1, 12))
52 DATA ((NL(I), I=1, 12))
53 DATA ((NL(I), I=1, 12))
54 DATA ((NL(I), I=1, 12))
55 DATA ((NL(I), I=1, 12))
56 DATA ((NL(I), I=1, 12))
57 DATA ((NL(I), I=1, 12))
58 DATA ((NL(I), I=1, 12))
59 DATA ((NL(I), I=1, 12))
60 DATA ((NL(I), I=1, 12))
61 DATA ((NL(I), I=1, 12))
62 DATA ((NL(I), I=1, 12))
63 DATA ((NL(I), I=1, 12))
64 DATA ((NL(I), I=1, 12))
65 DATA ((NL(I), I=1, 12))
66 DATA ((NL(I), I=1, 12))
67 DATA ((NL(I), I=1, 12))
68 DATA ((NL(I), I=1, 12))
69 DATA ((NL(I), I=1, 12))
70 DATA ((NL(I), I=1, 12))
71 DATA ((NL(I), I=1, 12))
72 DATA ((NL(I), I=1, 12))
73 DATA ((NL(I), I=1, 12))
74 DATA ((NL(I), I=1, 12))
75 DATA ((NL(I), I=1, 12))
76 DATA ((NL(I), I=1, 12))
77 DATA ((NL(I), I=1, 12))
78 DATA ((NL(I), I=1, 12))

```

```

IF (I.EQ.1) T=AM(1,I),T1=2
  IF (I.EQ.1000) GO TO 20
  ARG=AM(1,I)+T*AM(2,I)+T*AM(3,I)+T*AM(4,I)+T*AM(5,I)
  GO TO 25
20 ARG=AM(1,I)+T*AM(2,I)+T*AM(3,I)+T*AM(4,I)+T*AM(5,I)
25 CASP=ARG*1.987461847/MII
  RETURN
C *****
      ENTRY MOR
      T=1
      IF (I.EQ.1) T=AM(1,I),T1=2
      IF (I.EQ.1000) GO TO 30
      ARG=AM(1,I)+T*AM(2,I)+T*AM(3,I)+T*AM(4,I)+T*AM(5,I)
      GO TO 35
30 ARG=AM(1,I)+T*AM(2,I)+T*AM(3,I)+T*AM(4,I)+T*AM(5,I)
35 CASP=ARG*1.987461847/MII
  IF (I.EQ.1) T1=1,RETURN
  GO TO 1000
      ENTRY T1MII
      CASP=ARG*1.987461847/MII
      RETURN
C *****
      ENTRY CORE
      EDUNT=EDUNT+1
      IF (EDUNT.EQ.2) GO TO 40
      T=1
      GO TO 100
      ENTRY
      RETURN
40 EDUNT=1
  ARG=AM(1,I)+T*AM(2,I)+T*AM(3,I)+T*AM(4,I)+T*AM(5,I)
  CASP=ARG*1.987461847/MII
  RETURN
C *****

```


06/24/78 14.42.35

FTN 6.0-030

SUBROUTINE STRIDE 73/74 OPT=0 TRACE

```

80      1106 R(1)=V(1)/CSALFA
      1107 V(1)=R(1)*CSALFA
      1108 GO TO 1107
      C
85      1109 R(1)=V(1)/CSALFA
      1110 V(1)=R(1)*CSALFA
      1111 GO TO 1109
      C
90      1112 R(1)=V(1)/CSALFA
      1113 V(1)=R(1)*CSALFA
      1114 GO TO 1112
      C
95      1115 R(1)=V(1)/CSALFA
      1116 V(1)=R(1)*CSALFA
      1117 GO TO 1115
      C
100     1118 R(1)=V(1)/CSALFA
      1119 V(1)=R(1)*CSALFA
      1120 GO TO 1118
      C
105     1121 R(1)=V(1)/CSALFA
      1122 V(1)=R(1)*CSALFA
      1123 GO TO 1121
      C
110     1124 R(1)=V(1)/CSALFA
      1125 V(1)=R(1)*CSALFA
      1126 GO TO 1124
      C
115     1127 R(1)=V(1)/CSALFA
      1128 V(1)=R(1)*CSALFA
      1129 GO TO 1127
      C
120     1130 R(1)=V(1)/CSALFA
      1131 V(1)=R(1)*CSALFA
      1132 GO TO 1130
      C
125     1133 R(1)=V(1)/CSALFA
      1134 V(1)=R(1)*CSALFA
      1135 GO TO 1133
      C
130     1136 R(1)=V(1)/CSALFA
      1137 V(1)=R(1)*CSALFA
      1138 GO TO 1136
      C
135     1139 R(1)=V(1)/CSALFA
      1140 V(1)=R(1)*CSALFA
      1141 GO TO 1139
      C
140     1142 R(1)=V(1)/CSALFA
      1143 V(1)=R(1)*CSALFA
      1144 GO TO 1142
      C
145     1145 R(1)=V(1)/CSALFA
      1146 V(1)=R(1)*CSALFA
      1147 GO TO 1145
      C
150     1148 R(1)=V(1)/CSALFA
      1149 V(1)=R(1)*CSALFA
      1150 GO TO 1148
      C

```


[illegible]

[illegible]

08/24/78 14.42.35

FTK 4.6439

STRIDE 73/74 OPT-0 TRACE

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390 3700 3710 3720 3730 3740 3750 3760 3770 3780 3790 3800 3810 3820 3830 3840 3850 3860 3870 3880 3890 3900
391 3920 3930 3940 3950 3960 3970 3980 3990 4000 4010 4020 4030 4040 4050 4060 4070 4080 4090 4100 4110 4120
413 4130 4140 4150 4160 4170 4180 4190 4200 4210 4220 4230 4240 4250 4260 4270 4280 4290 4300 4310 4320 4330
434 4340 4350 4360 4370 4380 4390 4400 4410 4420 4430 4440 4450 4460 4470 4480 4490 4500 4510 4520 4530 4540
455 4550 4560 4570 4580 4590 4600 4610 4620 4630 4640 4650 4660 4670 4680 4690 4700 4710 4720 4730 4740 4750
476 4760 4770 4780 4790 4800 4810 4820 4830 4840 4850 4860 4870 4880 4890 4900 4910 4920 4930 4940 4950 4960
497 4970 4980 4990 5000 5010 5020 5030 5040 5050 5060 5070 5080 5090 5100 5110 5120 5130 5140 5150 5160 5170
518 5180 5190 5200 5210 5220 5230 5240 5250 5260 5270 5280 5290 5300 5310 5320 5330 5340 5350 5360 5370 5380
539 5390 5400 5410 5420 5430 5440 5450 5460 5470 5480 5490 5500 5510 5520 5530 5540 5550 5560 5570 5580 5590
560 5600 5610 5620 5630 5640 5650 5660 5670 5680 5690 5700 5710 5720 5730 5740 5750 5760 5770 5780 5790 5800
581 5810 5820 5830 5840 5850 5860 5870 5880 5890 5900 5910 5920 5930 5940 5950 5960 5970 5980 5990 6000 6010
602 6020 6030 6040 6050 6060 6070 6080 6090 6100 6110 6120 6130 6140 6150 6160 6170 6180 6190 6200 6210 6220
623 6230 6240 6250 6260 6270 6280 6290 6300 6310 6320 6330 6340 6350 6360 6370 6380 6390 6400 6410 6420 6430
644 6440 6450 6460 6470 6480 6490 6500 6510 6520 6530 6540 6550 6560 6570 6580 6590 6600 6610 6620 6630 6640
665 6650 6660 6670 6680 6690 6700 6710 6720 6730 6740 6750 6760 6770 6780 6790 6800 6810 6820 6830 6840 6850
686 6860 6870 6880 6890 6900 6910 6920 6930 6940 6950 6960 6970 6980 6990 7000 7010 7020 7030 7040 7050 7060
707 7070 7080 7090 7100 7110 7120 7130 7140 7150 7160 7170 7180 7190 7200 7210 7220 7230 7240 7250 7260 7270
728 7280 7290 7300 7310 7320 7330 7340 7350 7360 7370 7380 7390 7400 7410 7420 7430 7440 7450 7460 7470 7480
749 7490 7500 7510 7520 7530 7540 7550 7560 7570 7580 7590 7600 7610 7620 7630 7640 7650 7660 7670 7680 7690
770 7700 7710 7720 7730 7740 7750 7760 7770 7780 7790 7800 7810 7820 7830 7840 7850 7860 7870 7880 7890 7900
791 7910 7920 7930 7940 7950 7960 7970 7980 7990 8000 8010 8020 8030 8040 8050 8060 8070 8080 8090 8100 8110
812 8120 8130 8140 8150 8160 8170 8180 8190 8200 8210 8220 8230 8240 8250 8260 8270 8280 8290 8300 8310 8320
833 8330 8340 8350 8360 8370 8380 8390 8400 8410 8420 8430 8440 8450 8460 8470 8480 8490 8500 8510 8520 8530
854 8540 8550 8560 8570 8580 8590 8600 8610 8620 8630 8640 8650 8660 8670 8680 8690 8700 8710 8720 8730 8740
875 8750 8760 8770 8780 8790 8800 8810 8820 8830 8840 8850 8860 8870 8880 8890 8900 8910 8920 8930 8940 8950
896 8960 8970 8980 8990 9000 9010 9020 9030 9040 9050 9060 9070 9080 9090 9100 9110 9120 9130 9140 9150 9160
917 9170 9180 9190 9200 9210 9220 9230 9240 9250 9260 9270 9280 9290 9300 9310 9320 9330 9340 9350 9360 9370
938 9380 9390 9400 9410 9420 9430 9440 9450 9460 9470 9480 9490 9500 9510 9520 9530 9540 9550 9560 9570 9580
959 9590 9600 9610 9620 9630 9640 9650 9660 9670 9680 9690 9700 9710 9720 9730 9740 9750 9760 9770 9780 9790
980 9800 9810 9820 9830 9840 9850 9860 9870 9880 9890 9900 9910 9920 9930 9940 9950 9960 9970 9980 9990 10000

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CARD NO. SEVERITY DETAILS DIAGNOSIS OF PROBLEM
 204 1 AN IF STATEMENT MAY BE MORE EFFICIENT THAN A 2 OR 3 BRANCH COMPUTED GO TO STATEMENT-
 397 1 AN IF STATEMENT MAY BE MORE EFFICIENT THAN A 2 OR 3 BRANCH COMPUTED GO TO STATEMENT-
 398 1 AN IF STATEMENT MAY BE MORE EFFICIENT THAN A 2 OR 3 BRANCH COMPUTED GO TO STATEMENT-

```

1 SUBROUTINE WF(IJ,OUT1,OUT2,OUT3)
  COMMON/COMPARM/ALPHA(12),BETA(12),GAMMA(12),DELTA(12),Epsilon(12),
  1 FIB(12),FIB2(12),FIB3(12),FIB4(12),FIB5(12),FIB6(12),FIB7(12),FIB8(12),
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APPENDIX G

LISTING OF FUEL INSTRUCTION MODEL

PAGE 1

06/24/78 14:28:13

FTM 4.0-435

OPT-6 TRACE

PROGRAM INJECTI 73/74

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1  PROGRAM INJECTI (INPUT,OUTPUT,TAPEO=INPUT,TAPEO=OUTPUT)
2  CCCCCCCCCC
3  PROGRAM TO CALCULATE TRAJECTORIES FOR SIMPLEX OR DUAL ORIFICE
4  CHARGES AND ADDITIONS MADE 3/2/71 TO INTERFACE SP EVAP
5  CHARGES AND ADDITIONS MADE 7/29/71 FOR COMPARISON CAPABILITY
6  CHARGES REFLECT PLANS FOR THIS UPDATE TO BECOME PART OF COSMAN
7  OUTPUT OF ROUTINE IS LOCATION OF E-1,2,3,4,5,6,7,8,9 FOR EACH OF 5
8  COMMON /OUTPUT/ X(1),Y(1),Z(1),X(2),Y(2),Z(2),X(3),Y(3),Z(3),X(4),Y(4),Z(4),X(5),Y(5),Z(5)
9  COMMON /INPUT/ X(1),Y(1),Z(1),X(2),Y(2),Z(2),X(3),Y(3),Z(3),X(4),Y(4),Z(4),X(5),Y(5),Z(5)
10 COMMON /TIME/ X(1),Y(1),Z(1),X(2),Y(2),Z(2),X(3),Y(3),Z(3),X(4),Y(4),Z(4),X(5),Y(5),Z(5)
11 COMMON /DIMENSION/ DIM(102,5), EY(102,5), Y(102,5), VE(102,5)
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1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29 30 31 32 33 34 35 36 37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66 67 68 69 70 71 72 73 74 75 76 77 78 79 80 81 82 83 84 85 86 87 88 89 90 91 92 93 94 95 96 97 98 99 100 101 102 103 104 105 106 107 108 109 110 111 112 113 114 115 116 117 118 119 120 121 122 123 124 125 126 127 128 129 130 131 132 133 134 135 136 137 138 139 140 141 142 143 144 145 146 147 148 149 150 151 152 153 154 155 156 157 158 159 160 161 162 163 164 165 166 167 168 169 170 171 172 173 174 175 176 177 178 179 180 181 182 183 184 185 186 187 188 189 190 191 192 193 194 195 196 197 198 199 200 201 202 203 204 205 206 207 208 209 210 211 212 213 214 215 216 217 218 219 220 221 222 223 224 225 226 227 228 229 230 231 232 233 234 235 236 237 238 239 240 241 242 243 244 245 246 247 248 249 250 251 252 253 254 255 256 257 258 259 260 261 262 263 264 265 266 267 268 269 270 271 272 273 274 275 276 277 278 279 280 281 282 283 284 285 286 287 288 289 290 291 292 293 294 295 296 297 298 299 300 301 302 303 304 305 306 307 308 309 310 311 312 313 314 315 316 317 318 319 320 321 322 323 324 325 326 327 328 329 330 331 332 333 334 335 336 337 338 339 340 341 342 343 344 345 346 347 348 349 350 351 352 353 354 355 356 357 358 359 360 361 362 363 364 365 366 367 368 369 370 371 372 373 374 375 376 377 378 379 380 381 382 383 384 385 386 387 388 389 390 391 392 393 394 395 396 397 398 399 400 401 402 403 404 405 406 407 408 409 410 411 412 413 414 415 416 417 418 419 420 421 422 423 424 425 426 427 428 429 430 431 432 433 434 435 436 437 438 439 440 441 442 443 444 445 446 447 448 449 450 451 452 453 454 455 456 457 458 459 460 461 462 463 464 465 466 467 468 469 470 471 472 473 474 475 476 477 478 479 480 481 482 483 484 485 486 487 488 489 490 491 492 493 494 495 496 497 498 499 500 501 502 503 504 505 506 507 508 509 510 511 512 513 514 515 516 517 518 519 520 521 522 523 524 525 526 527 528 529 530 531 532 533 534 535 536 537 538 539 540 541 542 543 544 545 546 547 548 549 550 551 552 553 554 555 556 557 558 559 560 561 562 563 564 565 566 567 568 569 570 571 572 573 574 575 576 577 578 579 580 581 582 583 584 585 586 587 588 589 590 591 592 593 594 595 596 597 598 599 600 601 602 603 604 605 606 607 608 609 610 611 612 613 614 615 616 617 618 619 620 621 622 623 624 625 626 627 628 629 630 631 632 633 634 635 636 637 638 639 640 641 642 643 644 645 646 647 648 649 650 651 652 653 654 655 656 657 658 659 660 661 662 663 664 665 666 667 668 669 670 671 672 673 674 675 676 677 678 679 680 681 682 683 684 685 686 687 688 689 690 691 692 693 694 695 696 697 698 699 700 701 702 703 704 705 706 707 708 709 710 711 712 713 714 715 716 717 718 719 720 721 722 723 724 725 726 727 728 729 730 731 732 733 734 735 736 737 738 739 740 741 742 743 744 745 746 747 748 749 750 751 752 753 754 755 756 757 758 759 760 761 762 763 764 765 766 767 768 769 770 771 772 773 774 775 776 777 778 779 780 781 782 783 784 785 786 787 788 789 790 791 792 793 794 795 796 797 798 799 800 801 802 803 804 805 806 807 808 809 810 811 812 813 814 815 816 817 818 819 820 821 822 823 824 825 826 827 828 829 830 831 832 833 834 835 836 837 838 839 840 841 842 843 844 845 846 847 848 849 850 851 852 853 854 855 856 857 858 859 860 861 862 863 864 865 866 867 868 869 870 871 872 873 874 875 876 877 878 879 880 881 882 883 884 885 886 887 888 889 890 891 892 893 894 895 896 897 898 899 900 901 902 903 904 905 906 907 908 909 910 911 912 913 914 915 916 917 918 919 920 921 922 923 924 925 926 927 928 929 930 931 932 933 934 935 936 937 938 939 940 941 942 943 944 945 946 947 948 949 950 951 952 953 954 955 956 957 958 959 960 961 962 963 964 965 966 967 968 969 970 971 972 973 974 975 976 977 978 979 980 981 982 983 984 985 986 987 988 989 990 991 992 993 994 995 996 997 998 999 1000 1001 1002 1003 1004 1005 1006 1007 1008 1009 1010 1011 1012 1013 1014 1015 1016 1017 1018 1019 1020 1021 1022 1023 1024 1025 1026 1027 1028 1029 1030 1031 1032 1033 1034 1035 1036 1037 1038 1039 104

DATE	TIME	LOCATION	WIND	TEMP	SEA	REMARKS
1964-11-11	0000	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0100	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0200	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0300	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0400	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0500	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0600	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0700	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0800	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	0900	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1000	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1100	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1200	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1300	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1400	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1500	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1600	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1700	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1800	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	1900	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	2000	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	2100	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	2200	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	2300	10-10N 155-00E	0000	24.0	000	10-10N 155-00E
1964-11-11	2400	10-10N 155-00E	0000	24.0	000	10-10N 155-00E

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28C IF (I*COUNT).13.6E.H(11)) GO TO 290
290 IF (I*COUNT).13.6E.H(11)) GO TO 300
290 IF (I*COUNT).13.6E.H(11)) GO TO 300
290 DUM=H(11)
290 GO TO 310
300 IF (I*COUNT).13.6E.H(11)) GO TO 310
300 DUM=H(11)
300 GO TO 320
310 IF (I*COUNT).13.6E.H(11)) GO TO 330
310 DUM=H(11)
310 GO TO 340
320 IF (I*COUNT).13.6E.H(11)) GO TO 350
320 DUM=H(11)
320 GO TO 360
330 IF (I*COUNT).13.6E.H(11)) GO TO 370
330 DUM=H(11)
330 GO TO 380
340 IF (I*COUNT).13.6E.H(11)) GO TO 390
340 DUM=H(11)
340 GO TO 400
350 IF (I*COUNT).13.6E.H(11)) GO TO 410
350 DUM=H(11)
350 GO TO 420
360 IF (I*COUNT).13.6E.H(11)) GO TO 430
360 DUM=H(11)
360 GO TO 440
370 IF (I*COUNT).13.6E.H(11)) GO TO 450
370 DUM=H(11)
370 GO TO 460
380 IF (I*COUNT).13.6E.H(11)) GO TO 470
380 DUM=H(11)
380 GO TO 480
390 IF (I*COUNT).13.6E.H(11)) GO TO 490
390 DUM=H(11)
390 GO TO 500
400 IF (I*COUNT).13.6E.H(11)) GO TO 510
400 DUM=H(11)
400 GO TO 520
410 IF (I*COUNT).13.6E.H(11)) GO TO 530
410 DUM=H(11)
410 GO TO 540
420 IF (I*COUNT).13.6E.H(11)) GO TO 550
420 DUM=H(11)
420 GO TO 560
430 IF (I*COUNT).13.6E.H(11)) GO TO 570
430 DUM=H(11)
430 GO TO 580
440 IF (I*COUNT).13.6E.H(11)) GO TO 590
440 DUM=H(11)
440 GO TO 600
450 IF (I*COUNT).13.6E.H(11)) GO TO 610
450 DUM=H(11)
450 GO TO 620
460 IF (I*COUNT).13.6E.H(11)) GO TO 630
460 DUM=H(11)
460 GO TO 640
470 IF (I*COUNT).13.6E.H(11)) GO TO 650
470 DUM=H(11)
470 GO TO 660
480 IF (I*COUNT).13.6E.H(11)) GO TO 670
480 DUM=H(11)
480 GO TO 680
490 IF (I*COUNT).13.6E.H(11)) GO TO 690
490 DUM=H(11)
490 GO TO 700
500 IF (I*COUNT).13.6E.H(11)) GO TO 710
500 DUM=H(11)
500 GO TO 720
510 IF (I*COUNT).13.6E.H(11)) GO TO 730
510 DUM=H(11)
510 GO TO 740
520 IF (I*COUNT).13.6E.H(11)) GO TO 750
520 DUM=H(11)
520 GO TO 760
530 IF (I*COUNT).13.6E.H(11)) GO TO 770
530 DUM=H(11)
530 GO TO 780
540 IF (I*COUNT).13.6E.H(11)) GO TO 790
540 DUM=H(11)
540 GO TO 800
550 IF (I*COUNT).13.6E.H(11)) GO TO 810
550 DUM=H(11)
550 GO TO 820
560 IF (I*COUNT).13.6E.H(11)) GO TO 830
560 DUM=H(11)
560 GO TO 840
570 IF (I*COUNT).13.6E.H(11)) GO TO 850
570 DUM=H(11)
570 GO TO 860
580 IF (I*COUNT).13.6E.H(11)) GO TO 870
580 DUM=H(11)
580 GO TO 880
590 IF (I*COUNT).13.6E.H(11)) GO TO 890
590 DUM=H(11)
590 GO TO 900
600 IF (I*COUNT).13.6E.H(11)) GO TO 910
600 DUM=H(11)
600 GO TO 920
610 IF (I*COUNT).13.6E.H(11)) GO TO 930
610 DUM=H(11)
610 GO TO 940
620 IF (I*COUNT).13.6E.H(11)) GO TO 950
620 DUM=H(11)
620 GO TO 960
630 IF (I*COUNT).13.6E.H(11)) GO TO 970
630 DUM=H(11)
630 GO TO 980
640 IF (I*COUNT).13.6E.H(11)) GO TO 990
640 DUM=H(11)
640 GO TO 1000
650 IF (I*COUNT).13.6E.H(11)) GO TO 1010
650 DUM=H(11)
650 GO TO 1020
660 IF (I*COUNT).13.6E.H(11)) GO TO 1030
660 DUM=H(11)
660 GO TO 1040
670 IF (I*COUNT).13.6E.H(11)) GO TO 1050
670 DUM=H(11)
670 GO TO 1060
680 IF (I*COUNT).13.6E.H(11)) GO TO 1070
680 DUM=H(11)
680 GO TO 1080
690 IF (I*COUNT).13.6E.H(11)) GO TO 1090
690 DUM=H(11)
690 GO TO 1100
700 IF (I*COUNT).13.6E.H(11)) GO TO 1110
700 DUM=H(11)
700 GO TO 1120
710 IF (I*COUNT).13.6E.H(11)) GO TO 1130
710 DUM=H(11)
710 GO TO 1140
720 IF (I*COUNT).13.6E.H(11)) GO TO 1150
720 DUM=H(11)
720 GO TO 1160
730 IF (I*COUNT).13.6E.H(11)) GO TO 1170
730 DUM=H(11)
730 GO TO 1180
740 IF (I*COUNT).13.6E.H(11)) GO TO 1190
740 DUM=H(11)
740 GO TO 1200
750 IF (I*COUNT).13.6E.H(11)) GO TO 1210
750 DUM=H(11)
750 GO TO 1220
760 IF (I*COUNT).13.6E.H(11)) GO TO 1230
760 DUM=H(11)
760 GO TO 1240
770 IF (I*COUNT).13.6E.H(11)) GO TO 1250
770 DUM=H(11)
770 GO TO 1260
780 IF (I*COUNT).13.6E.H(11)) GO TO 1270
780 DUM=H(11)
780 GO TO 1280
790 IF (I*COUNT).13.6E.H(11)) GO TO 1290
790 DUM=H(11)
790 GO TO 1300
800 IF (I*COUNT).13.6E.H(11)) GO TO 1310
800 DUM=H(11)
800 GO TO 1320
810 IF (I*COUNT).13.6E.H(11)) GO TO 1330
810 DUM=H(11)
810 GO TO 1340
820 IF (I*COUNT).13.6E.H(11)) GO TO 1350
820 DUM=H(11)
820 GO TO 1360
830 IF (I*COUNT).13.6E.H(11)) GO TO 1370
830 DUM=H(11)
830 GO TO 1380
840 IF (I*COUNT).13.6E.H(11)) GO TO 1390
840 DUM=H(11)
840 GO TO 1400
850 IF (I*COUNT).13.6E.H(11)) GO TO 1410
850 DUM=H(11)
850 GO TO 1420
860 IF (I*COUNT).13.6E.H(11)) GO TO 1430
860 DUM=H(11)
860 GO TO 1440
870 IF (I*COUNT).13.6E.H(11)) GO TO 1450
870 DUM=H(11)
870 GO TO 1460
880 IF (I*COUNT).13.6E.H(11)) GO TO 1470
880 DUM=H(11)
880 GO TO 1480
890 IF (I*COUNT).13.6E.H(11)) GO TO 1490
890 DUM=H(11)
890 GO TO 1500
900 IF (I*COUNT).13.6E.H(11)) GO TO 1510
900 DUM=H(11)
900 GO TO 1520
910 IF (I*COUNT).13.6E.H(11)) GO TO 1530
910 DUM=H(11)
910 GO TO 1540
920 IF (I*COUNT).13.6E.H(11)) GO TO 1550
920 DUM=H(11)
920 GO TO 1560
930 IF (I*COUNT).13.6E.H(11)) GO TO 1570
930 DUM=H(11)
930 GO TO 1580
940 IF (I*COUNT).13.6E.H(11)) GO TO 1590
940 DUM=H(11)
940 GO TO 1600
950 IF (I*COUNT).13.6E.H(11)) GO TO 1610
950 DUM=H(11)
950 GO TO 1620
960 IF (I*COUNT).13.6E.H(11)) GO TO 1630
960 DUM=H(11)
960 GO TO 1640
970 IF (I*COUNT).13.6E.H(11)) GO TO 1650
970 DUM=H(11)
970 GO TO 1660
980 IF (I*COUNT).13.6E.H(11)) GO TO 1670
980 DUM=H(11)
980 GO TO 1680
990 IF (I*COUNT).13.6E.H(11)) GO TO 1690
990 DUM=H(11)
990 GO TO 1700
1000 IF (I*COUNT).13.6E.H(11)) GO TO 1710
1000 DUM=H(11)
1000 GO TO 1720
1010 IF (I*COUNT).13.6E.H(11)) GO TO 1730
1010 DUM=H(11)
1010 GO TO 1740
1020 IF (I*COUNT).13.6E.H(11)) GO TO 1750
1020 DUM=H(11)
1020 GO TO 1760
1030 IF (I*COUNT).13.6E.H(11)) GO TO 1770
1030 DUM=H(11)
1030 GO TO 1780
1040 IF (I*COUNT).13.6E.H(11)) GO TO 1790
1040 DUM=H(11)
1040 GO TO 1800
1050 IF (I*COUNT).13.6E.H(11)) GO TO 1810
1050 DUM=H(11)
1050 GO TO 1820
1060 IF (I*COUNT).13.6E.H(11)) GO TO 1830
1060 DUM=H(11)
1060 GO TO 1840
1070 IF (I*COUNT).13.6E.H(11)) GO TO 1850
1070 DUM=H(11)
1070 GO TO 1860
1080 IF (I*COUNT).13.6E.H(11)) GO TO 1870
1080 DUM=H(11)
1080 GO TO 1880
1090 IF (I*COUNT).13.6E.H(11)) GO TO 1890
1090 DUM=H(11)
1090 GO TO 1900
1100 IF (I*COUNT).13.6E.H(11)) GO TO 1910
1100
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443 DO 450 I=1,5
      CALL V(L,I)-V(L,I+1)
      CCCCCC
444
445 WRITE (6,1759) (X(I),I),Y(I),I-1,5),C9999(I),I),TTF(I),I),WE(I),I),E
      1759 FORMAT(1X,5F10.5)
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14-28-13

09/26/79

STN 4-6436

73/74

SUBROUTINE

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1  SUBROUTINE SUBROUTINE (I, J, K, L, M, N, O, P, Q, R, S, T, U, V, W, X, Y, Z)
2  COMMON /COMMON/ I, J, K, L, M, N, O, P, Q, R, S, T, U, V, W, X, Y, Z
3  DIMENSION I(100), J(100), K(100), L(100), M(100), N(100), O(100), P(100), Q(100), R(100), S(100), T(100), U(100), V(100), W(100), X(100), Y(100), Z(100)
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1  SUBROUTINE 61000 (SLOT, S1, S2, S3, S4, S5, S6, S7, S8, S9, S10, S11, S12, S13, S14, S15, S16, S17, S18, S19, S20, S21, S22, S23, S24, S25, S26, S27, S28, S29, S30, S31, S32, S33, S34, S35, S36, S37, S38, S39, S40, S41, S42, S43, S44, S45, S46, S47, S48, S49, S50, S51, S52, S53, S54, S55, S56, S57, S58, S59, S60, S61, S62, S63, S64, S65, S66, S67, S68, S69, S70, S71, S72, S73, S74, S75, S76, S77, S78, S79, S80, S81, S82, S83, S84, S85, S86, S87, S88, S89, S90, S91, S92, S93, S94, S95, S96, S97, S98, S99, S100)
2  COMMON /SLOT/ S1, S2, S3, S4, S5, S6, S7, S8, S9, S10, S11, S12, S13, S14, S15, S16, S17, S18, S19, S20, S21, S22, S23, S24, S25, S26, S27, S28, S29, S30, S31, S32, S33, S34, S35, S36, S37, S38, S39, S40, S41, S42, S43, S44, S45, S46, S47, S48, S49, S50, S51, S52, S53, S54, S55, S56, S57, S58, S59, S60, S61, S62, S63, S64, S65, S66, S67, S68, S69, S70, S71, S72, S73, S74, S75, S76, S77, S78, S79, S80, S81, S82, S83, S84, S85, S86, S87, S88, S89, S90, S91, S92, S93, S94, S95, S96, S97, S98, S99, S100
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FUNCTION TAB	73/74	PRT=0 TRACE	08/26/79	14-28-13	PAGE
1		FUNCTION TAB (X,X,Y,Y,STAB)			1
		DIMENSION X(1), Y(1)			
5		IF (X(1).GT.X(2)) F=F			
		GO TO J=1-MTAB			
		I=J			
10		DO 10 I=1,X(1)-1			
		10 CONTINUE			
		20 IF (I.ME.1) GO TO 30			
		30 J=I-1			
		DEL X(I)-X(J)			
		10 DEL Y(I)-Y(J)			
15		IF (X(1).EQ.0) GO TO 50			
		10 RETURN			
		40 RETURN			
		50 RETURN			
20		CALL EXIT			
		END			

CARD NR. SEVERITY DETAILS DIAGNOSIS OF PROBLEM
4 1 XX ARRAY REFERENCE OUTSIDE DIMENSION RANGES.


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1  SUBROUTINE ENAP (INTERR)
2  CCCCCC PROGRAMMED 1-22-71 BY W. TAYLOR.
3  CCCCCC THIS ROUTINE IS THE SAME AS IN PROGRAM IMPACT EXCEPT
4  CCCCCC FOR THE CARD CHANGE MARKER CASE
5
10  DATE, VES, ARE INPUT FOR MODP NO. 7 FOR JPA AND JPS/JPP ***
11  ***** NOTE *****
12  CCCCCC INPUT/ OUTPUT DEVICES ARE:
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155 VZ=SQRT(DUM1*0.2+DUM2*0.7)
160 C 110 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
165 C 120 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
170 C 130 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
175 C 140 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
180 C 150 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
185 C 160 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
190 C 170 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
195 C 180 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
200 C 190 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
205 C 200 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
210 C 210 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
215 C 220 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
220 C 230 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
225 C 240 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140
230 C 250 DELT=DELTA*DELTA
      IF (ABS(DELTA-DELTA0)) < 0.01 GO TO 140
      IF (ABS(DELTA-DELTA0)) > 0.01 GO TO 140

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FUNCTION VAPRUF	73/74	OPT=0 TRACE	FTW 4.64439	08/24/78	14.78.13	PAGE	1
1	C	FUNCTION VAPRUF (I)					
		10 TEMPER (BT) VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		11 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		12 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		13 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		14 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		15 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		16 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		17 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		18 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		19 VAPRUF= MJ FOR JPS, JPS/JPS FUEL VAPOR					
		20 RETURN					
		END					

FUNCTION	SECT	73/74	OPT=0 TRACE	FTN 4.64430	08/24/78	14.29.13	PAGE	1
1	C		FUNCTION SECT (1,50000) SCAM - SC RESUME AT 02 DES F LOC 1000.1810 SECT. 02 DES F LOC 1000.200-00000 RETURN END		PRDP PRDP PRDP PRDP PRDP PRDP	32 33 34 35 36 37		
5								

FUNCTION	SCRIPT	73/74	DPT-0 TRACE	PTS 4.0439	00/26/79	10.20.13	PAGE	2
1	C		FUNCTION SCRIPT (E) E- REACTION EVAPORATED, SC60- SC AT 60 DEG F SCRIPT- SC ESTIMATE AT 60 DEG F, SC AT 60 DEG F DATA SC60-175/55600-800 SC60-5600 IF (RFEEL.ME-4) SC60-5600 SCRIPT-1.076/(1.076/SC60-1.1071--6796101.) END		PROP PROP PROP PROP PROP PROP PROP PROP PROP PROP	30 30 30 30 30 30 30 30 30 30		
5								
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08/24/74 14.28.13

FTM 4.04439

73/74 OPT-0 TRACE

FUNCTION VAPOR

3

FUNCTION VAPOR (T,P)
 -1.14000 (1.1) -1.14000 (1.1)
 VAPOR - 8.16000 (1.1) - 8.16000 (1.1)
 VAPOR - 2.00000 (1.1) - 2.00000 (1.1)
 RETURN

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PAGE 1

FUNCTION NAME	73/74	OPT-0 TRACE	
1	FUNCTION NAME: AT	FUNCTION NAME: AT	73/74
	1-LENGTH (4) 1	1-LENGTH (4) 1	67
	ALSO: J=5	ALSO: J=5	68
	COMMON /IMPT2	COMMON /IMPT2	69
	1-LENGTH (4) 1	1-LENGTH (4) 1	70
	ALSO: J=5	ALSO: J=5	71
5	FUNCTION NAME: AT	FUNCTION NAME: AT	72
	1-LENGTH (4) 1	1-LENGTH (4) 1	73
	ALSO: J=5	ALSO: J=5	74
	COMMON /IMPT2	COMMON /IMPT2	75
	1-LENGTH (4) 1	1-LENGTH (4) 1	76
	ALSO: J=5	ALSO: J=5	77
10	FUNCTION NAME: AT	FUNCTION NAME: AT	78
	1-LENGTH (4) 1	1-LENGTH (4) 1	79
	ALSO: J=5	ALSO: J=5	80
	COMMON /IMPT2	COMMON /IMPT2	81
	1-LENGTH (4) 1	1-LENGTH (4) 1	82
	ALSO: J=5	ALSO: J=5	83
	COMMON /IMPT2	COMMON /IMPT2	84
	1-LENGTH (4) 1	1-LENGTH (4) 1	85
	ALSO: J=5	ALSO: J=5	86
	COMMON /IMPT2	COMMON /IMPT2	87
	1-LENGTH (4) 1	1-LENGTH (4) 1	88
	ALSO: J=5	ALSO: J=5	89
	COMMON /IMPT2	COMMON /IMPT2	90
	1-LENGTH (4) 1	1-LENGTH (4) 1	91
	ALSO: J=5	ALSO: J=5	92
	COMMON /IMPT2	COMMON /IMPT2	93
	1-LENGTH (4) 1	1-LENGTH (4) 1	94
	ALSO: J=5	ALSO: J=5	95
	COMMON /IMPT2	COMMON /IMPT2	96
	1-LENGTH (4) 1	1-LENGTH (4) 1	97
	ALSO: J=5	ALSO: J=5	98
	COMMON /IMPT2	COMMON /IMPT2	99
	1-LENGTH (4) 1	1-LENGTH (4) 1	100
	ALSO: J=5	ALSO: J=5	101
	COMMON /IMPT2	COMMON /IMPT2	102
	1-LENGTH (4) 1	1-LENGTH (4) 1	103
	ALSO: J=5	ALSO: J=5	104
	COMMON /IMPT2	COMMON /IMPT2	105
	1-LENGTH (4) 1	1-LENGTH (4) 1	106
	ALSO: J=5	ALSO: J=5	107
	COMMON /IMPT2	COMMON /IMPT2	108
	1-LENGTH (4) 1	1-LENGTH (4) 1	109
	ALSO: J=5	ALSO: J=5	110
	COMMON /IMPT2	COMMON /IMPT2	111
	1-LENGTH (4) 1	1-LENGTH (4) 1	112
	ALSO: J=5	ALSO: J=5	113
	COMMON /IMPT2	COMMON /IMPT2	114
	1-LENGTH (4) 1	1-LENGTH (4) 1	115
	ALSO: J=5	ALSO: J=5	116
	COMMON /IMPT2	COMMON /IMPT2	117
	1-LENGTH (4) 1	1-LENGTH (4) 1	118
	ALSO: J=5	ALSO: J=5	119
	COMMON /IMPT2	COMMON /IMPT2	120
	1-LENGTH (4) 1	1-LENGTH (4) 1	121
	ALSO: J=5	ALSO: J=5	122
	COMMON /IMPT2	COMMON /IMPT2	123
	1-LENGTH (4) 1	1-LENGTH (4) 1	124
	ALSO: J=5	ALSO: J=5	125
	COMMON /IMPT2	COMMON /IMPT2	126
	1-LENGTH (4) 1	1-LENGTH (4) 1	127
	ALSO: J=5	ALSO: J=5	128
	COMMON /IMPT2	COMMON /IMPT2	129
	1-LENGTH (4) 1	1-LENGTH (4) 1	130
	ALSO: J=5	ALSO: J=5	131
	COMMON /IMPT2	COMMON /IMPT2	132
	1-LENGTH (4) 1	1-LENGTH (4) 1	133
	ALSO: J=5	ALSO: J=5	134
	COMMON /IMPT2	COMMON /IMPT2	135
	1-LENGTH (4) 1	1-LENGTH (4) 1	136
	ALSO: J=5	ALSO: J=5	137
	COMMON /IMPT2	COMMON /IMPT2	138
	1-LENGTH (4) 1	1-LENGTH (4) 1	139
	ALSO: J=5	ALSO: J=5	140
	COMMON /IMPT2	COMMON /IMPT2	141
	1-LENGTH (4) 1	1-LENGTH (4) 1	142
	ALSO: J=5	ALSO: J=5	143
	COMMON /IMPT2	COMMON /IMPT2	144
	1-LENGTH (4) 1	1-LENGTH (4) 1	145
	ALSO: J=5	ALSO: J=5	146
	COMMON /IMPT2	COMMON /IMPT2	147
	1-LENGTH (4) 1	1-LENGTH (4) 1	148
	ALSO: J=5	ALSO: J=5	149
	COMMON /IMPT2	COMMON /IMPT2	150
	1-LENGTH (4) 1	1-LENGTH (4) 1	151
	ALSO: J=5	ALSO: J=5	152
	COMMON /IMPT2	COMMON /IMPT2	153
	1-LENGTH (4) 1	1-LENGTH (4) 1	154

FUNCTION CPCT	73/74	CPT-0 TRACE	FTM 4.64439	08/24/78	14.26.13	PAGE	1
1	E	FUNCTION CPCT IT-528601 V. TIMER (R) CPCT, CP FOR LTOUTD J04, J05/J06 52860-56 RESIDUE AT 60 DEC F FOR J04 CPCT (1-181-0004-501)/5081528601 RETURN END		PROG PROG PROG PROG PROG PROG	78 78 80 81 82 83		
5							

OPT=0 TRACE

SUBROUTINE SCALES

```

1  SUBROUTINE SCALES (MAX,MIN,LENGTH,STPP,START)
2  REAL MAX,MIN,LENGTH
3  DIMENSION STPP(101),START(101)
4  DATA STPP /0.1,0.01,0.001,0.0001,0.00001,0.000001,0.0000001,0.00000001,0.000000001,0.0000000001/
5  DATA START /0.1,0.01,0.001,0.0001,0.00001,0.000001,0.0000001,0.00000001,0.000000001,0.0000000001/
6  IF (MAX.EQ.0) THEN
7    MAX=1.0
8  ELSE IF (MIN.EQ.0) THEN
9    MIN=0.0000000001
10  IF (LENGTH.EQ.0) THEN
11    LENGTH=1.0
12  ELSE IF (STPP.EQ.0) THEN
13    STPP=0.1
14  ELSE IF (START.EQ.0) THEN
15    START=0.1
16  IF (MAX.LT.MIN) THEN
17    MAX=MIN
18  IF (MIN.LT.0) THEN
19    MIN=0.0
20  IF (LENGTH.LT.0) THEN
21    LENGTH=0.0000000001
22  IF (STPP.LT.0) THEN
23    STPP=0.1
24  IF (START.LT.0) THEN
25    START=0.1
26  RETURN
27  END
28
29  C 40 FORMAT (/101 VARIABLES OUTSIDE RANGE OF SUBROUTINE SCALE, //101,6
30  1 MAX = ,E12.4,101 MIN = ,E12.4)
31  END

```

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